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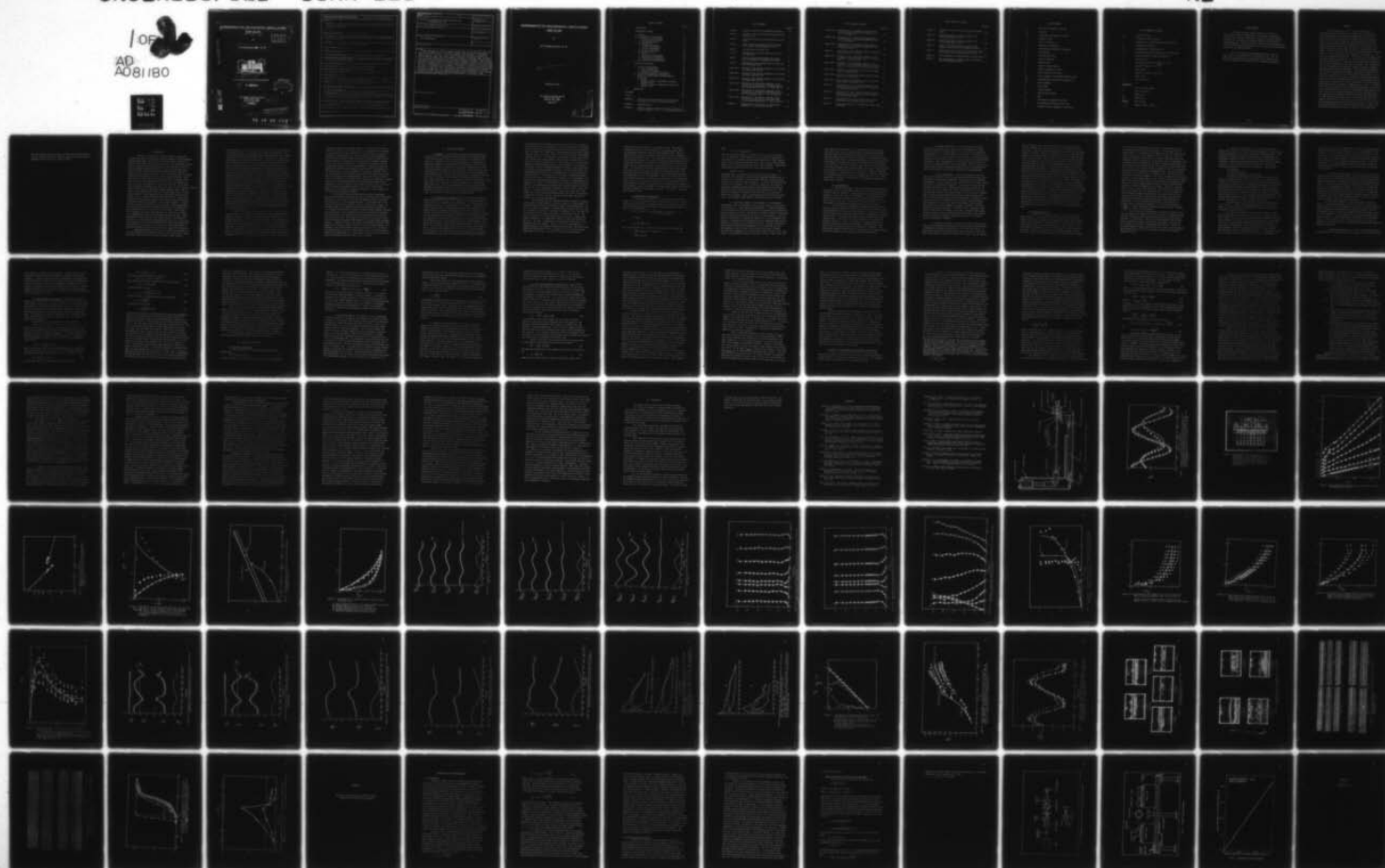
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EXPERIMENTS ON TRANSITIONAL OSCILLATORY PIPE FLOW, (U)
AUG 79 B R RAMAPRIAN, S W TU
IIHR-221

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Microcopy Resolution Test Chart

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EXPERIMENTS ON TRANSITIONAL OSCILLATORY
PIPE FLOW

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B. R. Ramaprian and S. W. Tu



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by

B. R. Ramaprian and S. W. Tu

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LIST OF SYMBOLS

A	area of cross-section of the pipe
A_e	exit area
C_D	coefficient of discharge of the slot
D	diameter of pipe
F	factor in equation 3
f	frequency of oscillation
f_t	characteristic frequency of turbulence
H	constant head
h_t	frictional head loss
K	factor in equation 4
L	length of pipe
M	number of cycles sampled
N	number of samples in a cycle
P	static pressure at any point
P_A	static pressure at an upstream reference point
ΔP^*	non-dimensional pressure drop (Equation 17)
R_e	Reynolds number
r	local radius
S	Strouhal number
ΔT	sampling time interval
t	time
U	instantaneous longitudinal velocity
U^+	non-dimensional velocity in wall layer
u	turbulent velocity component in x-direction

LIST OF SYMBOLS (continued)

u_*	friction velocity
V	instantaneous radial velocity
v	turbulent velocity component in radial direction
x	longitudinal coordinate
x^*	non-dimensional x-coordinate = x/D
y^+	non-dimensional radial coordinate in the wall layer
β	pressure gradient parameter (Equation 23)
λ	friction factor
η	non-dimensional radial coordinate = $1-2r/D$
Ω	frequency parameter, $[D/2 \sqrt{\frac{2\pi f}{\nu}}]$
ρ	fluid density
ν	kinematic viscosity of the fluid
τ	shear stress
τ_w	wall shear stress

Subscripts:

m	cross-sectional average
p	periodic component
q	quasi-steady
max	maximum value
<u>overbar</u>	time average
<u>< ></u>	ensemble (phase) average

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ABSTRACT

Fully developed oil flow in a smooth circular pipe at a mean Reynolds number of about 2100 was subjected to a nominally sinusoidal flow modulation at frequencies ranging from 0.05 - 1.75 Hz. It was observed that flow oscillation increased the critical Reynolds number and, under certain conditions, even brought about laminarization of the flow, which would be intermittently turbulent at the mean Reynolds number under quasi-steady (infinitely small oscillation frequency) conditions. The occurrence and extent of laminarization was, however, found to depend on factors such as the intermittency of turbulent puffs in the mean quasi-steady flow, frequency of oscillation, etc. Two series of experiments were performed. In one series, the oscillatory flow was almost completely laminarized. In the other series, the oscillatory flow was fully turbulent. In both the cases, instantaneous velocities in the flow were measured using Laser Doppler anemometry. The instantaneous velocity was decomposed into time-mean, periodic and random components employing ensemble averaging techniques. The experiments indicated that the laminarized oscillatory flow behaves very similar to laminar oscillatory flow at either end of the Strouhal number range studied. The oscillatory turbulent flow was found to depend on both the Strouhal number and the ratio of the oscillation frequency (f) to some characteristic frequency (f_t) of turbulence in the flow. The design of the present experimental facility made it possible to study the flow at $f/f_t \approx 1$, a condition that could not be attained in most previous investigations. It was found, that at this frequency of oscillation, the Reynolds stresses generally remained frozen at an average state during the entire oscillation cycle. The turbulent structure showed significant departures from equilibrium at all times during the oscillation cycle. As a result, there was a net change in the time-mean velocity profile near the wall and a net increase in the time-mean wall shear stress and power loss due to friction. The data also indicated that the direct interaction between oscillation and the turbulent structure was essentially confined to the Stokes layer.

The study suggests that quasi-steady turbulence models may not be adequate to describe unsteady flows when the time scale of unsteadiness is comparable to that of dominant turbulent eddies.

I. INTRODUCTION

The study of unsteady shear flows is relevant to many areas of application such as aerodynamics, ship hydrodynamics, biofluid mechanics and wind engineering. Much of the study reported in the literature on unsteady flows, however, concerns laminar flows. Exact solutions are available for relatively simple unsteady laminar flow situations in the classical literature [(see Rosenhead 1963)]. Laminar flows in pipes due to periodic pressure gradients have been studied by Richardson and Tyler (1929), and Uchida (1956) and others. The situation with regard to unsteady transitional and turbulent flows is, however, less satisfactory. While there have been some attempts to analyze the problem of stability in periodic flows (e.g., Kerczek and Davis 1974, 1975, Hino and Sawamoto 1975, Hino et al 1976), much remains to be studied in this area. Of the laboratory experiments on periodic pipe channel flow that have been reported in the literature, most pertain to high Reynolds number turbulent flows. The earliest of such experiments were reported by Schulz-Grunow (1940). More recent experiments in this category are those performed by Hirose and Oka (1969), Lu et al, (1973), and Acharya and Reynolds (1975). In all these experiments fully developed turbulent pipe flow was perturbed by imposing a periodic modulation in discharge at a prescribed frequency. Of these, the work of Acharya and Reynolds involved the most detailed measurements such as Reynolds shear stress, though the amplitude of flow modulation in their experiments was less than 5 per cent of the mean. These experiments suggested that even at that amplitude, the structure of turbulence can be significantly affected in the Stokes layer near the wall. Their measurements in this layer were very limited because of the thinness of the layer. Lu et al experienced considerable difficulty in the use of hot film anemometry as well as in analog data processing in their experiments on oscillatory flow of water in a circular pipe. Their measurements of mean and turbulent velocities did not lead to any significant conclusions.

One would intuitively expect that the effects of unsteadiness on the flow structure will be stronger on flows in the neighborhood of transition than on flows at very large Reynolds numbers. This is because

transition process can be sensitive to the strong acceleration/deceleration in the unsteady flow. The experience with steady flows subjected to spatial pressure gradients has confirmed that pressure gradients have a significant effect on the critical Reynolds number. Strong effects of periodic flow modulation on the flow characteristics at transitional Reynolds numbers have, indeed, been observed in the experiments of Sarpkaya (1966) and in the more recent studies of Gerrard (1971) and Hino and Sawamoto (1975). From a study of the growth of disturbances in sinusoidally modulated pipe flow in the mean flow Reynolds number range of 2000-5000, Sarpkaya concluded that flow pulsation increases the critical Reynolds number. Gerrard's experiments related to periodic pipe flow at a mean Reynolds number of 3700 while the experiments of Hino and Sawamoto pertained to purely oscillatory pipe flow (i.e., at a mean Reynolds number of zero). These latter two studies were mainly qualitative but they indicated that, in general, turbulence is inhibited during the acceleration part of the modulation cycle and enhanced during the retardation part. In fact, the flow, under certain circumstances, appeared to remain laminar during the acceleration part of the cycle. Indications of inhibition of turbulence or delayed transition have also been observed in some of the in-vivo studies of pulsatile blood flow in the aorta of mammals (e.g., Falsetti et al 1972, Kiser et al 1976). However, the instrumentation and data reduction techniques used in the blood flow studies, as well as in the other laboratory studies mentioned above, were not sufficiently sophisticated to yield detailed quantitative information on the flow structure.

There is one class of unsteady turbulent flows, however, that has been studied in fair detail using moderate to highly sophisticated data reduction techniques. This is the unsteady turbulent boundary layer in a periodic free stream. Most of these studies (Karlsson 1959, Houdeville et al 1976, Cousteix et al 1977, and Patel 1977) pertain to zero pressure gradient boundary layers though some experiments on adverse pressure gradient flows have been reported recently (Kenison 1977, Houdeville and Cousteix 1978). The experiments on the zero pressure gradient boundary layers have, generally, lead to the conclusion that flow modulation has no effect on the average behavior of the flow and that the turbulent structure can still be

described by quasi-steady turbulence models. A careful study of these investigations, however, reveals that in all these experiments, the frequency of flow modulation was small compared with the characteristic frequency of turbulence in the boundary layer. One can expect to find a significant effect of flow modulation on the average flow structure only when the modulation frequency is comparable to the characteristic turbulent frequency in the flow. The very recent report of Houdeville and Cousteix (1978) on the unsteady boundary layer in the neighborhood of separation (where this condition is satisfied) does indicate strong effects of flow modulation on the flow structure. Hence, the behavior of an unsteady turbulent flow is not only determined by the Strouhal number (ratio of the time scale of mean flow to the time scale of unsteadiness), but also by the ratio of the time scale of unsteadiness to the characteristic time scale of turbulence. Further, since most of the interaction between the impressed oscillation and the turbulence structure is likely to occur within the Stokes layer, it is necessary to design the experiment carefully so as to get a thick enough Stokes layer and yet keep the modulation frequency at a value comparable to the characteristic turbulent frequency.

The present study was directed towards obtaining experimental data on fully developed oscillatory pipe flow at transitional Reynolds numbers. The nature of the periodic flow was found to depend strongly on the nature of the steady flow at the mean Reynolds number. It was found that if the steady mean flow was fully turbulent (with an intermittency of unity), the flow would remain fully turbulent when the Reynolds number was modulated at a frequency large enough to approach the characteristic turbulent frequency. On the other hand, if the steady mean flow was not turbulent but contained turbulent puffs at a low intermittency, the flow would tend to laminarize on periodic oscillation. Both these flow situations were studied in detail using Laser Doppler anemometry (LDA) together with a digital phase averaging technique. Important features of the present experiments, particularly with regard to the turbulent unsteady flow are (i) the oscillation frequency was comparable to the characteristic turbulence frequency in the flow and (ii) the viscous sublayer (2 mm) and Stokes sublayer (6 mm) were thick enough to permit detailed measurements in a region where the interaction of flow oscillation and turbulence have been found to be very strong.

II. EXPERIMENTAL PROGRAM

A. General. A test facility for producing sinusoidally oscillating pipe flow at transitional Reynolds numbers was designed and built for the present study. This facility used Eureka oil (of kinematic viscosity, $\nu = 1.384 \times 10^{-5} \text{ m}^2/\text{s}$ at 26°C) and consisted of a long pipe of 50 mm diameter in which the oscillating flow was maintained. The flow oscillation was produced by varying the flow exit area sinusoidally by a rotating sleeve situated at the exit end of the pipe. The design of the rotating sleeve was very similar to that used in the classical experiments of Schultz-Grunow (1940). The exit area was kept small in comparison with the pipe area so that most of the head loss in the system occurred at the exit. Under such conditions, it is possible to obtain a discharge rate nearly proportional to the exit area. Velocity measurements were made using a single channel LDA. The data was acquired and processed using the IIHR IBM/1800 Data Acquisition System and a data processing technique developed by Mueller and Ramaprian (1977) for the analysis of unsteady turbulent flows. The details are described in the following sections

B. Description of the Apparatus. The experimental apparatus is shown schematically in figure 1. Oil is pumped by the circulating pump from the sump tank to the constant level overhead tank. The overhead tank is a cylindrical reservoir of 0.5 m diameter \times 0.75 m height. The head is maintained constant (about 4 m above the ground level) by providing a 50 mm diameter overflow pipe which returns the extra oil to the sump tank. Oil from the constant head tank flows down through the 100 mm diameter inlet pipe and then through the 200 mm diameter curved pipe. A set of turning vanes is provided in the curved pipe to distribute the flow uniformly in the pipe. The horizontal section of the 200 mm pipe acts as a calming chamber. This section is followed by a bell-shaped contraction nozzle of 50 mm exit diameter. The test pipe is made of copper and has a nominal inlet diameter of 50 mm. It has a total length of 8.8 m, (i.e., $L/D = 176$) which ensures full development of flow even under laminar flow conditions. The pipe has been assembled from sections. The joints between the different sections

have been matched with special care insuring that there are no irregularities in the surface. Twenty-eight wall static pressure taps of 1 mm diameter have been provided at regular intervals along the pipe for the measurement of pressure loss through pipe. These pressure taps have been provided along the bottom of the tube in order to prevent air bubbles from accumulating near the holes. Provision has also been made for flush mounting pressure transducers at three locations along the pipe. The first one is at a point 1.3 m from the contraction exit. The second one is at a point 50 mm upstream from the measurement location and the third at 1.3 m upstream of the second. Pressure transducers mounted at locations 2 and 3 can be used to obtain the pressure gradient in the pipe. The test section where velocity measurements were made is a plexiglass tube, 0.3 m long and 50 mm in internal diameter. The upstream end of the tube is machined and matched with the copper pipe. The other end is connected to a 50 mm diameter \times 300 mm long copper tube whose downstream end is closed. Two longitudinal rectangular slots, 50 mm \times 3.2 mm, milled on the surface of this tube along two generators 180 degrees apart from each other, provide the exit for the oil. The oil falls into a rectangular plexiglass collection chamber (vented adequately to the atmosphere) from where it flows into a weigh tank. The weigh tank rests on a platform weighing machine and is used for measuring the mass rate of flow of the oil. The oil from the weigh tank can be drained via a valve into the sump tank.

The technique used for producing discharge oscillation is similar to that used by Schultz-Grunow. The device consists of a hollow copper cylindrical sleeve rotating over the slotted copper tube mentioned above. One end of the sleeve is profiled on a milling machine in such a way as to form, on development, two cycles of a sine wave of amplitude 12 mm. The other end of the sleeve is closed and is attached to a 13 mm diameter shaft. The shaft is connected to a variable speed motor, by means of a coupling that permits adjustment of the longitudinal position of the sleeve relative to the slots. The shaft is supported by a bearing housed in the wall of the plexiglass collection chamber. The motor is mounted independently on a bracket secured to the framework supporting the apparatus. The motor is manufactured by Bodine Electric and is a geared D.C. motor having an output speed range of 1.2-55 rpm. Its speed is regulated electronically by

controlling the motor voltage via a feed-back circuit. The regulator maintains the speed of the motor within 1% of the preset speed, which is continuously selectable within the range mentioned above. When the sleeve rotates, the area of opening of the pair of slots is continuously varied by the profiled sleeve. It is seen that the exit area variation will be a sinusoidal function of time with the variation going through two cycles during each revolution of the sleeve. The mean exit area can be adjusted within limits by changing the axial location of the sleeve relative to the slots. In the present study, this location has been chosen (after several trial runs) such that the mean flow Reynolds number would be about 2100. The sleeve profile was initially designed for an estimated discharge modulation amplitude of $0.35 \times$ mean discharge. Later tests showed that the actual discharge modulation at infinitely low frequencies (i.e., quasi-steady state), was in fact, quite close to this value. With the present design, it is possible to produce fully laminar flow at the minimum slot opening and fully turbulent flow at the maximum slot opening (under steady flow conditions). At higher frequencies, the amplitude is reduced. This aspect is discussed next in greater detail.

C. Performance of the Apparatus

1. Quasi-steady performance. If H is the gross head available (about 2.7 m), h_f the overall head loss in the system, V_e the exit velocity, V the test section velocity, A_e the exit area, A the cross sectional area of the test section and C_D the discharge coefficient (assumed constant), we have, for quasi-steady flow,

$$H - h_f = V_e^2/2g - V^2/2g \approx \frac{V_e^2}{2g} \quad \left(\text{Since } V \text{ is very much smaller than } V_e \right) \quad (1)$$

$$AV = C_D A_e V_e$$

or

$$V = C_D \frac{A_e}{A} \sqrt{2g(H - h_f)} \quad (2)$$

If $h_f = K V^2/2g$, where K is a constant for the system, one finally gets

$$\begin{aligned} V &= \sqrt{2gH} (C_D A_e / A) [1 / \{1 + K(C_D A_e / A)^2\}^{1/2}] \\ &= \sqrt{2gH} C_D (A_e / A) F \end{aligned} \quad (3)$$

where

$$F = [1/\{1 + K(C_D A_e/A)^2\}]^{1/2}$$

Since C_D is assumed constant, V is proportional to A_e , if F is constant; i.e., if $K(A_e/A)^2 \ll 1$. The frictional loss in the various components of the system can be estimated using standard handbook data. These estimates yield a value of $K \approx 2$ for the present system. The ratio A_e/A has a maximum value of 0.1 in the present case (for fully "open" position). Substituting these values, one gets, for the fully "open" sleeve position,

$$K(A_e/A)^2 = 0.02 \quad (4)$$

This means that F varies from 1.0 to 0.98 from the fully closed to fully open sleeve positions. Thus an almost sinusoidal discharge rate (or velocity) can be expected. The quasi-steady discharge variation with the rotation of the sleeve is shown in figure 2. It is seen that the modulation is very nearly sinusoidal. It is possible to improve the wave shape of modulation by departing slightly from an exact sinusoidal sleeve profile. The required sleeve profile can then, be calculated from Eq. (3). This requires a knowledge of the precise values of K and C_D as functions of quasi-steady discharge. These can be obtained after the steady flow operation. In the present design, however, this procedure was not followed.

2. Unsteady performance. The performance of the system will be described by Eq. (3) only when the exit area is constant or varied infinitely slowly (i.e., under quasi-steady conditions). At finite frequencies of area variation, the flow in the system will be governed by the appropriate unsteady equations of motion. Specifically, the dynamic response of the system will be affected by the inertia of the fluid. As a consequence, as the frequency of oscillation is increased the amplitude of the flow modulation will decrease, the modulation will be distorted from the sinusoidal shape and the pressure at any point in the system will oscillate. Further, the discharge and pressure oscillations will generally be out of phase with the exit area variation. Some of these effects are seen from figure 2 showing the shape of the discharge (or cross sectional average velocity, U_m) vs. time curve, at two different oscillation frequencies; 0.057 Hz and 1.75 Hz. In

this figure, the distribution of U_m is normalized with respect to the quasi-steady cross sectional average velocity at the mid slot opening. The quasi-steady velocity distribution (U_q) as well as an exact sinusoidal distribution are also shown in the figure. The reduction in amplitude and the phase shift of discharge modulation, as well as the distortion in the shape of the modulation curve can be easily seen from the figure. It is seen that at the lower frequency, these effects are very small while at the higher frequency, they are perceptible. We, however, regard the distortion from the sinusoidal shape to be still small enough to be ignored for the purpose of the present study. Likewise, the reduction in amplitude at the higher frequency is no cause for concern, since it is still large enough (20% of the mean) to allow useful and meaningful measurements to be made at this frequency.

D. Instrumentation

1. Pressure measurement. Wall static pressure distribution along the pipe in steady flow was measured using the static pressure taps and an inverted U-tube oil manometer. The most upstream static pressure hole was connected to one of the limbs of the manometer. The other limb could be connected to any static pressure hole via a manifold with which all the static pressure holes were in communication through individual stop cocks. The manometer thus measured the pressure drop from the first hole.

In the unsteady flow experiments, pressure was measured using a pressure transducer mounted flush with the inner surface of the pipe. Pressure measurements were made at only one position viz. at station 2 in Fig. 1. Unsteady pressure drop measurements were, however, not made due to instrumentation problems. The pressure transducer used was an ENDEVCO 8510 semiconductor type, of range 0-15 psi, with a sensitivity of 9.5 mv/psi at an excitation voltage of 5 volts. An IIHR-built strain gage balance and 5-volt-power supply was used with the transducer. The unbalanced voltage output from the bridge was amplified by a PRESTON D.C. amplifier. The instantaneous amplified output which was proportional to the static pressure was measured using the data acquisition technique described later.

2. Discharge measurements. The time averaged flow rate was measured using the weigh tank. The flow rate was measured by clocking the time required for a preset weight of oil to flow into the weigh tank. Unfortunately, due to the small capacity of the tank, it was necessary to limit the duration of oil collection to 15-20 s only. This resulted in some inaccuracy in the estimate of the flow rate, especially in the unsteady flow experiments. These measurements of flow rate were, however, neither critical nor extremely important in the present study. In fact, the flow rate could be more accurately determined in specific cases by integrating the velocity distribution across the pipe obtained from LDA measurements.

3. Velocity measurements. Velocity measurements in unsteady flow studies reported so far in the literature have been made using either pitot-tubes or hot-wire/film anemometry. These probes have two important disadvantages; (i) they disturb the flow and (ii) they do not allow reversals in velocity to be detected or measured. In addition, the Pitot tube has the added limitations that it cannot measure turbulent intensity nor can it even be used in any except very slowly oscillating flows. One of the most important features of the present study is the use of LDA, a technique that can measure instantaneous flow velocities without disturbing the flow. The LDA has also the additional advantages that its signal is proportional to the velocity and that it does not require calibration against other standards. One can, thus, avoid the calibration drift problems associated with hot-film anemometry in liquids. Reversal of flow can be detected and measured using LDA if a "frequency shift" technique is used. The LDA system used in the present studies used a frequency-shift feature though flow reversal did not actually occur in the range of flows studied. The single channel LDA system of IIHR and the details of the traverse system are described in appendix A.

4. Reference time signal. In the present report, the time history of the flow during the oscillation cycle was studied using the instant of maximum slot opening as the reference ($t = 0$) point in the cycle. As will be seen later, the Data Acquisition System was designed to use this point as the instant at which data sampling should begin. For this purpose

an electromagnetic device was used to produce a voltage pulse at the instant of maximum slot opening once during each revolution of the profile sleeve. (Note that this corresponds to once in every two oscillation cycles). The device included an electromagnetic pick up (1.5 mm diameter) mounted on the support frame and a thin steel rod (1.5 mm diameter) attached to the motor shaft. The position of the rod was carefully adjusted such that during its rotation the tip passed within 1 mm of the pick up, cutting the magnetic field. The voltage induced in the pick up was used as the reference time signal. The intensity and duration of the pulse would depend upon the diameter of the rod and its rotational speed. The diameter of the rod (1.5 mm) was determined from the requirement that a signal of sufficient strength to drive the Data Acquisition System was to be produced at the lowest speed studied. With this diameter and with the radius of rotation of the rod of about 150 mm, the pulse duration was found to vary from about 2.5 degrees, at the lowest speed, to about 3.5 degrees at the highest speed of rotation. This corresponds to the range 5-7 degrees when referred to an oscillation cycle and represents the overall uncertainty in the reference time signal. The phase angle measurements reported in this study are all subjected to this uncertainty. The angular position of the rod was adjusted such that the rod was aligned with the pick up in the maximum slot opening position. A 360-degree graduated protractor fixed to the plexiglass collection chamber and a pointer attached to the shaft enabled setting up the sleeve at any desired position (θ) relative to the maximum slot opening position ($t = 0$ or $\theta = 0$) in steady flow experiments.

E. Experimental Details

1. General. As already mentioned, two series of experiments were carried out. In both the series, the steady flow had a Reynolds number of about 2900 at maximum slot opening ($\theta=0^\circ$) and a Reynolds number of about 1300 at minimum slot opening ($\theta=180^\circ$). The mean steady flow Reynolds number was about 2100 and this occurred at $\theta \approx 90^\circ$. However, in the first series, the steady flow at $\theta=90^\circ$ was found to be fully turbulent at all times. In fact, the intermittency of turbulence remained at unity for $\theta \leq 100^\circ$. When this flow was oscillated at the highest possible frequency

of 1.75 Hz, the flow remained fully turbulent. Instantaneous velocity measurements were obtained across the pipe for this situation (Run 13). A rough estimate of the turbulent burst frequency in this flow using the criterion of Rao et al, (1971) indicates a value of about 2 Hz. Thus the oscillation frequency can be expected to interact significantly with the turbulent structure in this flow. In the second series of experiments, while the steady flow at the maximum and minimum slot opening behaved exactly as in the first series, the mean flow at $\theta=90^\circ$ exhibited an intermittent turbulent structure. The structure strongly resembled the puff type transitional structure studied by Wygnanski and Champagne (1973). In fact, the steady flow became fully turbulent only at values of $\theta \leq 60^\circ$. When this flow was oscillated (at whatever frequency) it was found to laminarize with the intermittency of puffs dropping almost to zero. This is clearly seen from figure 3 where a photograph of the storage oscilloscope traces corresponding to the center line velocity signals obtained from the LDA under three different conditions are shown superimposed on one another. These are: i) steady flow at $\theta=0^\circ$, $Re = 2872$ (fully turbulent), ii) steady flow at $\theta=180^\circ$, $Re = 1278$ (fully laminar) and (iii) oscillatory flow at 0.057 Hz between the above two Reynolds numbers (laminarized). The peak velocity in the oscillatory flow is different from the velocity in steady turbulent flow because the steady flow is laminar and hence has a different velocity distribution. Velocity measurements were made in this laminarized unsteady flow at oscillation frequencies of 1.75 Hz (Run 23) and 0.057 Hz (Run 24). These frequencies correspond to Strouhal numbers S (defined as $\frac{2\pi f D}{U_m}$) of 1.0 and 0.032 respectively.

In both the series, measurements of velocity distribution in the pipe were made for the steady flows at $\theta=0$ and $\theta=180^\circ$. In addition, steady flow axial pressure drop data were obtained for several (fixed) angular positions, θ of the sleeve. These steady flow experiments can be considered to approximate closely to quasi-steady experiments. They are used as a reference in the study of the unsteady flow behavior. The use of these data instead of steady flow data from other sources is both necessary and desirable in view of the very low Reynolds numbers and transitional nature of the flow.

2. Quasi-steady measurements. One of the features of the present design is that it allows one to make measurements at steady flow conditions corresponding to any desired point on the oscillation cycle. These measurements closely approximate to quasi-steady flow measurements, i.e., measurements obtained in unsteady flow oscillating at infinitesimally low frequencies. These quasi-steady measurements form the basis for studying the effect of flow oscillation at finite frequencies. Quasi-steady measurements were made in both series of experiments. These included:

- (1) discharge
- (2) pressure drop and
- (3) velocity distribution across the pipe.

The discharge measurements were made using the weigh tank and have been already referred to earlier in Section D.2. As mentioned previously, it was found that due to the small collection time used, there was some inaccuracy introduced into the discharge measurements. The discharge data obtained from the weigh tank measurements were compared with the more accurate values obtained from the integration of velocity profiles in the test section and a correction factor for the former was arrived at. This was used for the rest of the discharge data from the weigh tank. These discharge measurements were made for several fixed slot openings (i.e., for several fixed values of θ) in both the experimental series.

The distribution of static pressure along the pipe was measured only in series 2. Pressure drop measurements were made for several values of θ . These pressure measurements were made using the inverted oil manometer mentioned earlier.

The velocity measurements were made in both series. However, they were made only for two values of θ ; $\theta=90^\circ$ and $\theta=0^\circ$ (Runs 11, 12; 21, 22). Further, the velocity profiles were measured at 16 points across the pipe in series 1. In series 2, velocities were measured at a fewer number of points. Since these measurements appeared to reproduce closely the first series of measurements, it was felt unnecessary to obtain data at finer intervals. The velocity measurements were made using the IIHR Data Acquisition System, as described in Section F. Measurements at $\theta=90^\circ$ (i.e., in laminar flow) served to check the accuracy of measurement as

well as the quality of flow (axisymmetry) in the pipe by comparing the observation with the theoretical parabolic profile. Measurements in fully turbulent flow ($\theta=0^\circ$) provided the basis for studying the effect of flow oscillation. The turbulent velocity distribution in the pipe at low Reynolds numbers is strongly dependent on the Reynolds number and possibly on the characteristics of the specific experimental apparatus. It is thus necessary to use the quasi-steady measurements in the same apparatus at similar Reynolds numbers in order to make any comparisons with unsteady flow measurements.

3. Unsteady flow measurements. The flow was oscillated at the desired frequency by setting the voltage control of the motor at the appropriate position. The rotational speed (equal to twice the oscillation frequency) was measured by clocking the time taken for 50 revolutions of the sleeve. Several minutes were allowed to elapse after starting the oscillations before the measurements were made. As in the case of quasi-steady flow, velocity measurements were made at 16 points across the pipe. The instantaneous velocity signal from the LDA, was read on to the IIHR Data Acquisition System and processed using the procedure described in section F. The reference time signal from the magnetic pick-up was used as the synchronizing signal in the data acquisition process.

An oscillation frequency of 1.75 Hz was studied in series 1. (Run 13). As already mentioned, the flow was observed to be fully turbulent in this case. At lower frequencies (say <1 Hz), the flow was found to switch intermittently between laminar and turbulent regimes. This was accompanied by large variations in the "mean" velocity of the flow. Hence, it was not possible to make any quantitative velocity measurements under these conditions. In the second series of experiments, the flow remained laminar or nearly laminar at 1.75 Hz (Run 23) as well as at a very low frequency, viz. 0.057 Hz (Run 24). Detailed velocity profiles were obtained at these two frequencies.

4. Intermittency measurements. A careful and extended study did reveal that even in the second series of experiments, the flow did not remain

fully laminar at all oscillation frequencies. It became turbulent intermittently and this intermittency was found to depend on the oscillation frequency. In order to study this aspect in some detail, the velocity signal from the LDA was recorded on a strip chart recorder for a duration long enough to allow one to estimate the intermittency of turbulence from the record. This duration corresponded approximately to 300 cycles or 5 minutes whichever was larger. Such records were obtained for several oscillation frequencies in the range of 0.05 Hz - 1.75 Hz and for two points in the pipe, viz., $r = 0$ mm, and $r = 18.4$ mm.

F. Data Acquisition and Processing. The procedure used in the present study for the analysis of unsteady turbulent flows is based on that used by Nakato (1974) and is essentially similar to that used by many recent investigators of oscillatory turbulent boundary layers. The author considers it to be superior and more informative than the analog procedures used by previous investigators of pulsating flows in arteries or rigid walled-tubes. The analysis can be used in a degenerate form for unsteady laminar flows, steady turbulent and steady laminar flows also. The analysis is briefly described below.

Let the instantaneous velocity $U(y, ,t)$ be written as:

$$U(r,\theta,t) = \bar{U}(r) + U_p(r,\theta) + u(r,\theta,t) = \langle U(r,\theta) \rangle + u(r,\theta,t) \quad (8)$$

where \bar{U} is the time mean velocity, u is the turbulent (random) velocity, and $\langle U \rangle$ is the deterministic velocity. The deterministic velocity can be obtained by a process of ensemble averaging. In the present periodic flow, ensemble averaging is equivalent to phase averaging i.e., averaging over the values obtained at identical values of r and θ in a large number of cycles. Thus,

$$\langle U(r,\theta) \rangle = \frac{1}{N} \sum_{i=1}^N U_i(r,\theta,t) \quad (9)$$

where N is the total number of cycles being averaged and U_i is the velocity in the i th cycle. The time mean value $\bar{U}(r)$ is obtained by long time averaging or equivalently by averaging $\langle U \rangle (r,\theta)$ over a cycle. Thus,

$$\bar{U}(r) = \frac{1}{2\pi} \int_0^{2\pi} \langle U(r,\theta) \rangle d\theta \quad (10)$$

If M discrete samples are taken during a cycle, we can write

$$\bar{U}(r) = \frac{1}{M} \sum_{j=1}^M \langle U_j(r, \theta_j) \rangle \quad (11)$$

The random velocity component u is obtained as

$$u(r, \theta, t) = U(r, \theta, t) - \langle U(r, \theta) \rangle \quad (12)$$

The ensemble average value of turbulent velocity u_p' defined by

$$u_p'(r, \theta) = \sqrt{\langle u^2(r, \theta, t) \rangle} \quad (13)$$

is obtained from the process

$$u_p'(r, \theta) = \sqrt{\left[\frac{1}{N} \sum_{i=1}^N u_i^2(r, \theta, t) \right]} \quad (14)$$

and the rms value of turbulent velocity $u'(y)$, defined by

$$u'(r) = \sqrt{u_p'^2(r, \theta)} \quad (15)$$

is obtained from the process

$$u'(r) = \sqrt{\frac{1}{M} \sum_{j=1}^M u_p'^2(r, \theta_j)} \quad (16)$$

In the present experiments, the Data Acquisition System was programmed to sample the LDA output once at the end of each sampling interval (ΔT), starting from the instant when the synchronizing signal (reference time signal) was received. ΔT was so chosen that $100 \Delta T \approx$ the period of oscillation. This would ensure that 100 samples could be taken per cycle. However, only 96 samples were taken, no samples being taken at the end of 97th, 98th, 99th, and 100th time intervals. These "holes" in the data were required in order to allow for the fact that the period of oscillation might not be exactly equal to but less than $100 \Delta T$. It may be noted that with the present program, data would be acquired actually from two consecutive oscillation cycles, the first cycle yielding 50 (No. 1 - No. 50) samples and the second cycle yielding 47 (No. 50 - No. 96) samples. A total of 100 revolutions were used for phase averaging ($N = 100$) at the higher oscillation frequency. At the lower frequency, 25 revolutions were used. From the sampled data, the various velocities \bar{U} , U_p , u' , etc were computed according to Eqs (8) through (12). In most cases, the experiments were repeated thrice and the results averaged over the three experiments. If the results in consecutive experiments differed significantly from one

another, the experiments were repeated till three consecutive experiments gave nearly the same results. (Such repetitions were, however, rarely necessary). The value of \bar{U} varied insignificantly among consecutive repetitions, while the scatter in $\langle U \rangle$ was within 1% and the scatter in u' within 5%. The computer programs in Assembler Language used in the present experiments for both the acquisition and the subsequent processing of the data were developed by Mueller (see Mueller and Ramaprian 1977) from an earlier version developed by Nakato (1974). A listing of the program package used in the present experiments is given in Appendix C. One of the important features of the present program was that it would detect the LDA signal drop-out and reject the samples taken during such a cycle. Data acquisition would then proceed until N valid revolutions were sampled. However, with the use of frequency shift technique, there was virtually no "signal dropout" problem and this feature in the program was never made use of.

The above program package was also used for processing unsteady laminar flows, the value of u' in this case being used as a measure of the noise in the optics and electronics. It was found that u' ranged from 2-5 parts per 1000 in these cases, indicating the acceptability of the experimental procedure. The program package was also used for processing steady flow (laminar and turbulent) data, the quantities \bar{U} and u' being the only quantities sought for in these cases. While experimenting with steady flows, a fictitious synchronizing signal was provided from a square wave generator with a period of approximately 3 seconds. With 100 "cycles" of sampling, this would result in an overall averaging time of 5 minutes.

The unsteady data acquisition program package was also used for the unsteady pressure measurements referred to in section D.1.

III. RESULTS AND DISCUSSION

A. Steady Flow Measurements

1. Axial pressure drop. The nondimensional pressure drop ΔP^* defined by

$$\Delta P^* = (P_A - P) / (1/2 \rho \bar{U}_{qm}^2) \quad (17)$$

is shown in figure 4 for various values of θ (i.e., for various Reynolds

numbers). P_A is the static pressure at an upstream reference point, $x=0$ (see figure 1). P is the static pressure at a longitudinal location x and ρ is the fluid density. The values shown are from the second series of experiments. The figure shows that mean flow has attained full development at all Reynolds numbers for $x^* = x/D \geq 70$. The quasi-steady friction factor, λ_q is defined in the usual way as

$$\lambda_q(\theta) = - \left[\frac{dP}{dx}(\theta) D \right] / \left[\frac{1}{2} \rho \bar{U}_{qm}^2 \right] = \frac{d(\Delta P^*)}{dx^*} \quad (18)$$

and thus, is given by the slope of the lines in figure 4. The values of λ_q at different Reynolds numbers are shown in figure 5. Also shown for comparison are the laminar relation, $\lambda = 64/Re$ and the Blasius relation for low Reynolds number turbulent flows, $\lambda = 0.3165 Re^{-1/4}$ (Schlichting 1968). The value of \bar{U}_{qm} used in figures 4 and 5 were obtained from discharge measurements made using the measuring tank. Figure 5 is presented to show that the apparatus was functioning as expected and that the flow was transitional.

2. Velocity distribution. The results of velocity measurement at $\theta=180^\circ$ (minimum slot opening) and $\theta=0^\circ$ (maximum slot opening) are shown in figure 6. In each case, data obtained in both the series of experiments are shown even though fewer points are shown for series 2. This is considered adequate in view of the excellent repeatability observed between the two series of steady flow experiments. In the case of laminar flow ($\theta=180^\circ$), the data are seen to agree well with the theoretical parabolic profile. This good agreement, however, has been obtained, as already mentioned, by applying a constant "zero correction" to the apparent location of the measurement point. The adjustment is justified by the fact that a constant zero correction brings the measured profile in agreement with the parabolic profile. The same correction was applied to the turbulent flow ($\theta=0^\circ$) measurements also. It is seen from the figure that the mean velocity profiles in turbulent flow obtained from the two series of experiments also indicate agreement with each other. The agreement between the two sets of data obtained with a gap of several months in between establishes the accuracy of the measurement procedure. It also confirms that the behavior of the

quasi-steady flow at both the maximum and minimum end of the oscillation cycle did not change even though the transitional character at intermediate Reynolds numbers had changed.

The velocity profile for the turbulent flow at $\theta=0^\circ$ is shown in figure 7 in the usual wall layer coordinate U^+ ($=\bar{U}/u_*$) vs. Y^+ [$=(D/2-r)u_*/\nu$] u_* being the shear velocity, $\sqrt{\tau_w/\rho}$ where τ_w is the wall shear stress. The value of u_* was obtained from the quasi-steady pressure drop and discharge data for $\theta=0^\circ$ using the relation,

$$\lambda_q = \frac{1}{8} \frac{u_*^2}{U_{qm}^2} \quad (19)$$

The measured velocity distribution is compared with the universal law of the wall, namely $U^+ = Y^+$ in the viscous sub-layer and $U^+ = 5.75 \log Y^+ + 5.5$ in the fully turbulent region. The deviation of the experimental data from the universal log law is to be expected in view of the very low Reynolds number of the flow. On the other hand, the fact that the first data point near the wall falls on the linear $U^+ = Y^+$ curve indicates not only that this point is in the viscous sub-layer but also that the value of u_* and r are accurate.

3. Turbulence intensity distribution. Figure 6 introduced earlier, also shows the distribution of the rms intensity, u' of the longitudinal turbulent velocity fluctuations in the steady turbulent flow at $\theta=0$. The distribution is normalized using the velocity and length scales, u_* and $D/2$ respectively. Consequently, the distribution can be expected to show Reynolds number dependence in the inner region. This is, in fact, the case as is seen from the comparison with the data of Laufer (1954) obtained at a Reynolds number of 5×10^5 . The distribution in the region $0.5 < (1-2r/D) < 1$ seen to coincide reasonably well with Laufer's data while in the region $(1-2r/D) < 0.5$, a strong Reynolds number effect is observed. In fact, the large viscous region in the present case allows one to observe the gradual decrease of u' from a maximum towards zero at the wall, a feature which is usually difficult to observe in higher Reynolds number laboratory flows. The purpose of presenting the steady flow

turbulence distribution in figure 6 is to provide a basis for the comparison with the unsteady turbulent flow data. It is clear that it is very important to make comparisons in approximately the same Reynolds number range in order to arrive at reliable conclusions.

B. Velocity Distribution in Unsteady Flow. Figure 8 shows the distribution of the time-averaged velocity \bar{U} across the pipe in the three runs 13, 23, and 24. The velocities, in each case, are normalized with respect to the corresponding velocity at the pipe axis (\bar{U}_{\max}). The distributions are compared with the quasi-steady velocity distributions corresponding to $\theta=180^\circ$ and $\theta=0^\circ$. It is seen from the figure that the unsteady flows in run 23 and run 24 that appeared to be laminar were, indeed, very nearly laminar i.e., they exhibit nearly parabolic velocity distributions. In fully developed oscillatory laminar pipe flow of a Newtonian fluid, the time-mean velocity distribution should be identical to that of the steady Poiseuille flow since the velocity field is determined from the linear equation

$$\frac{\partial U}{\partial t} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + \nu \left[\frac{\partial^2 U}{\partial r^2} + \frac{1}{r} \frac{\partial U}{\partial r} \right] \quad (20)$$

It is seen that, in the high frequency run 23, in which the intermittency of turbulent puffs was negligibly small (see figure 23), the time-mean unsteady flow behaves almost exactly like laminar flow. The deviation of the experimental data of run 24 from the parabolic profile has been caused by the flow becoming turbulent with a larger intermittency than in run 23. It is, however, important to observe from figure 8 that the effect of flow oscillation on the time-mean velocity gradient and hence the wall shear stress, is negligible in both these runs.

When the oscillatory flow is turbulent, the total shear stress (τ) distribution in the pipe is given by the linear equation

$$\frac{\partial U}{\partial t} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + \frac{1}{\rho r} \frac{\partial(\tau r)}{\partial r} \quad (21)$$

and hence the distribution of time averaged shear stress, $\bar{\tau}$ is now given by

$$\bar{\tau}/\rho = \nu \frac{\partial \bar{U}}{\partial r} - \overline{uv} \quad (22)$$

(where u and v are the turbulent velocity fluctuations in the x and r

directions, respectively), the velocity field is not determined by a linear equation. The time averaged velocity distribution, and hence the time averaged wall shear stress need not, therefore, be necessarily the same as in the steady flow at the mean Reynolds number. It is, in fact, seen from figure that the time-mean velocity distribution in the unsteady turbulent flow of run 13 exhibits a point of inflection near the wall and thus differs from the steady state turbulent velocity profile. The time mean velocity gradient at the wall is slightly larger than in the steady case resulting in a larger time-mean wall shear stress. This observation differs from those reported by previous investigators of oscillatory turbulent boundary layers, who concluded that unsteadiness has no effect on the time-mean properties (or even the turbulent structure) of the flow. However, as already mentioned, a significant difference between the present experiment and the earlier experiments is that the oscillation frequency in the present case is comparable to the characteristic turbulent frequency.

Figure 9 presents the variation of the periodic component U_p of the velocity through the oscillation cycle at a few typical points across the pipe. The velocity is normalized with respect to the amplitude $(U_{qmp})_{max}$ of the quasi-steady cross sectional average periodic velocity. The variations are shown only for 700 degrees of oscillation cycle, short record gaps being present (for reasons mentioned earlier) from $0 - 7.2^\circ$ and $698.4 - 720^\circ$, i.e., a total of 4 sampling periods. For run 13, the data are shown only for 600 degrees of oscillation cycle, due to some difficulties encountered during data acquisition. These difficulties were subsequently removed before the second series of experiments were started. However, since data over only 360 degrees of oscillation cycle are sufficient for the purpose of analysis, the loss of redundant data is not serious. In each of the figures 9 (a), (b), (c), the distributions of the unsteady cross sectional average periodic velocity, U_{mp} and quasi-steady cross sectional average periodic velocity, U_{qmp} (proportional to the effective modulation in exit area) are also shown for comparison. The latter curve is the same as the periodic part of the velocity distribution shown in figure 2. A comparison of the laminar flow data for runs 23 and 24 shows that the phase-wise variations are strongly dependent on the oscillation frequency. The variations

appear to be very nearly sinusoidal at the lower frequency while significant distortion in the wave shape can be observed at the higher oscillation frequency. The distortion at the higher frequency is, as mentioned earlier, due to nonlinear effects.

It is also clear from the figures 9 (a), and 9 (b), that at the higher oscillation frequency, there is a significant phase shift between the velocity variation and the exit area opening. Most of this phase shift is brought about by the global dynamics of the system and is observable as the phase shift of unsteady cross sectional average flow. However, there is also a relative phase shift between the local velocity and the cross sectional average velocity. The flow in the wall region leads the cross sectional average flow while the flow in the core region lags behind the average flow. Unfortunately, owing to the uncertainty in phase angle measurement ($\pm 3.5^\circ$) and the distortion in the modulation profile, it is not possible to make a precise quantification of the phase differences nor is it possible to look for differences between the laminar and turbulent flow.

Figures 10 (a), (b), and (c) show cross plots of the distribution of the periodic velocity, U_p across the pipe for a few typical fixed phase angles in the oscillation cycle. It is seen that at the higher oscillation frequency, the variations in U_p are confined essentially to $\eta = (1-2r/D) \leq 0.25$ (i.e., the Stokes layer), the rest of the flow oscillating virtually as one solid mass at all times. At the lower frequency, U_p varies across the entire pipe at all times. The responses of turbulent and laminar flows appear to be qualitatively similar.

Figure 11 shows the distribution of the "amplitude", $(U_p)_{\max}$ of the periodic velocity across the pipe for the three experiments. Since the velocity modulation is distorted from a sine wave especially at the higher frequency, it is not strictly appropriate to use the term "amplitude" without making a formal harmonic analysis. However, in the present case, $(U_p)_{\max}$ denotes one half of the peak to peak variation in the periodic velocity U_p . In the figure $(U_p)_{\max}$ is normalized with respect to the amplitude $(U_{mp})_{\max}$ of the cross sectional average periodic velocity. It is more clearly seen from this figure that at the higher frequency, the amplitude variations are confined to a small region ($\eta \leq 0.25$) near the wall while at the lower frequency the variations extend over the entire pipe cross section.

Also, it is seen that an overshoot occurs in the amplitude distribution. The dominant effect of oscillation frequency is clearly seen from this figure. At the same time, it is possible to notice, in this figure, a difference between the responses of laminar and turbulent flow in the near-wall region. The turbulent flow data of run 13 exhibit a larger overshoot than the laminar flow data of run 23. Also shown in the figure are the results computed from the exact solution of Uchida (1956) for fully developed laminar periodic flow in a pipe under the influence of a pressure gradient sinusoidally varying with time. The pressure gradient variation in the present experiments at the higher frequency differs significantly from that assumed in Uchida's analysis. The experiment at the lower frequency, however, approximates closely to the theoretical case. The data for this experiment are seen to agree reasonably well with the exact solution, any apparent discrepancy being possibly due to the intermittency effects mentioned earlier.

Lastly, the distribution of the ensemble average velocity $\langle U \rangle$ at prescribed phase angles are shown in figures 12 a, b, and c, for a few typical points in the oscillation cycle, for each of the runs. The distribution of the time-mean velocity, \bar{U} is also shown, in each case, for comparison. The velocities are normalized with respect to the time-mean velocity at the center line (\bar{U}_{\max}) corresponding to each run. The distributions at the higher frequency indicate simple displacement but very little distortion from the shape of the time-mean profile in the core region. Near the wall, (in the Stokes layer) however, the profiles cross over and suffer some distortion. However, no reverse flows were observed in the present experiments. At the lower frequency, the different profiles of $\langle U \rangle$ show distortion with respect to the time mean profile across the entire pipe because of the variation of both the amplitude and phase angle of the periodic velocity continuously across the pipe.

C. Effect of Flow Modulation on Turbulence and Transition

1. General. The data obtained in the two series of present experiments provide some insight into the effects of impressed unsteadiness on the structure of turbulence and transition in pipe flow. For convenience, the two series of experiments will be discussed one by one.

2. Results of Series 1 experiments (turbulent unsteady flow):

The distribution of the rms turbulent intensity u' , normalized with respect to \bar{u}_*^1 is shown in figure 13. Comparison with the steady flow data for $\theta=0$ shows that in the oscillatory flow there is a slight decrease in the maximum turbulence intensity near the wall, while the turbulence intensity farther away from the wall is not affected. The near-wall region where the turbulent intensity is affected extends approximately over 25 per cent of the pipe radius and this region coincides with the Stokes layer where significant effects of flow oscillation are observed on the time-mean and periodic structures of the flow also. This result is in agreement with the conclusions of Acharya and Reynolds (1975) that the structure of turbulence is primarily affected within the Stokes layer. The distributions of the ensemble averaged turbulence intensity $u'_p(\theta)$ normalized with respect to the corresponding shear velocity $u_{*p}(\theta)$ are also shown in figure 13 for a few typical fixed phase angles of the oscillation cycle. Large variations in the distributions from one another and from the distribution of u'/\bar{u}_* indicate that the turbulence structure is highly disturbed from equilibrium. The variations in the relative turbulent intensity (u'_p/u_{*p}) with time are shown in figure 14 for two typical locations across the pipe. These figures suggest that the flow was undergoing rapid structural distortion in time. Actually, the wall shear stress (u_{*p}) could nearly follow the changes through the discharge cycle while the turbulent u -fluctuations could not. This is seen clearly from figure 14 which also shows the variation of u_{*p} and the variation of u'_p (not normalized) at these two typical points in the pipe. It is seen that u_{*p} oscillates with a slight phase lead with respect to the cross sectional average periodic velocity U_{mp} , while u'_p remains

¹The shear velocity $u_{*p}(\theta)$ in unsteady flow was obtained from the ensemble average velocity gradient at the wall. The velocity gradient at the wall was calculated from the measured $\langle U(\theta) \rangle$ at the first point near the wall assuming a linear velocity distribution in the viscous sublayer at all instants. This procedure was found to be generally satisfactory as verified from checks made in steady laminar and turbulent flow. In these cases, the wall shear stress obtained by this method compared well (within 3%) with the value obtained from pressure drop measurements. From the ensemble averaged value u_{*p} , the time averaged value \bar{u}_* was obtained from the discrete analog of the relation,

$$\bar{u}_*^2 = \frac{1}{2\pi} \int_0^{2\pi} u_{*p}^2 d\theta$$

practically constant throughout the oscillation cycle. Such a freezing of the turbulent normal stress can be expected to occur when the flow is subjected to rapid strain rates, i.e., when changes occur at time scales comparable to some important characteristic time scale of turbulence. In a wall-bounded flow, we can regard the turbulent burst frequency, f_t to determine such a characteristic time scale (at least near the wall). In the present case the estimated burst frequency is about 2.3 Hz, (using the criterion $\frac{U_m}{f_t D} \approx 5$ of Rao et al 1971). The estimate is rough but is sufficient to indicate that one can expect to find interaction between the external oscillation and the internal turbulence structure when the flow pulsates at a frequency of 1.75 Hz. Stress-freezing is well documented in rapidly accelerated steady flows but studies of rapidly decelerated steady flows are difficult to perform, since the flow in such cases would separate very quickly. One of the interesting features of the present experiments is that the flow experiences large pressure gradients of alternating sign but yet does not actually separate. An estimate of the severity of the pressure gradient in the present case can be made by calculating the value of the Clauser pressure gradient parameter β defined by (neglecting the shear effects),

$$\beta = \frac{D}{2\rho u_*^2} \frac{\partial P}{\partial x} \approx \frac{D}{2u_*^2} \frac{dU_m}{dt} \quad (23)$$

Such a calculation shows that β varies from about -40 to about +40 during a cycle. The magnitudes of β attained during the cycle are comparable with the values for some of the severe adverse pressure gradient steady flows reported in the Proceedings of the Stanford Conference (Coles and Hirst 1978). Not only are the pressure gradients very large but they vary rapidly, the value of $d\beta/dt$ being of the order of 100 sec^{-1} , (based on a variation in β from 40 to -40 in half the period of oscillation). It is thus clear that the turbulent structure will be in a highly disturbed state. Hence, quasi-steady turbulence models based on local equilibrium assumption cannot be expected to describe the flow at such oscillation frequencies.

The quantity which is of greater value than u' in understanding the structure of turbulence is the Reynolds shear stress - $\rho \overline{uv}$. Unfortunately,

on account of instrumentation limitations, it was not possible to make direct measurements of the Reynolds shear stress. However, it is possible to compute it, perhaps with some loss of accuracy, from the measured wall shear stress and velocity distribution. For this purpose, we write the instantaneous x-momentum equation for pipe flow as

$$\rho \frac{\partial U}{\partial t} + \rho U \frac{\partial U}{\partial x} + \rho V \frac{\partial U}{\partial r} = - \frac{\partial P}{\partial x} + \frac{1}{r} \frac{\partial(\tau r)}{\partial r} \quad (24)$$

where V is the instantaneous velocity in the radial direction. Performing an ensemble average on this equation, one gets, for fully developed unsteady turbulent flow,

$$\rho \frac{\partial \langle U \rangle}{\partial t} = - \frac{\partial \langle P \rangle}{\partial x} + \frac{1}{r} \frac{\partial \langle \tau r \rangle}{\partial r} \quad (25)$$

$$\text{where } \langle \tau \rangle = \tau_{\text{laminar}} - \rho \langle uv \rangle \quad (26)$$

We define $-\rho \langle uv \rangle$ as the ensemble averaged Reynolds shear stress. Multiplying both sides of the equation (25) by $2\pi r$ and integrating across the pipe, one gets (after inserting the phase average notations introduced earlier)

$$\rho \frac{\partial U_m(\theta)}{\partial t} = - \frac{\partial \langle P \rangle}{\partial x}(\theta) + \frac{4\tau_w(\theta)}{D} \quad (27)$$

Eliminating $\frac{\partial P}{\partial x}$ between equations (25) and (27) one gets

$$\frac{\tau}{\rho}(r, \theta) = \frac{1}{r} \int_0^r \frac{\partial}{\partial t} [\langle U(r, \theta) \rangle - U_m(\theta)] \cdot r \, dr + \frac{2\tau_w(\theta)r}{D} \quad (28)$$

and

$$-\langle uv \rangle(r, \theta) = \frac{\tau}{\rho}(r, \theta) - v \frac{\partial \langle U(r, \theta) \rangle}{\partial r} \quad (29)$$

The ensemble (phase) averaged Reynolds shear stress $-\langle uv \rangle$ was obtained from Equations (28) and (29) using measured velocity and wall shear stress data. The process required differentiation with respect to time and integration across the pipe both of which were performed numerically on a computer. The velocity-time data were smoothed in order to reduce the numerical noise in differentiation. The procedure was found to work reasonably well because the velocity values were available at very close time intervals (50 values per cycle), velocity gradients in the radial direction were not severe (due to the low Reynolds number of the flow), sufficient cycles were used for phase averaging (effectively 300) and lastly, the three terms in equation (28) were all of similar order of magnitude.

Variation of the ensemble averaged Reynolds shear stress during the cycle is shown in figures 15 a, b, c for three typical locations in the pipe, viz; 1, 2 and 10 mm from the wall. Although there is some scatter in the data, the results are still good enough to allow one to arrive at meaningful conclusions especially in the region of flow where the Reynolds shear stress is significant. Very near the wall, $\langle uv \rangle$ shows a cyclical variation but lags behind U_m (and hence behind u_{*p} also). As the distance from the wall increases, the amplitude of variation of $\langle uv \rangle$ decreases until it becomes almost indistinguishable from scatter beyond the Stokes layer (as seen from figure 15c). The well-defined cyclical variation of $\langle uv \rangle$ in the inner layer (figures 15 a, b) is in contrast to the frozen structure of u'_p . This suggests that the modulation in $\langle uv \rangle$ might have originated from modulations in the ensemble averaged intensity, v'_p . This is possible since the v-fluctuations are likely to be of finer scale than the u-fluctuations (by a factor of nearly 5 as observed by Ramaprian, 1975) and hence can respond more readily to the impressed oscillations. Since the time scale gets larger as the distance from the wall increases, the response of $\langle uv \rangle$ must be expected to diminish eventually in the core region. The nearly frozen structure of $\langle uv \rangle$ in the core region (figure 15c) thus indicates rapid strain rates. The departure from local equilibrium is again seen from the variations in $\langle uv \rangle / u_{*p}^2$ during the oscillation cycle.

Figure 16 a, b, c, and d are cross plots of the above data and show some typical distributions of the total, laminar and ensemble averaged Reynolds shear stresses, across the pipe for fixed phase angles during the cycle. The distributions are normalized using the relevant inner layer scales of velocity, (u_{*p}) and length, (v/u_{*p}) . The large variations in the distribution of the stresses from one point in the cycle to the other (seen more clearly from these figures) again indicate that the turbulence structure is far from equilibrium and hence cannot be described by quasi-steady models. Figure 17 shows the time averaged distributions of each of the above stresses using \bar{u}_* as the scaling velocity. These distributions were obtained by averaging the computed distributions at 50 phase positions in the cycle. It is seen that except for a slight discrepancy near the wall, the time-averaged total shear stress $\bar{\tau}$ shows the expected

linear distribution. This indicates that there were no significant errors in the numerical procedure used for calculating the shear stresses from the experimental data. Some of the important features pertaining to figures 16 and 17 that require comments are:

- (i) The laminar shear stress is significant upto a considerable distance from the wall. This is to be expected in view of the low Reynolds number of the flow.
- (ii) The time averaged turbulent shear stress reaches a maximum at about 6 mm ($\eta=0.25$) from the wall i.e., at about the same location where u' reaches a maximum. It is important to note that this is within the Stokes layer.
- (iii) The time averaged laminar shear stress distribution exhibits a local minimum near the wall. This is due to the presence of a point of inflection in the time-mean velocity profile.
- (iv) The distribution of the time-mean Reynolds shear stress also exhibits a kink within the Stokes layer. Also, it is observed that, in the region very close to the wall, the time-mean Reynolds shear stress attains a value larger than in steady flow.
- (v) The time-mean distributions of the stresses are not significantly different from the corresponding distributions in steady flow, in the region beyond the Stokes layer. However, by affecting the distributions within the Stokes layer, the imposed unsteadiness produces an increase in the time-mean velocity gradient at the wall and hence increases the wall shear stress. This is seen from figures 14 a, b, where the quasi-steady time-mean value, u_{*qm} (obtained from pressure drop measurements at the mean Reynolds number of 2100) is shown as a horizontal dashed line against the distribution of u_{*p} in unsteady flow. The time-mean value of u_{*p} is clearly larger than the quasi-steady mean value of u_* .

Figure 18 shows a few typical distributions of the ensemble average velocity $\langle U \rangle$ in the inner layer co-ordinates $\langle U \rangle / u_{*p}$ vs $(D/2-r)u_{*p}/\nu$. The time-mean distribution \bar{U}/\bar{u}_* vs $(D/2-r)\bar{u}_*/\nu$ is also shown in the figure.

The data display exactly the trend that one would expect to see. In the region very close to the wall $y^+ < 10$, the ensemble average velocity scales with the corresponding u_{*p} but at larger distances from the wall, the flow structure does not keep in step with u_{*p} and hence the data at different phase angles exhibit different distributions. It is also important to note that there is a net difference between time averaged velocity distribution in the unsteady flow (shown by open circles) and the velocity distribution in steady flow (shown by the full line). This difference is seen more clearly in this figure than in figure 8, discussed earlier.

The quantity, $E_p = \int_0^R \{ \langle \tau \rangle \frac{\partial \langle U \rangle}{\partial r} \} 2\pi r dr$ represent the rate of work done per unit length of pipe by the shear stress and hence its average value over an oscillation cycle represents the power loss in the pipe. The term E_p normalized with respect to $(\rho \bar{U}_{qm}^3 \pi D/4)$ is shown in figure 19 as a function of the phase angle. The corresponding power loss in a hypothetical quasi-steady turbulent flow can be obtained for the same Reynolds number modulation using the Blasius relation, $\lambda = 0.3165 Re^{-1/4}$. Also, for the actual transitional quasi-steady flow, the power loss for the same Reynolds number can be obtained from the quasi-steady pressure drop data of figure 4 (or alternately the friction factor data of figure 5). Both these distributions are also shown in figure 19. It is seen that flow oscillation in run 13 at a high frequency results in an increase in average power loss when compared with the quasi-steady transitional flow. This is, however, to be expected since the unsteady flow is fully turbulent during the entire cycle, whereas the quasi-steady flow is not. However, it is interesting to observe that the unsteady flow has a slightly higher average power loss when compared to the hypothetical fully turbulent quasi-steady flow also.

3. Results of Series 2 experiments (laminarized unsteady flow)

During the second series of experiments, the unsteady flow remained nearly laminar. Since this was a very significant observation, it was carefully verified to insure that the laminarization was not due to any obvious reasons such as an increase in fluid viscosity, reduction in flow velocity, etc. Starting from a fully turbulent flow at the fully open slot position, the flow could be laminarized by just rotating the sleeve at the lowest possible speed (0.057 Hz). The photographs in figure 20 show a few typical

oscilloscope traces obtained from the LDA at several oscillation frequencies and include data from two radial locations, $r = 0$ and $r = 18.4$ mm. In each photograph, three traces are shown: (i) fully turbulent steady flow at $\theta=0$ corresponding to a Reynolds number of about 2900, (ii) fully turbulent laminar flow at $\theta=180^\circ$, and (iii) fully or partially laminarized oscillatory flow. The photographs generally confirm that the oscillatory flow had a strong tendency towards laminarization under the operating conditions of the series 2 experiments.

A careful study of the traces at several oscillation frequencies indicated that laminarization was not always complete, and that the oscillatory flow did, in fact, become turbulent at times (as seen in some of the photographs in figure 20). The intermittency of this occurrence depended on the oscillation frequency. In order to make a more detailed study of this phenomenon, several long-time records of the LDA signal were obtained using a strip chart recorder. The record length in all the cases was equal to 300 cycles or 5 minutes whichever was longer. Records were obtained for $r = 0$ and $r = 18.4$ mm. Similar records were obtained in quasi-steady flow for comparison. A few typical records are shown in figures 21 and 22. It is seen that the flow does become turbulent several times during the duration of the record. Estimating the intermittency of turbulence from such records is no doubt difficult and subjective; particularly when turbulent and oscillation frequencies are not well separated. The following procedure was arbitrarily selected for making a rough estimate of the intermittency. The procedure is based on the observation (and assumption) that whenever the flow became turbulent, its velocity level would jump upwards or downward from the laminar value depending on whether the point under consideration was in the wall region or on the centerline. In both the cases, a distortion would be observed in the velocity signal recorded on the strip chart. The dynamic response of the recorder (5 Hz) was adequate for indicating this distortion. A short length of the laminar record traced out on a transparent sheet would be moved over the record and portions of the record that did not coincide with the laminar record would be marked out as turbulent intervals. The intervals marked T in the photographs of figure 22 correspond to typical turbulent intervals. The intermittency factor, γ was defined as the ratio of the total turbulent interval to the

total record length. In the case of steady flow, the turbulent intervals could be easily recognized without much ambiguity.

The intermittency factor is plotted in figure 23 for quasi-steady flow as a function of quasi-steady Reynolds number. It is seen that the mean quasi-steady flow ($\theta=90^\circ$, i.e., $Re \approx 2100$) has an intermittency of about 0.2. The intermittency factor for oscillatory flow is shown in figure 24 as a function of oscillation frequency. A parameter often used in characterizing laminar oscillatory pipe flows is Ω defined as $[D/2\sqrt{\frac{2\pi f}{\nu}}]$. It is seen that Ω is proportional to the ratio of the pipe radius, to the thickness of the Stokes layer. The values of Ω are also shown in figure 24. The data for unsteady transitional flow show some interesting trends. The intermittency is very low at either end of the frequency range studied ($\Omega=4-22$). However, it increases fairly significantly and appears to reach a maximum around an oscillation frequency of about 0.4 Hz ($\Omega \approx 12$). This maximum intermittency factor attained, is not very small, and, at $r=18.4$ mm, is indeed comparable to that of the mean quasi-steady flow. Lastly, the data indicate different values for intermittency near the wall and at the center. It is interesting to note that Yellin (1966) also observed that when transition occurred in pulsatile flows, the disturbances were typically restricted to the core. However, the authors have no explanation at this time for this behavior of the flow. The other aspects of transition in oscillatory flows are examined in some detail below.

Wyganski and Champagne (1973) have reported detailed study of the steady transitional pipe flow. They divide intermittent transitional turbulence into two categories - the "puff" type and the "slug" type. Puffs are caused by large disturbances at the inlet region of the pipe and are actually remnants of a partial relaminarization process. Slugs, on the other hand, originate from the instability of the boundary layer and represent various stages of amplification of these disturbances. The puffs usually occur in the Reynolds number range of 2000-2700 while the slugs appear generally at very much larger Reynolds numbers. The intermittency measurements in steady flow in the present case are compared in figure 23 with the puff flow data from Wyganski and Champagne. The qualitative agreement between the two sets of data suggests that the present transitional flow can be regarded as a 'puff' type flow. This is further borne out by the

fact that the turbulent puffs are of approximately the same intensity near the wall as at the center line (as seen from the strip chart record), unlike a slug type flow which is known to exhibit an increase in intensity from the centerline to the wall. It may be noted also that the flow is fully turbulent at about $Re = 2700$.

The development of turbulence through a puff-type transition process does not depend on shear layer instability near the pipe wall since the disturbance is provided by the inlet conditions but depends on the existence of a Reynolds number above a critical value so that the initial turbulence can be sustained. This threshold critical value is about 2000 and transition to turbulence can not occur below this Reynolds number. In a flow subjected to a favorable pressure gradient, this critical Reynolds number is known to increase. But, in an adverse pressure gradient, it will not decrease significantly below the threshold value. Hence, if the Reynolds number of flow oscillates around 2000, the net effect would be an increase in the critical Reynolds number and hence a partial or complete laminarization of the initial turbulent puffs. The increase in the critical Reynolds number will be larger at larger favorable pressure gradients and hence one would expect to find a greater degree of laminarization as the oscillation frequency increases. This is, exactly what is observed in figure 24 as a decrease in the intermittency in the range of 0.4 Hz - 1.75 Hz ($\Omega=12-22$) with the flow being almost completely laminar at 1.75 Hz. The existence of a maximum intermittency (almost equal to the intermittency in the mean steady flow) at about 0.4 Hz ($\Omega \approx 12$) appears somewhat to contradict the above argument. It is, however, important to note that at low frequencies, (0 - 0.4 Hz), ($\Omega = 0-12$) the favorable pressure gradients are very small (at the amplitude of modulation employed) and consequently, the effect on the critical Reynolds number is negligibly small at these frequencies. On the other hand, the extent of laminarization of the puffs depends not only on the critical Reynolds number but also on the length of time in a cycle the puffs are exposed to a Reynolds number lower than the critical Reynolds number. At low frequencies the latter effect becomes dominant and since the residence time of the puffs below the critical Reynolds number increases as the oscillation frequency is reduced, the intermittency of puffs would

decrease with frequency in this range. The results in this range agree qualitatively with those of Sarpkaya (1966) whose experiments extended over the range $\Omega = 4-7.8$. He found that at small amplitudes of modulation ($\lambda = 0.2 - 0.3$) there was only a slight increase in critical Reynolds number above the steady state value and that increase in the oscillation frequency in this range reduced the rise in critical Reynolds number. Sarpkaya noticed negligible effect of oscillation on the transition characteristics at $\Omega = 7.8$ (which, incidentally, he regarded as 'rapid' oscillation). It is interesting to note that at about 0.4 Hz corresponding to $\Omega \approx 12$ the present unsteady flow exhibits the maximum intermittency. The present observations are thus in qualitative agreement with those of Sarpkaya. There is, however, quantitative disagreement between the present data and those of Sarpkaya with respect to the actual magnitudes of the critical Reynolds number at the various values of Ω . This is due largely to the difference between the definitions of critical Reynolds number used in the two cases. In the present case, the critical Reynolds number is taken to be the Reynolds number at which the puffs (external disturbances) disappear whereas Sarpkaya defined it as the Reynolds number at which the external disturbances cease to amplify. It is thus clear that the present definition describes the lower bound for the puff-type transition process.

The major difficulty with studies connected with puff-type transition is that the process is very sensitive to the nature of external disturbances and other ambient conditions. It is thus very difficult to find repeatability in observations over a period of time. This is especially true when an additional factor, namely flow oscillation, is introduced. This has been clearly demonstrated by the two series of experiments reported in this paper. The two series gave entirely different results under what apparently appeared to be identical conditions. It is worth examining the reasons for this at least in a qualitative way. As mentioned already, the mean steady flow ($\theta=90^\circ$) was fully turbulent in the Series 1 experiments. In fact, it was fully turbulent even at $\theta=100^\circ$ (corresponding to $Re \approx 2000$). Unfortunately, intermittency measurements were not made in these series. However, one can visualize (without much error) the intermittency variation with Reynolds number to be as shown in figure 23. It is very clear that

in this flow, transition occurred within a very narrow range of Reynolds numbers, unlike in the second series of experiments in which it was spread over a much wider range of Reynolds numbers. The reason for this is not known with certainty but a reasonable guess is as follows. The first series of experiments were conducted in summer during which time, the laboratory temperature was about 30°C while the fluid temperature remained at about 26°C. Since the pipe was not insulated, there was heat transfer from the ambient to the fluid. This would aid the process of transition. On the other hand, the second series of experiments were conducted in winter when the laboratory temperature was around 20°C while the fluid temperature still remained at 26°C. There was, thus, a heat transfer from the fluid to the surroundings. This loss of energy to the surroundings would reduce the energy available for producing and completing the transition and hence would tend to stabilize the flow.

The two intermittency distributions shown in figure 23 for the two series can be used to explain qualitatively the observed difference in response of the flow to oscillate at a high frequency in the two cases. Flow oscillation at a high frequency would raise the critical Reynolds number from its value of about 2000 at quasi-steady state by an amount, say, ΔRe . This is equivalent to moving the operating line, i.e., mean flow Reynolds number of the unsteady flow to the left by ΔRe in figure 23. It is seen that in the series 2 experiments, the new operating line corresponds to a laminarized flow (of very small intermittency) while in the series 1 experiments, it corresponds to fully turbulent flow (of intermittency 1). It is to be mentioned here that laminarized oscillatory flow can be observed only under very restricted conditions. These include puff-type transition (i.e., transition brought about by inlet disturbances), a relatively small intermittency of puffs at the mean Reynolds number and either strong pressure gradient fluctuations (high frequency, large amplitude oscillation) or large puff-residence time (long enough pipe). These conditions are often found in the pulsatile flow of blood in the mammalian aorta and hence laminarization of the flow can be expected to occur in such cases. This is, in fact, corroborated by some of the recent in-vivo aorta experiments mentioned at the beginning of this paper.

IV. CONCLUSIONS

The present study has lead to the following conclusions:

(i) Periodic oscillation of discharge tends to increase the critical Reynolds number of puff-type transitional pipe flow. Under certain conditions, the transitional flow may be laminarized on periodic oscillation. For a given amplitude of flow modulation the extent of laminarization depends on factors such as the intermittency of puffs in the quasi-steady mean flow, the oscillation frequency and the residence time of the puffs in the pipe.

(ii) The laminarized periodic flow behaves very much like laminar periodic flow. For example, the time-mean flow properties remain unchanged from those of quasi-steady mean flow and the phase lag and amplitude of the periodic velocity component depend strongly on the Strouhal number.

(iii) When the oscillatory flow is fully turbulent, its time mean and periodic structure qualitatively resemble those of oscillatory laminar flow at the same Strouhal number. However, the behavior of the oscillatory turbulent flow is also influenced by an additional parameter, namely the ratio of the oscillation frequency to some characteristic frequency of turbulence. When this ratio is of the order unity, the oscillations interact with the turbulent structure. Important differences can be observed between laminar and turbulent flows at such oscillation frequencies. For example, the time-mean velocity profile in the oscillatory flow exhibits a point of inflection near the wall, and the time mean wall shear stress and power loss increase from their quasi-steady values. Also, the periodic velocity component exhibits an overshoot in the Stokes layer, the magnitude of the overshoot being larger than in laminar oscillatory flows at the same Strouhal number.

(iv) At the interactive frequency of scillation, mentioned above, the ensemble averaged turbulence intensity is frozen everywhere in the pipe. The ensemble averaged Reynolds shear stress is able to follow the oscillation cycle (with some lag) only very close to the wall. However, beyond the Stokes layer, it is also frozen at some average value. The stress freezing

is brought about by the large and rapidly varying strain rates. The ensemble averaged Reynolds stresses as well as the ensemble averaged velocity do not scale with the corresponding ensemble averaged wall shear stress indicating significant departures from local structural equilibrium.

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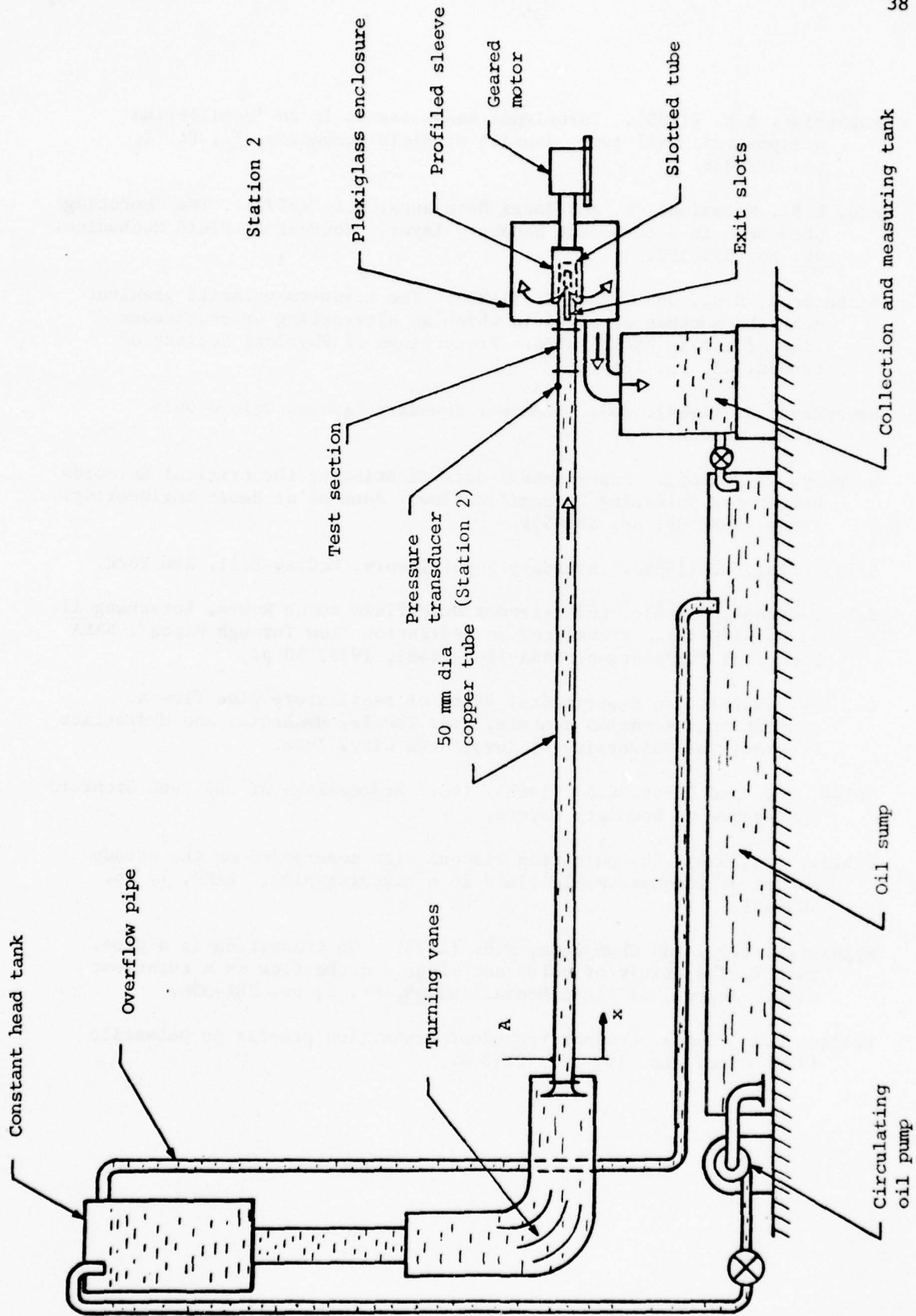


Figure 1. Schematic layout of the experimental apparatus

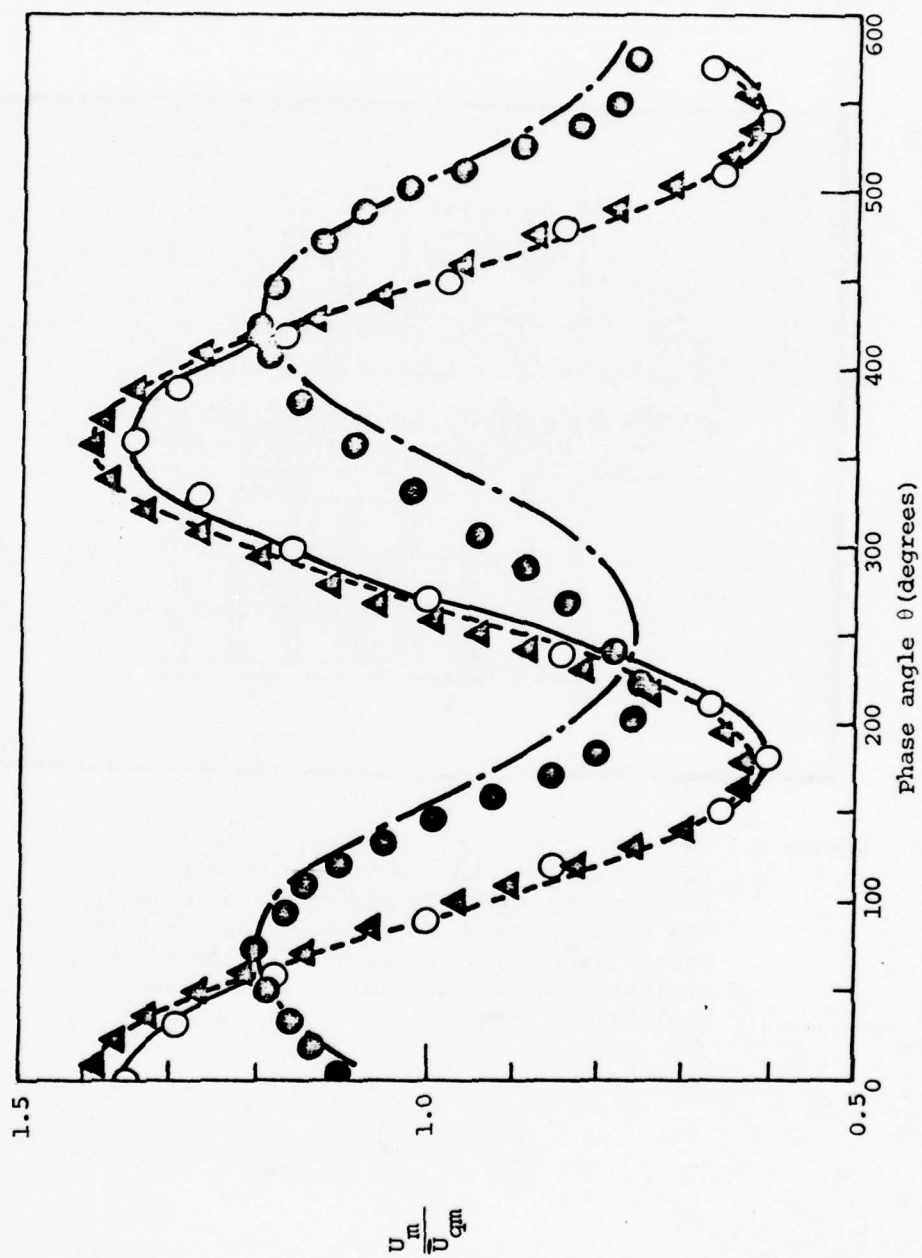


Figure 2. Variation of the cross sectional average velocity during a cycle.
 0, quasi-steady; Δ , oscillatory flow at 0.057 Hz (Run 24); \bullet , oscillatory flow at 1.75 Hz (Run 13); Lines denote exact sine waves with corresponding amplitude; ---, quasi-steady; -.-, 0.057 Hz; —, 1.75 Hz

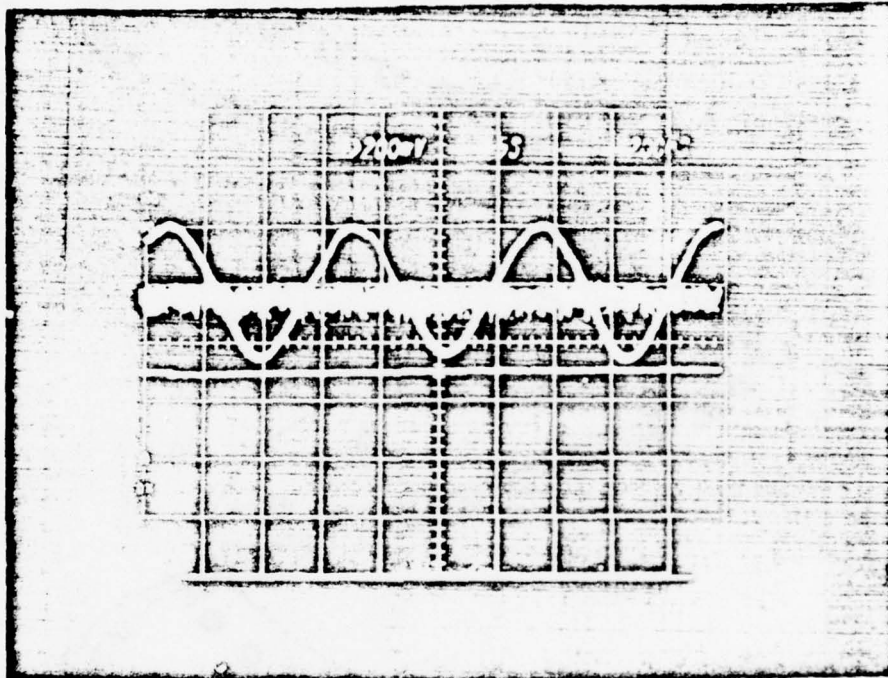


Figure 3. Oscilloscope traces of velocity signals From LDA ($r=0$). The smooth horizontal trace corresponds to steady laminar flow ($\theta=180^\circ$); the hashed horizontal trace corresponds to steady turbulent flow ($\theta=0^\circ$); the smooth sinusoidal trace corresponds to laminarized oscillatory flow

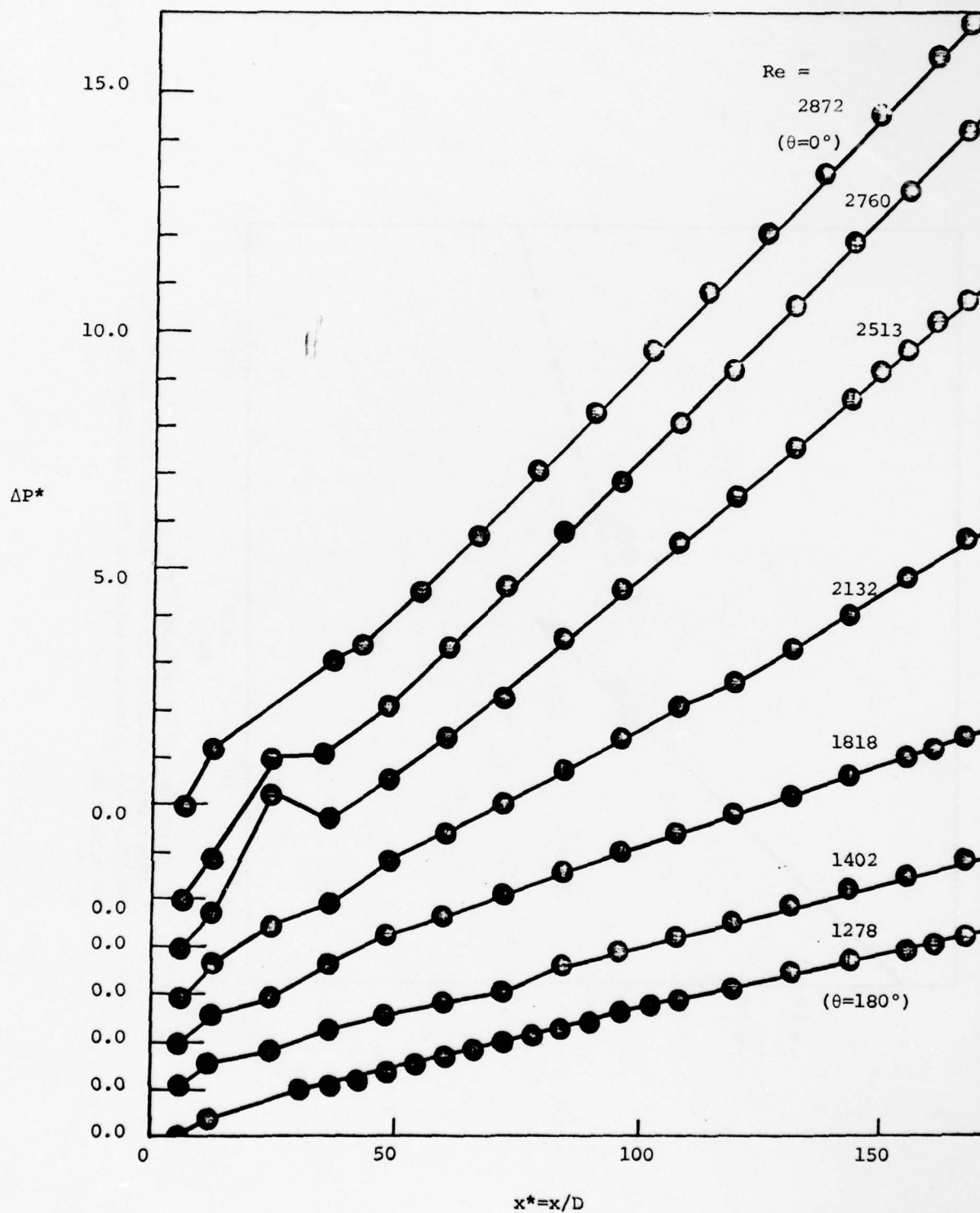


Figure 4. Static pressure drop along the pipe in steady flow; results from experiments of series 2.

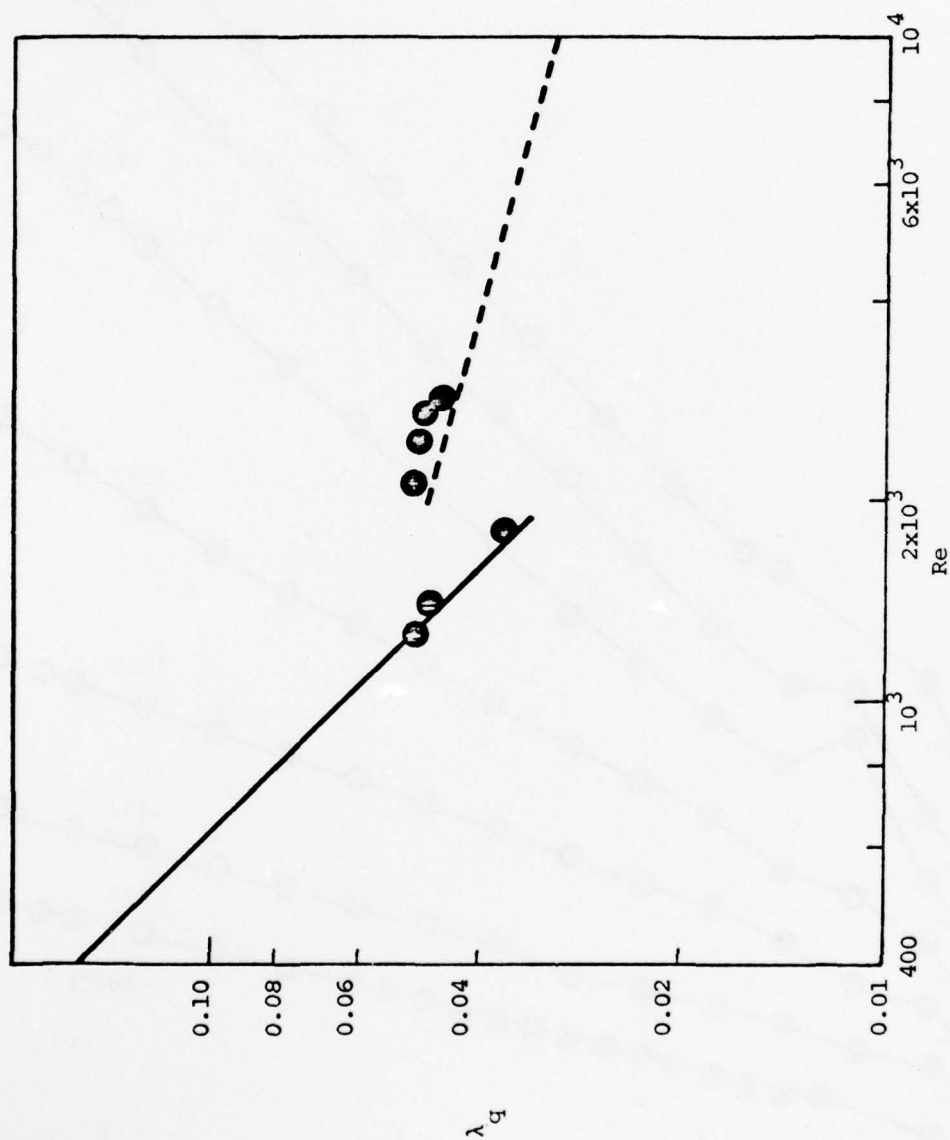


Figure 5. Friction factor in steady flow
 ● Experiment (series 2); —, laminar flow relation $\lambda = 64/Re$; ---, Blasius equation for turbulent flow, $\lambda = 0.3165 Re^{-1/4}$

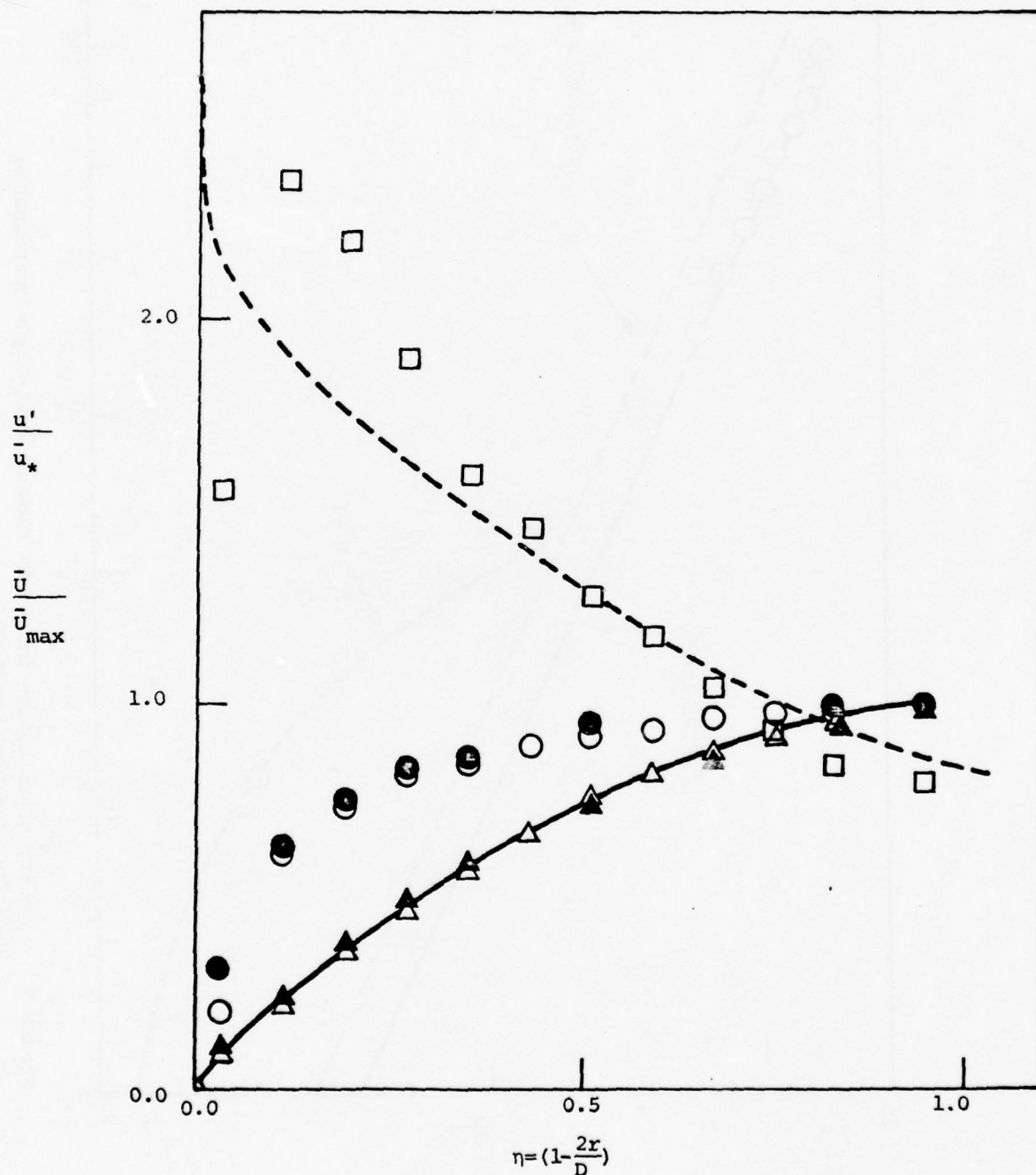


Figure 6. Distributions of mean and turbulent velocities in steady flow.
 mean { Δ , Run 11; \blacktriangle , Run 21 Laminar flow at $\theta=180^\circ$ ($Re=1278$)
 velocity \circ , Run 12; \bullet , Run 22 Turbulent flow at $\theta=0^\circ$ ($Re=2870$)
 ---, theoretical parabolic profile for laminar flow
 Turbulent intensity: \square , Run 12; --- data from Laufer (1954)
 for $Re=5 \times 10^5$

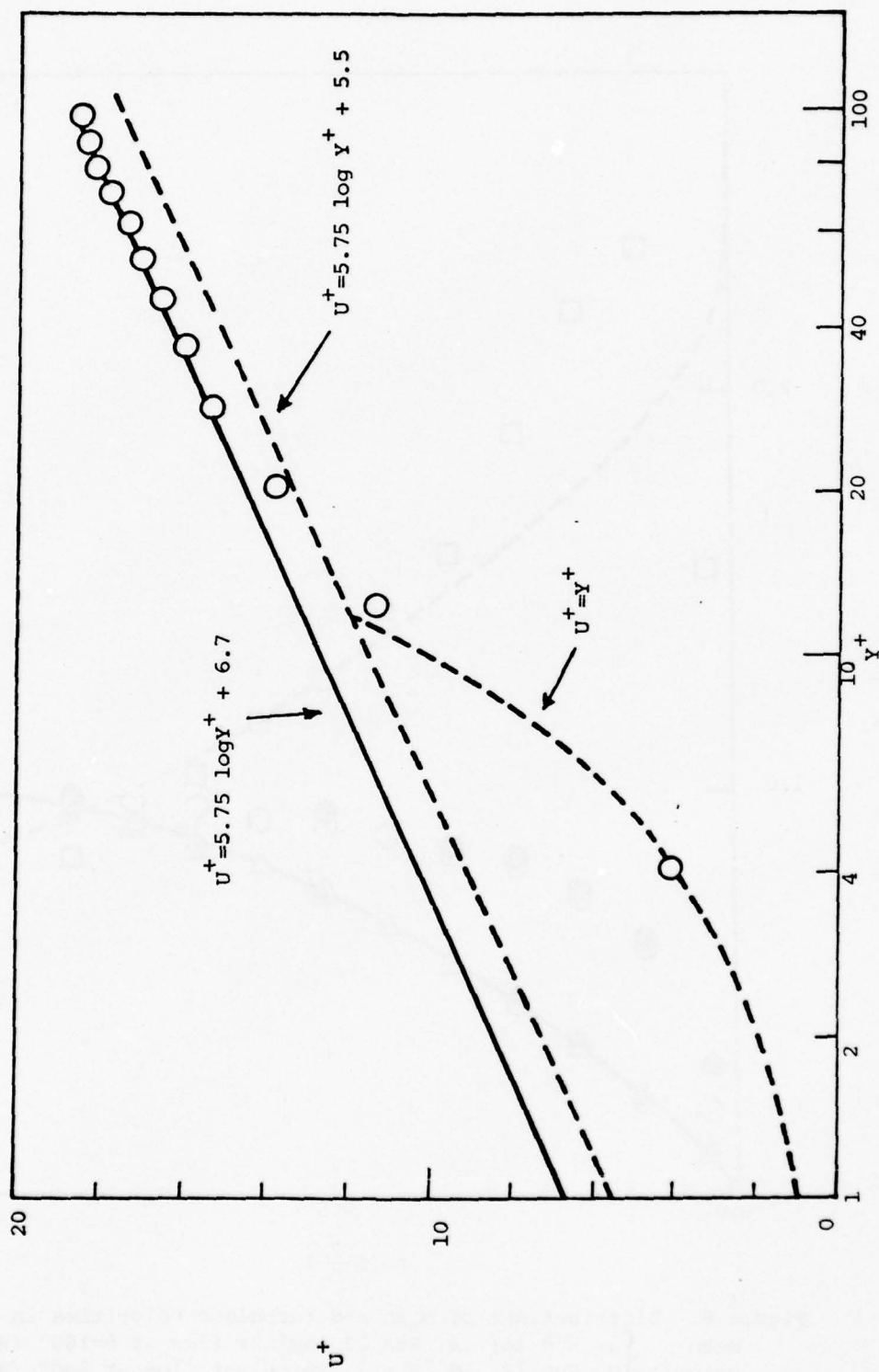


Figure 7. Velocity distribution in steady flow in wall-layer coordinates
 $\theta=0$ (Maximum slot opening)

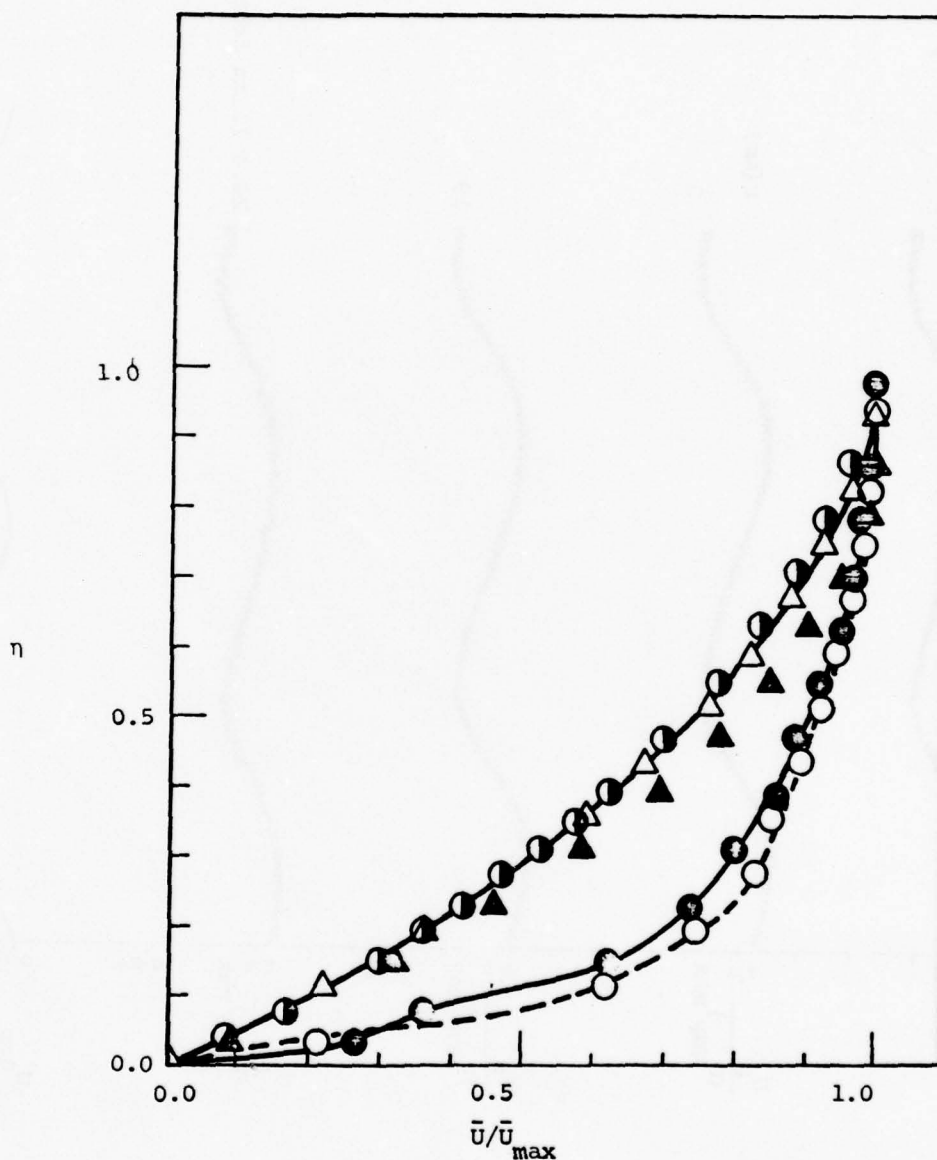


Figure 8. Distribution of the time-mean velocity across the pipe in unsteady flow.

- Δ , steady laminar flow ($\theta=180^\circ$); $-\theta-$, steady turbulent flow ($\theta=0^\circ$),
- \bullet , unsteady turbulent flow at $f=1.75$ Hz (Run 13);
- \circ , unsteady laminarized flow at $f=1.75$ Hz (Run 23),
- \blacktriangle , unsteady laminarized flow at $f=0.057$ Hz (Run 24);
- , theoretical parabolic profile for laminar flow

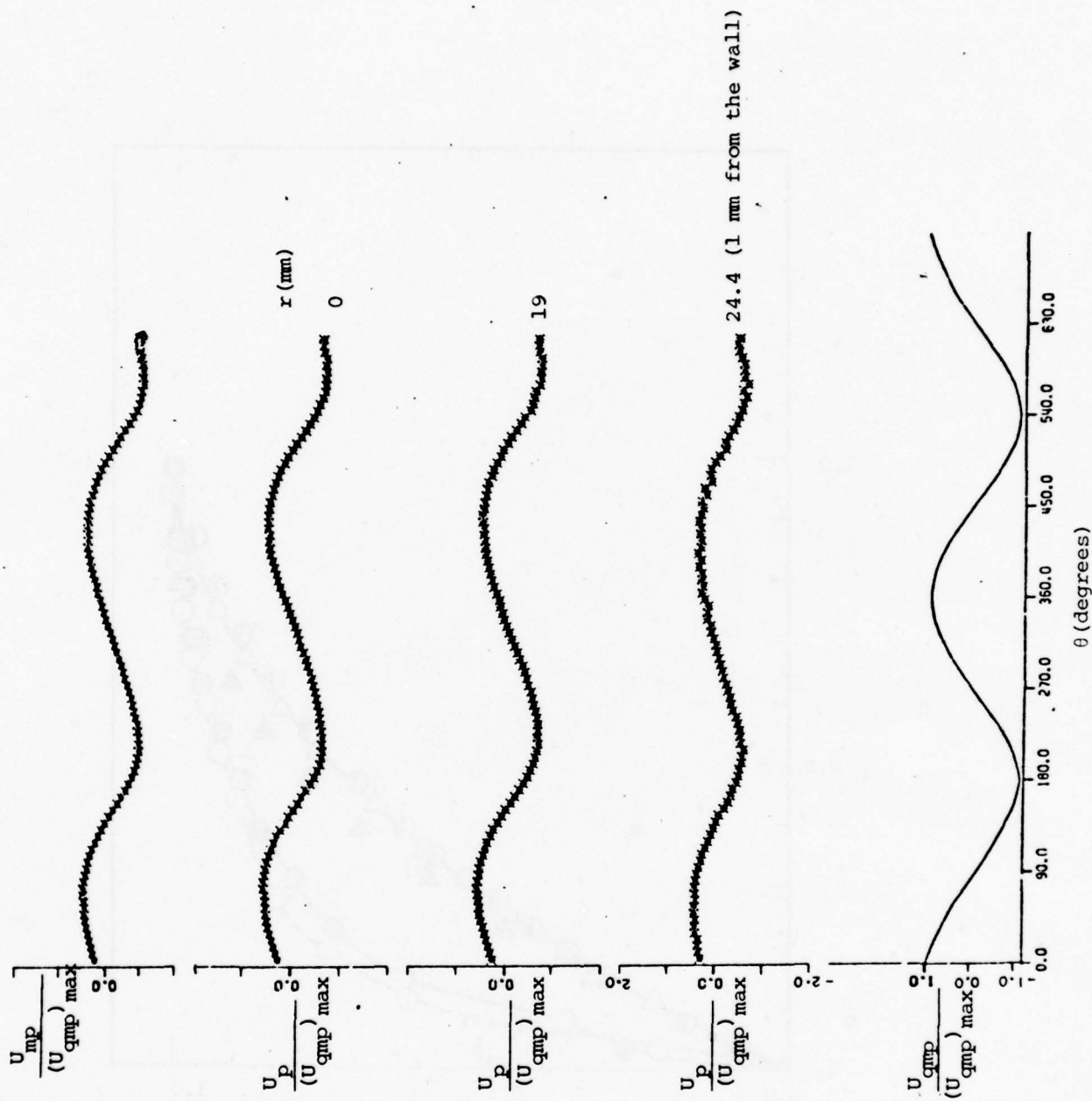


Figure 9(a). Variation of the periodic component of the velocity with phase angle (Run 13).

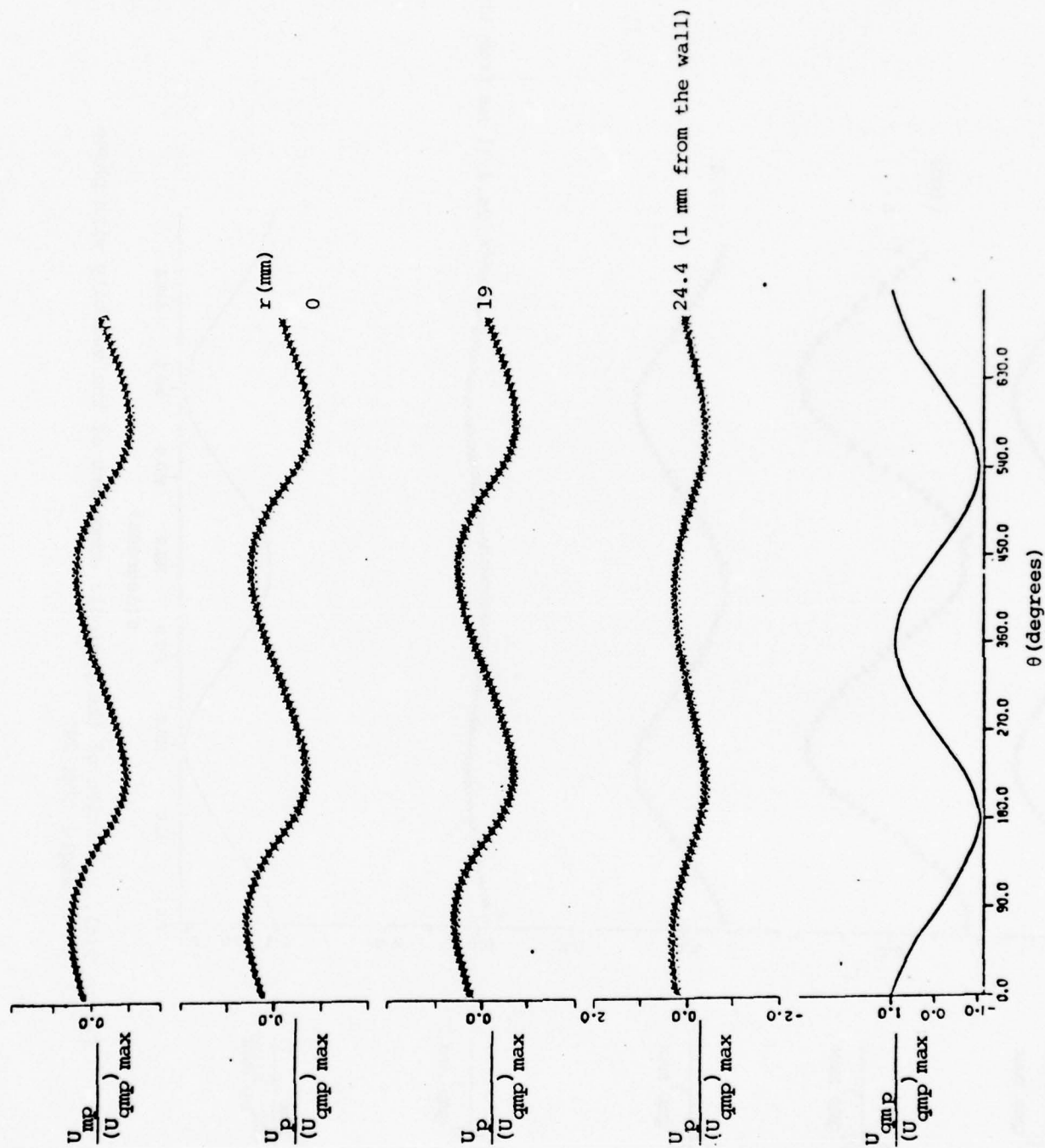


Figure 9(b). Variation of the periodic component of the velocity with phase angle (Run 23).

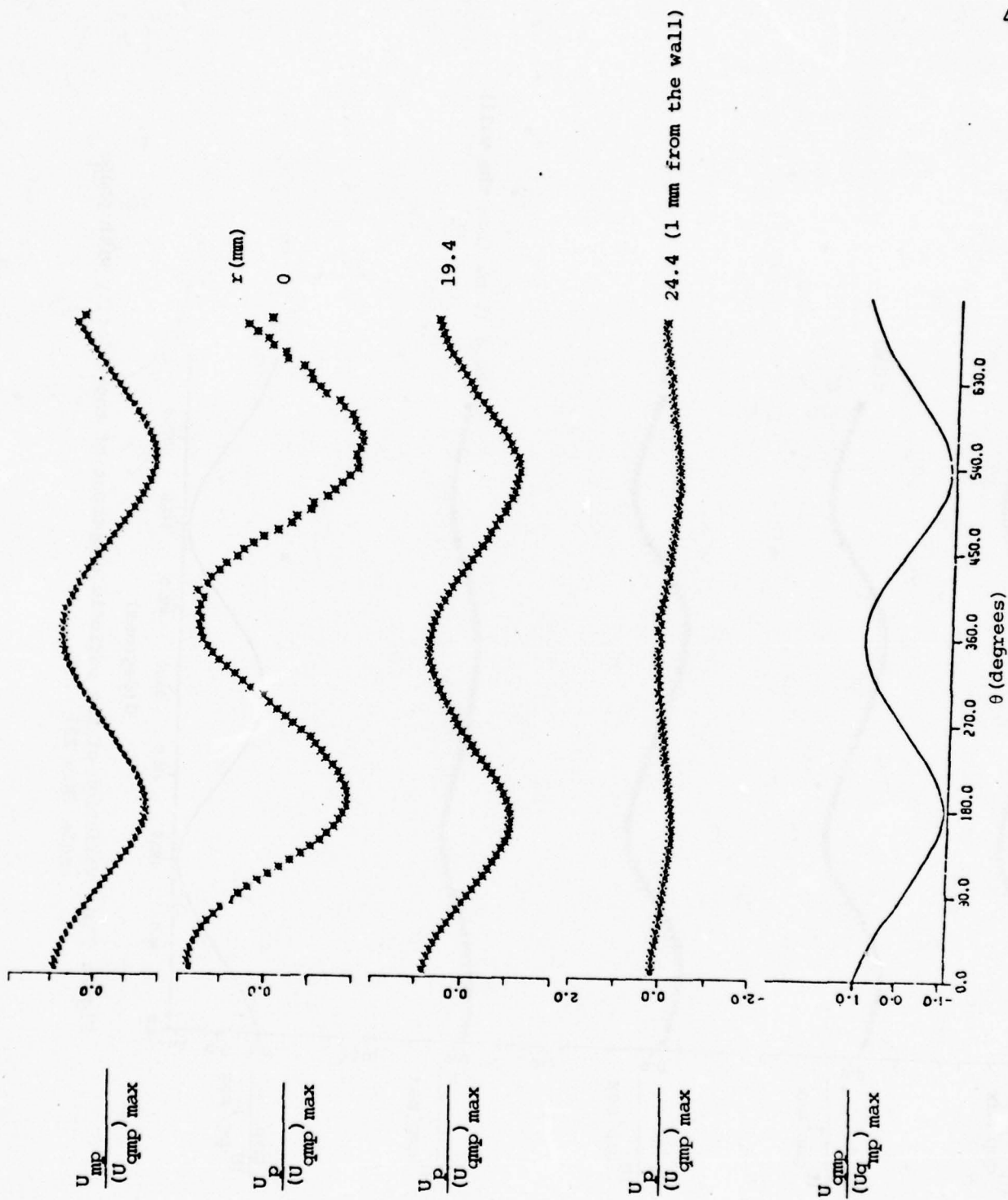


Figure 9(c). Variation of the periodic component of the velocity with phase angle (Run 24)

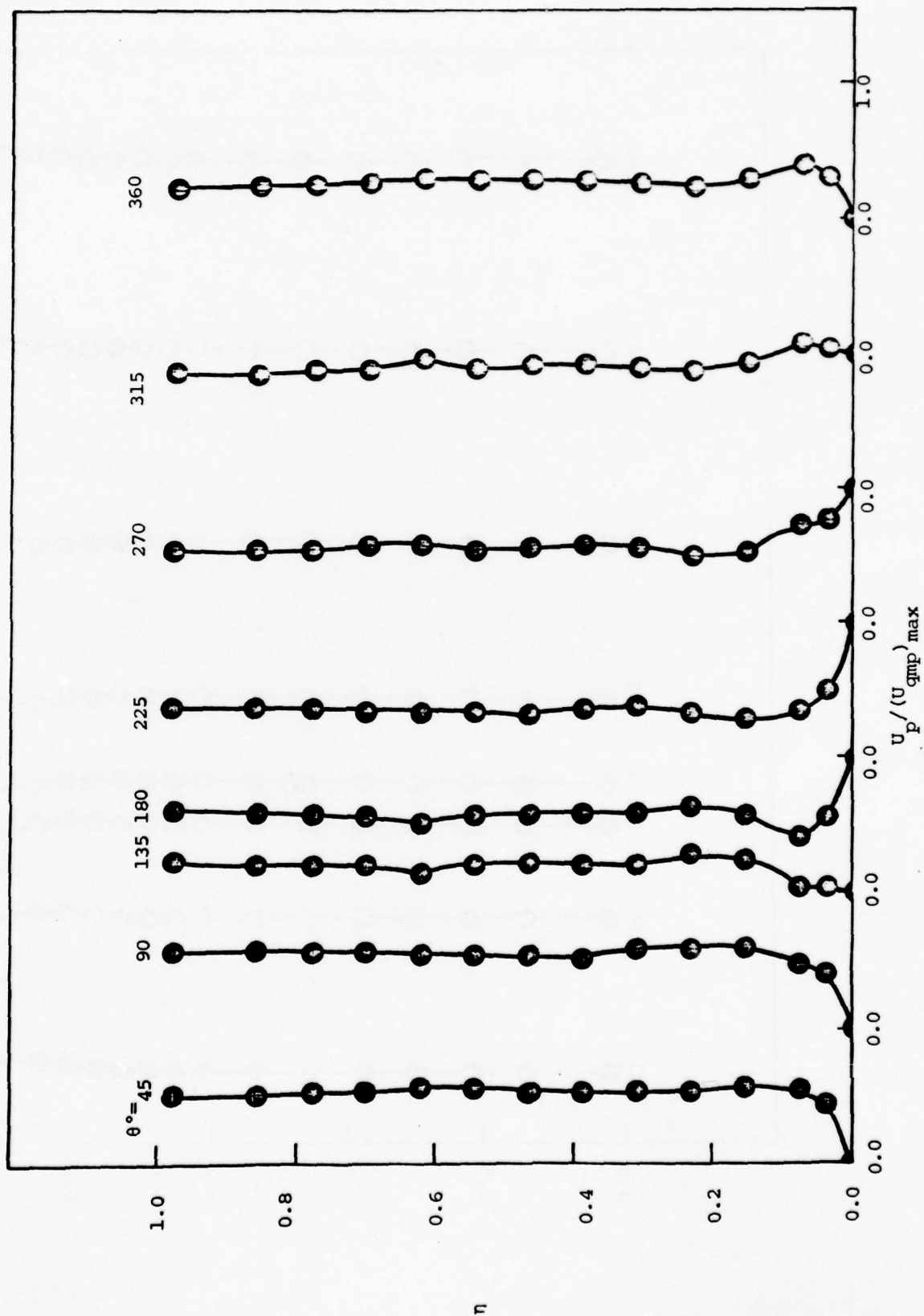


Figure 10(a) Distribution of the periodic component of the velocity across the pipe at fixed phase angle in oscillating turbulent flow; $f=1.75$ Hz (Run 13).

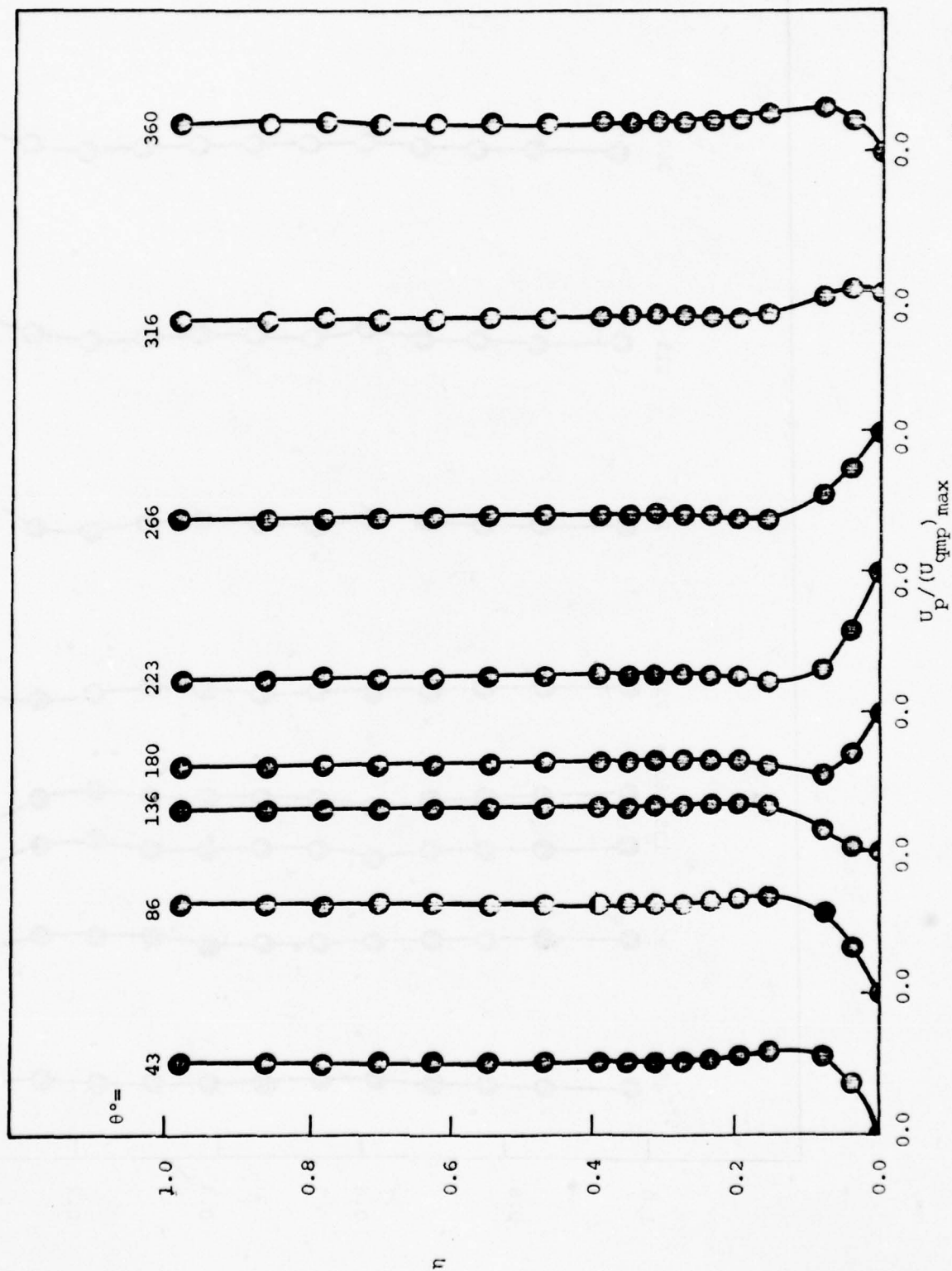


Figure 10(b). Distribution of the periodic component of the velocity across the pipe at fixed phase angle in oscillating laminar flow; $f=1.75$ Hz (Run 23)

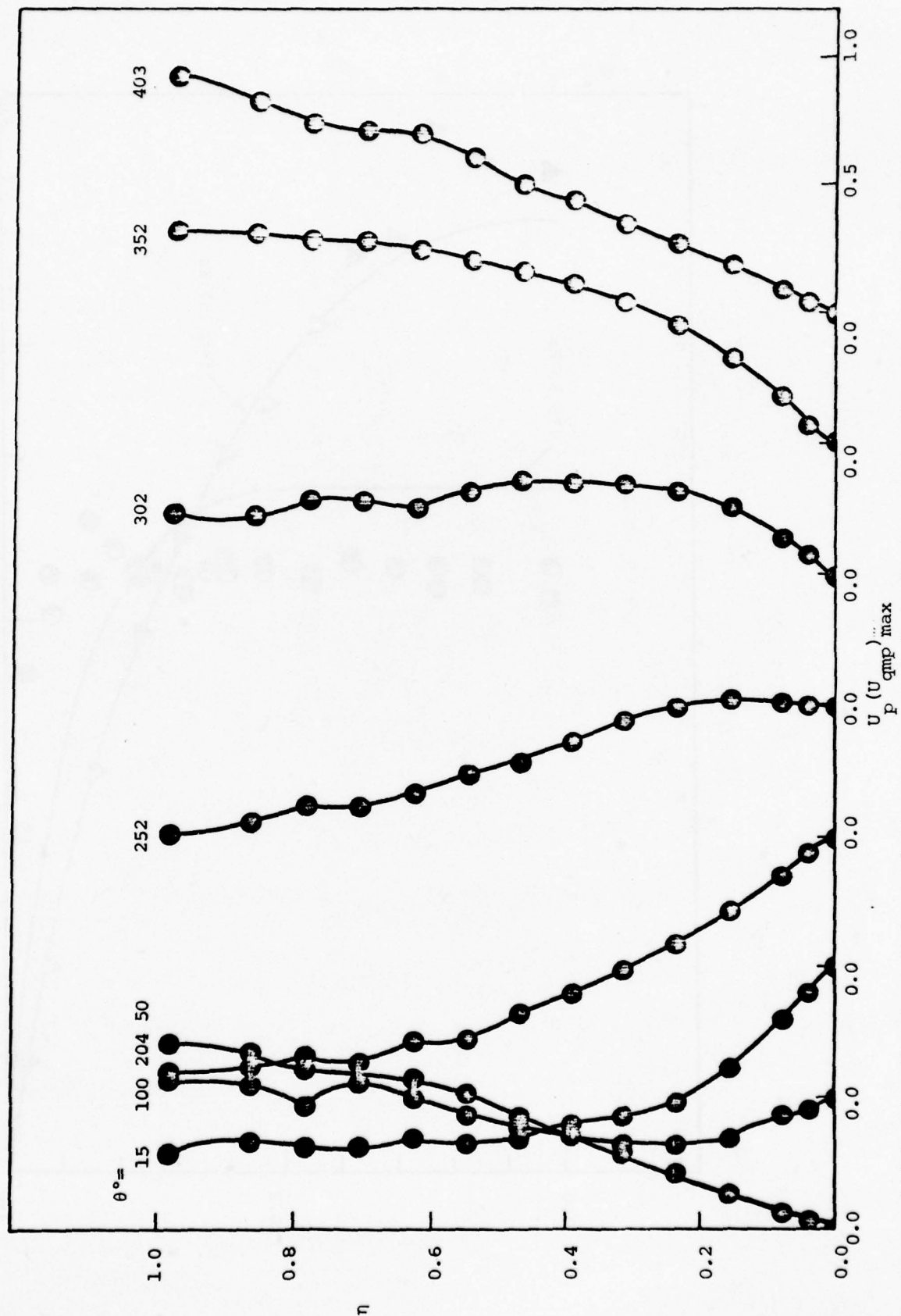


Figure 10(c). Distribution of the periodic component of the velocity across the pipe at fixed phase angle in oscillating laminar flow; $f=0.057$ Hz (Run 24)

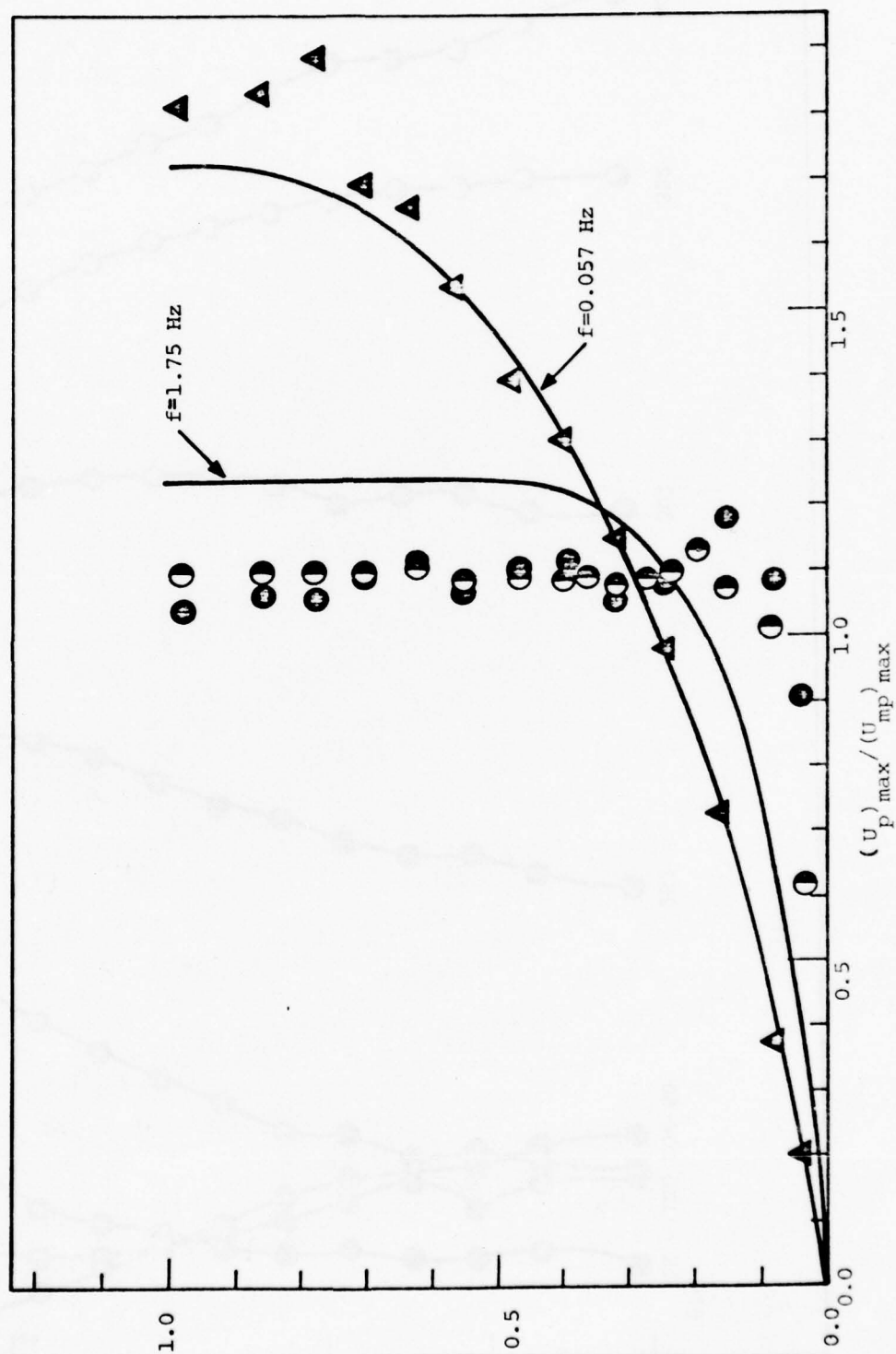


Figure 11. Distribution of the amplitude of the periodic component of velocity across the pipe. \circ , Run 13; \bullet , Run 23; \triangle , Run 24; —, Laminar theory from Uchida (1956) ($f=1.75 \text{ Hz}$); ---, Laminar theory from Uchida (1956) ($f=0.057 \text{ Hz}$).

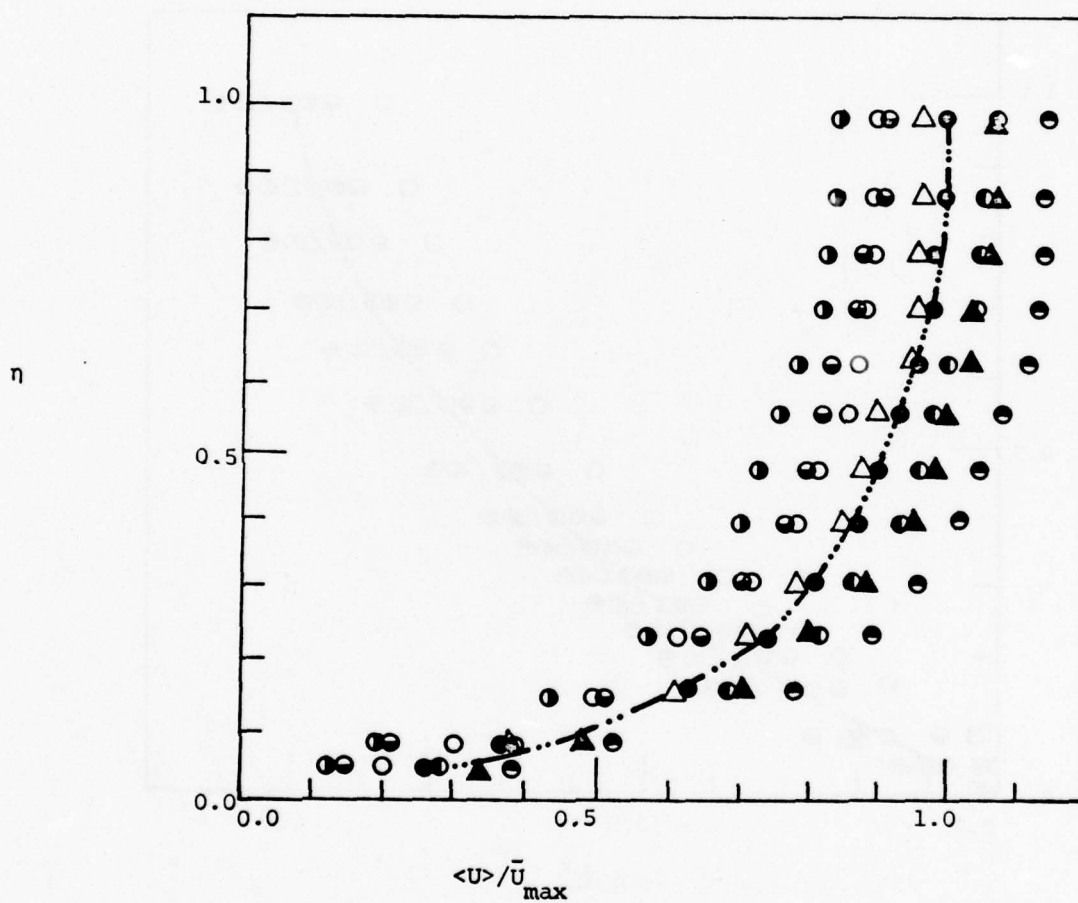


Figure 12(a). Distribution of the ensemble average velocity across the pipe in oscillatory turbulent flow, $f=1.75$ Hz (Run 13)

symbol, phase angle θ (degrees): \bullet , 45° ; \circ , 135° ; \ominus , 180° ; \oplus , 225° ; \circ , 270° ; Δ , 315° ; \blacktriangle , 360° ; $-\bullet-$, time-mean velocity

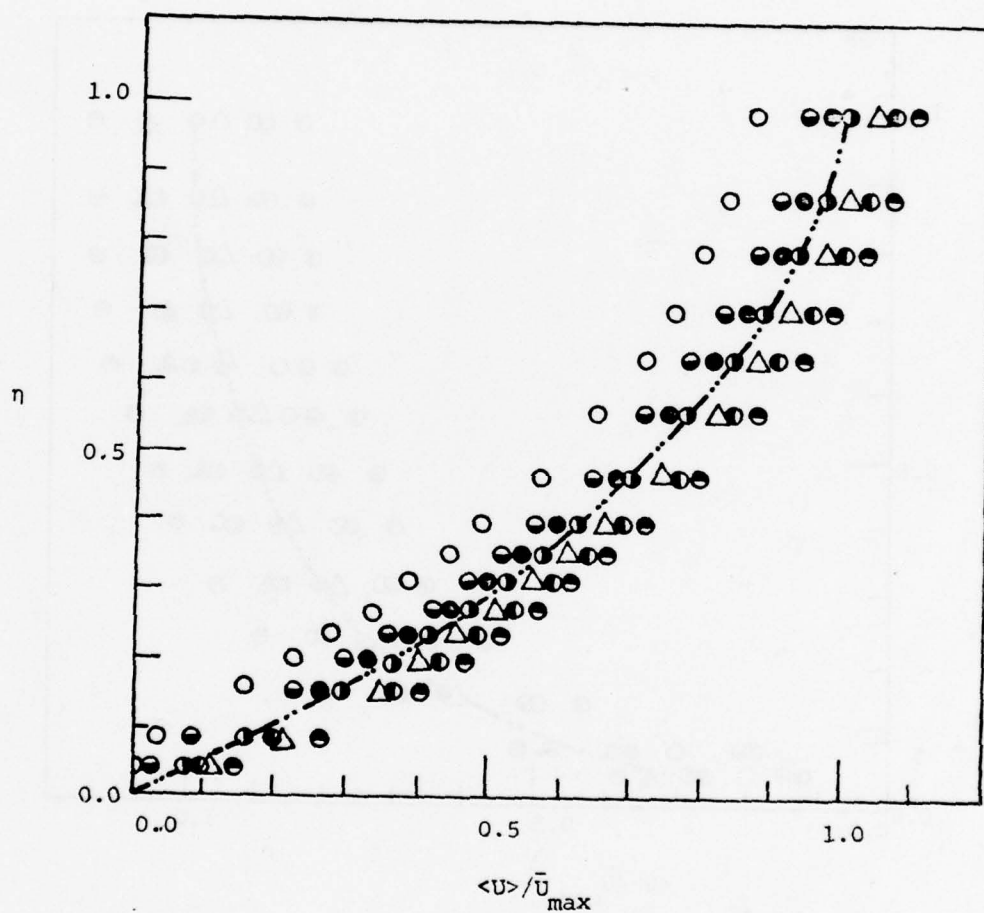


Figure 12(b). Distribution of the ensemble average velocity across the pipe in oscillatory laminarized flow, $f=1.75$ Hz (Run 23)
 symbol, phase angle θ (degrees): \circ , 45° ; \bullet , 135° ; \circ , 180° ;
 \bullet , 225° ; \bullet , 315° ; Δ , 360° ; $-\cdots-\circ-\cdots-$; time-mean velocity

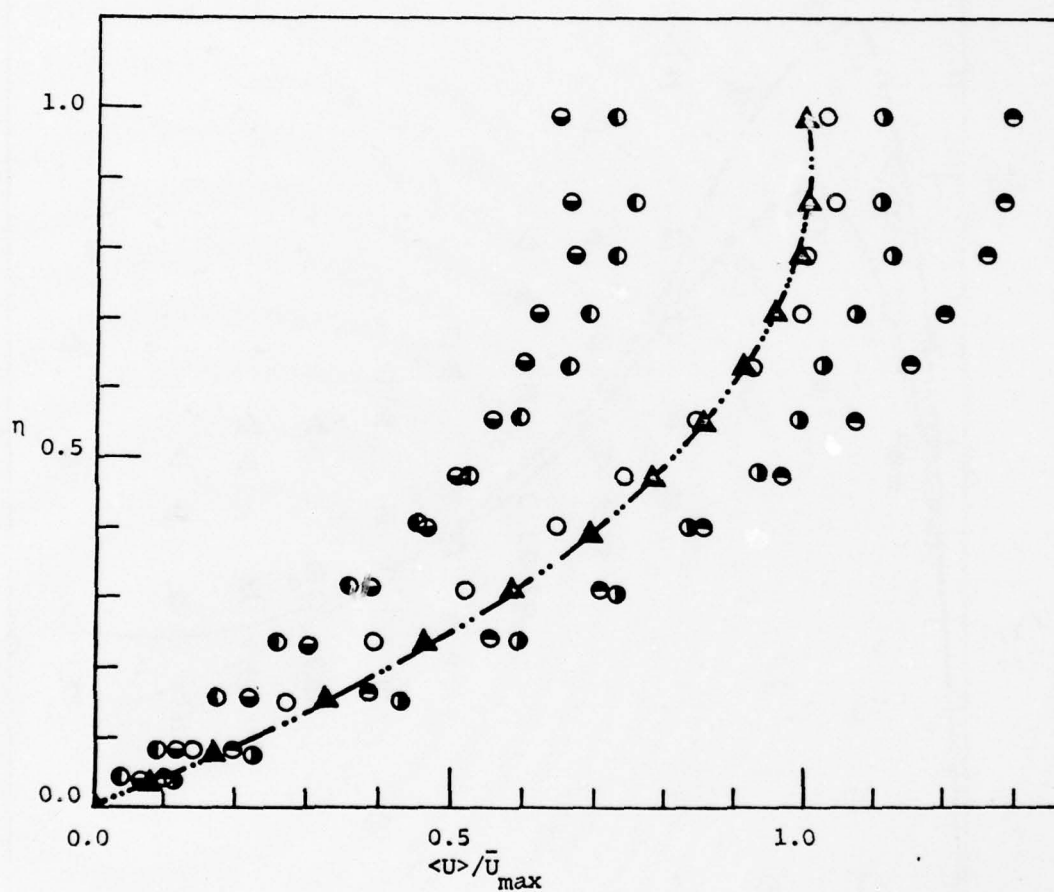


Figure 12(c). Distribution of the ensemble average velocity across the pipe in oscillatory laminarized flow, $f=0.057$ Hz (Run 24).
 symbol, phase angle θ (degrees) \circ , 50° ; \bullet , 100° ; \bullet , 150° ;
 \bullet , 200° ; \circ , 300° ; $-\cdots\triangle\cdots$, time-mean velocity

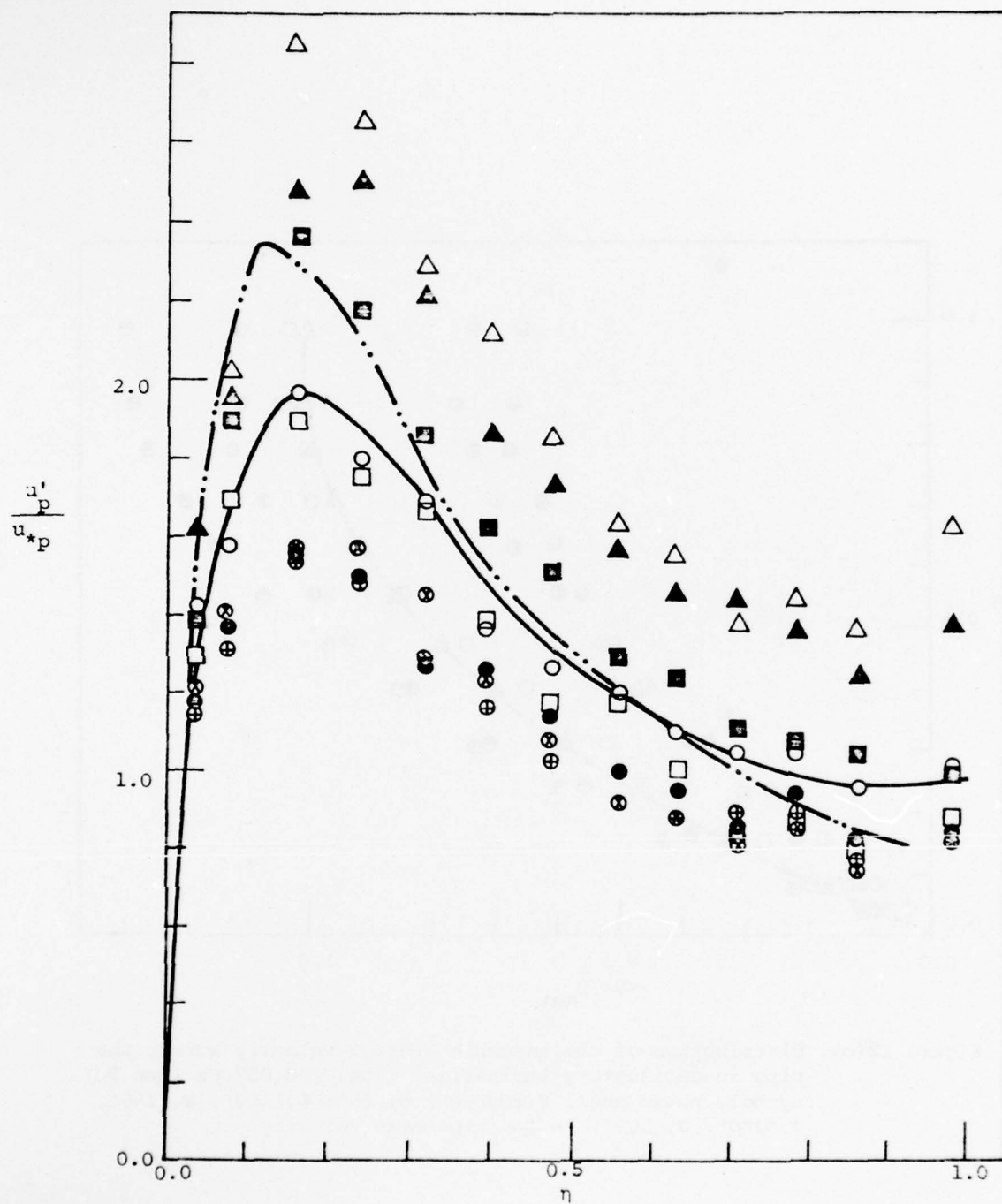


Figure 13. Distribution of the turbulent intensity across the pipe in run 13 ($f=1.75$ Hz).
 —, time averaged turbulent intensity u'/\bar{u}_* in oscillatory flow;
 — · —, u'/u_* in quasi-steady flow at $\theta=0^\circ$
 Data points denote the ensemble average turbulent intensity u'/u_{*p}
 symbol, phase angle: \circ , 6° ; \odot , 45° ; \bullet , 90° ; \circ , 135° ; \blacktriangle , 180° ; \triangle , 225° ; \blacksquare , 270° ; \square , 315°

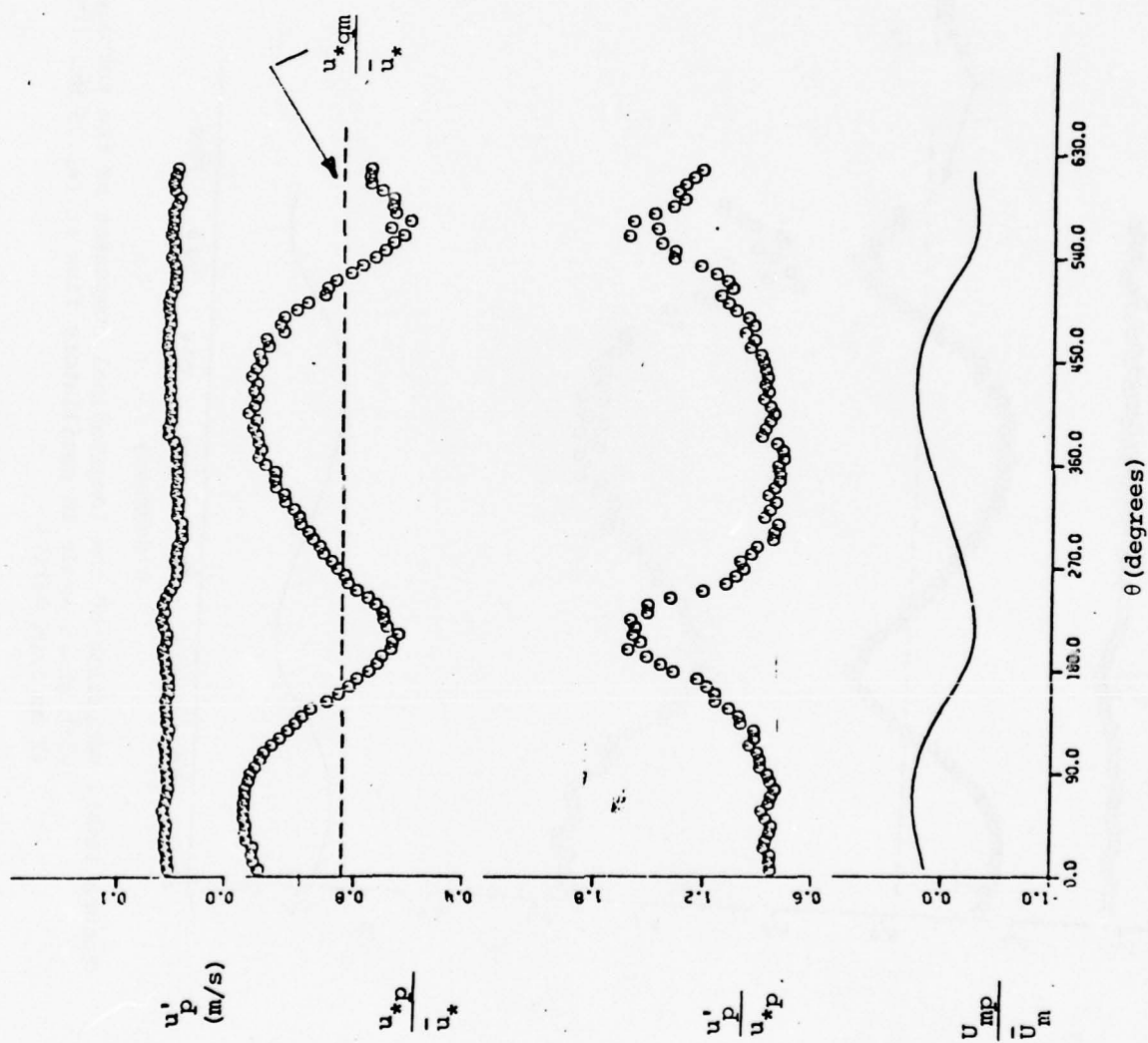


Figure 14 (a). Variation of the longitudinal component of the turbulent velocity with phase angle in oscillatory flow at $f=1.75$ Hz ($r=0$).

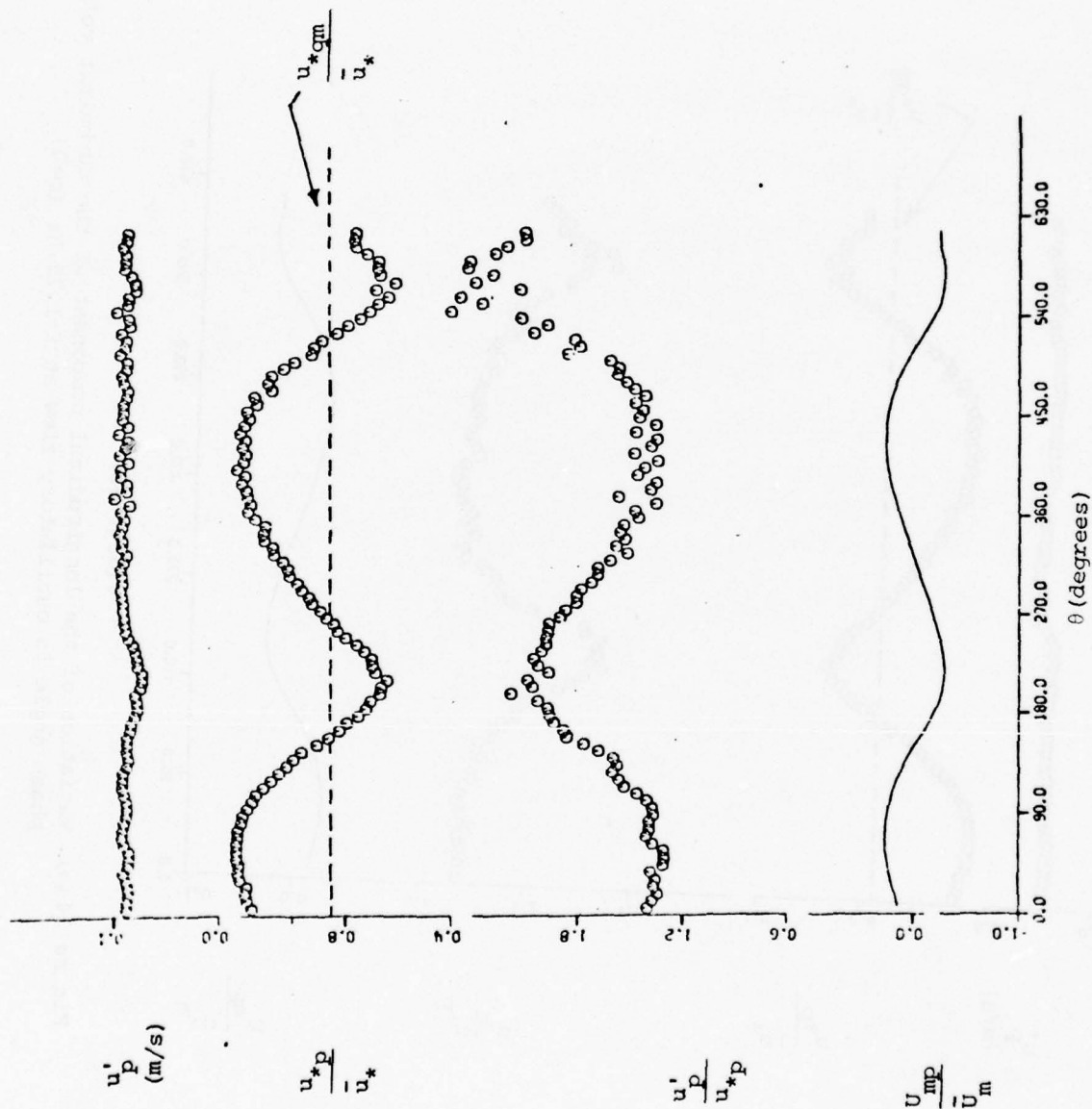


Figure 14(b). Variation of the longitudinal component of the turbulent velocity with phase angle in oscillatory flow at $f=1.75$ Hz. $[r=23.4$ mm (2 mm from wall)]

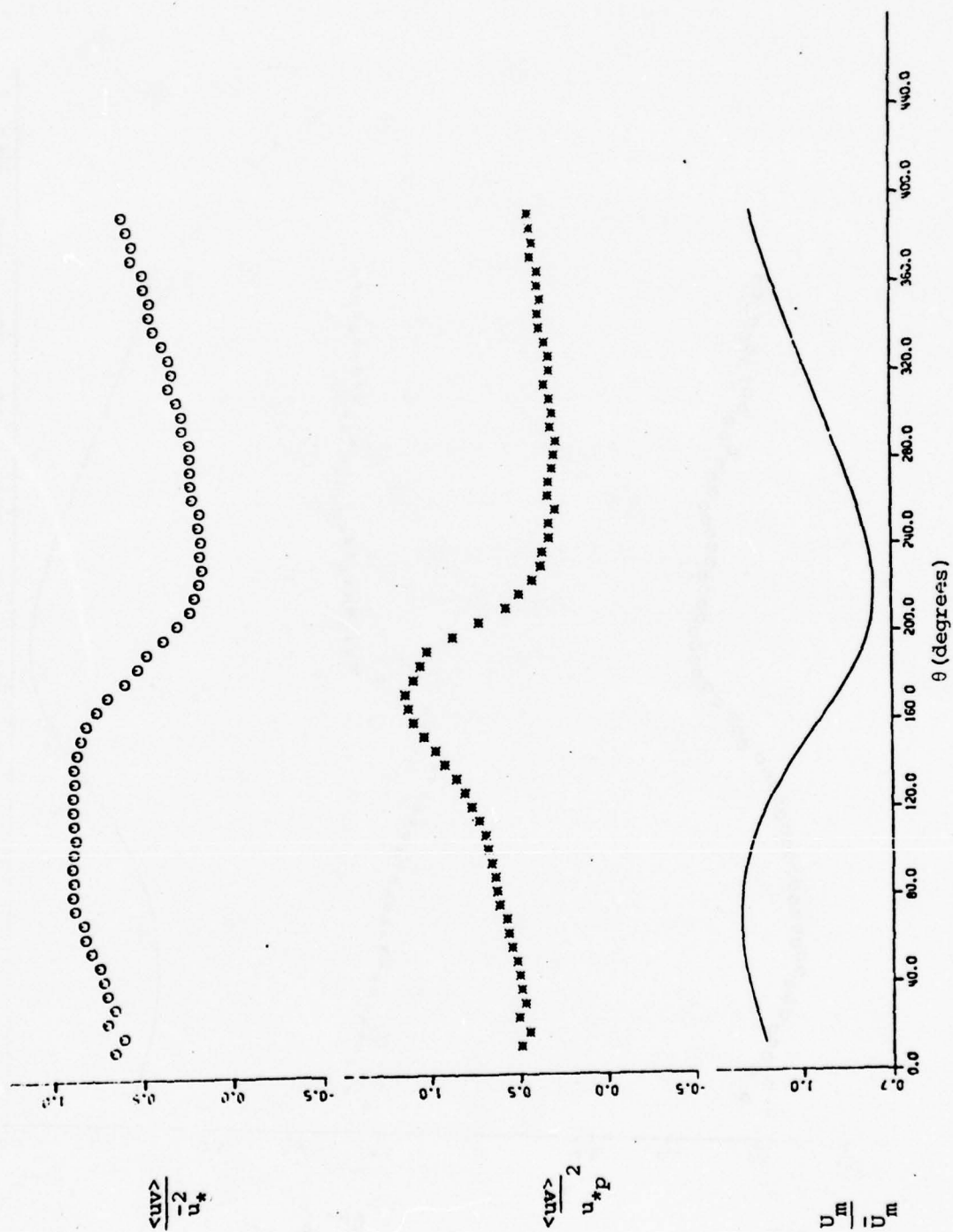


Figure 15(a). Variation of the Reynolds shear stress with phase angle in oscillatory flow. distance: 1 mm from the wall; $f=1.75$ Hz (Run 13)

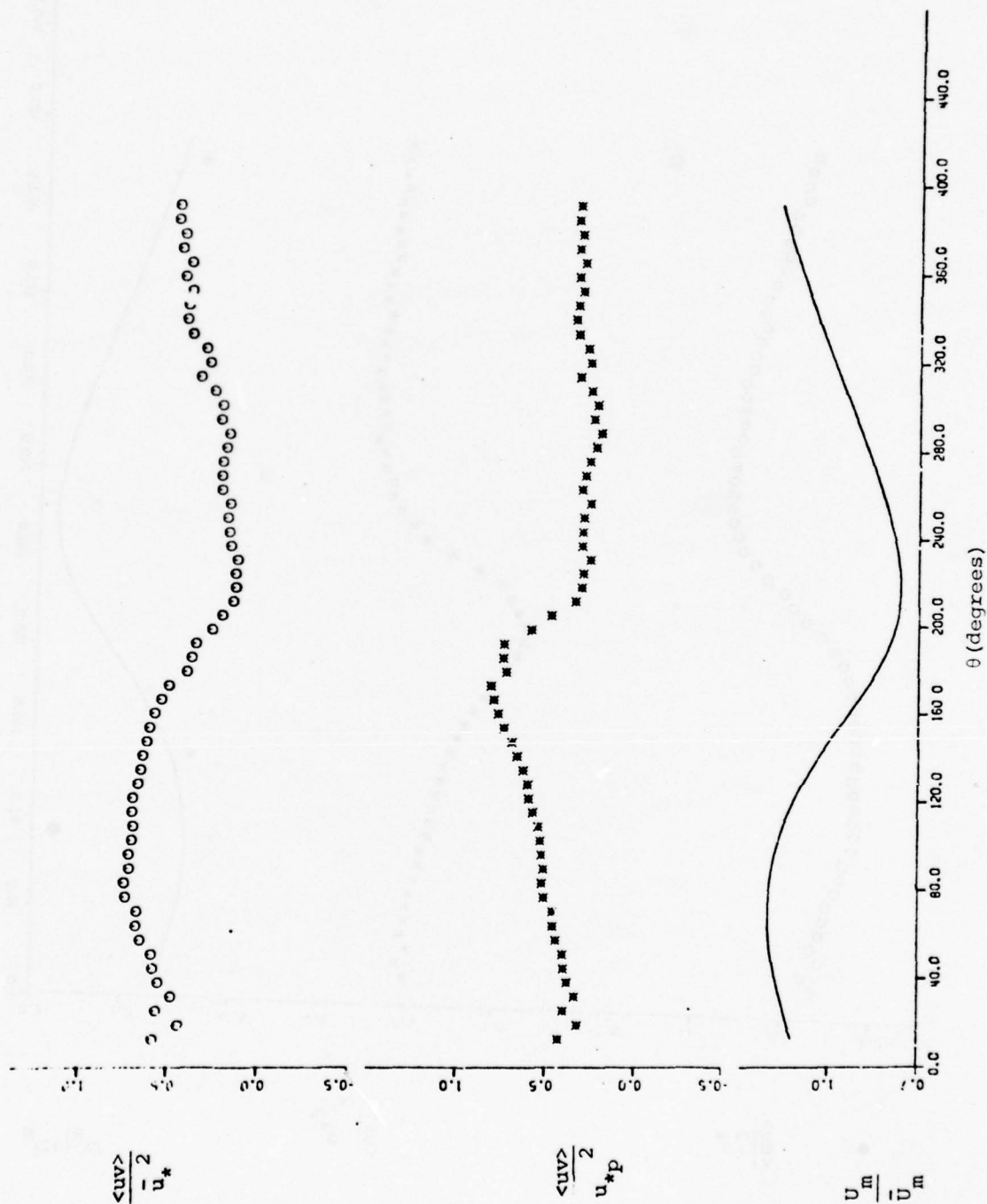


Figure 15(b). Variation of the Reynolds shear stress with phase angle in oscillatory flow. distance: 2 mm from the wall; $f=1.75$ Hz (Run 13)

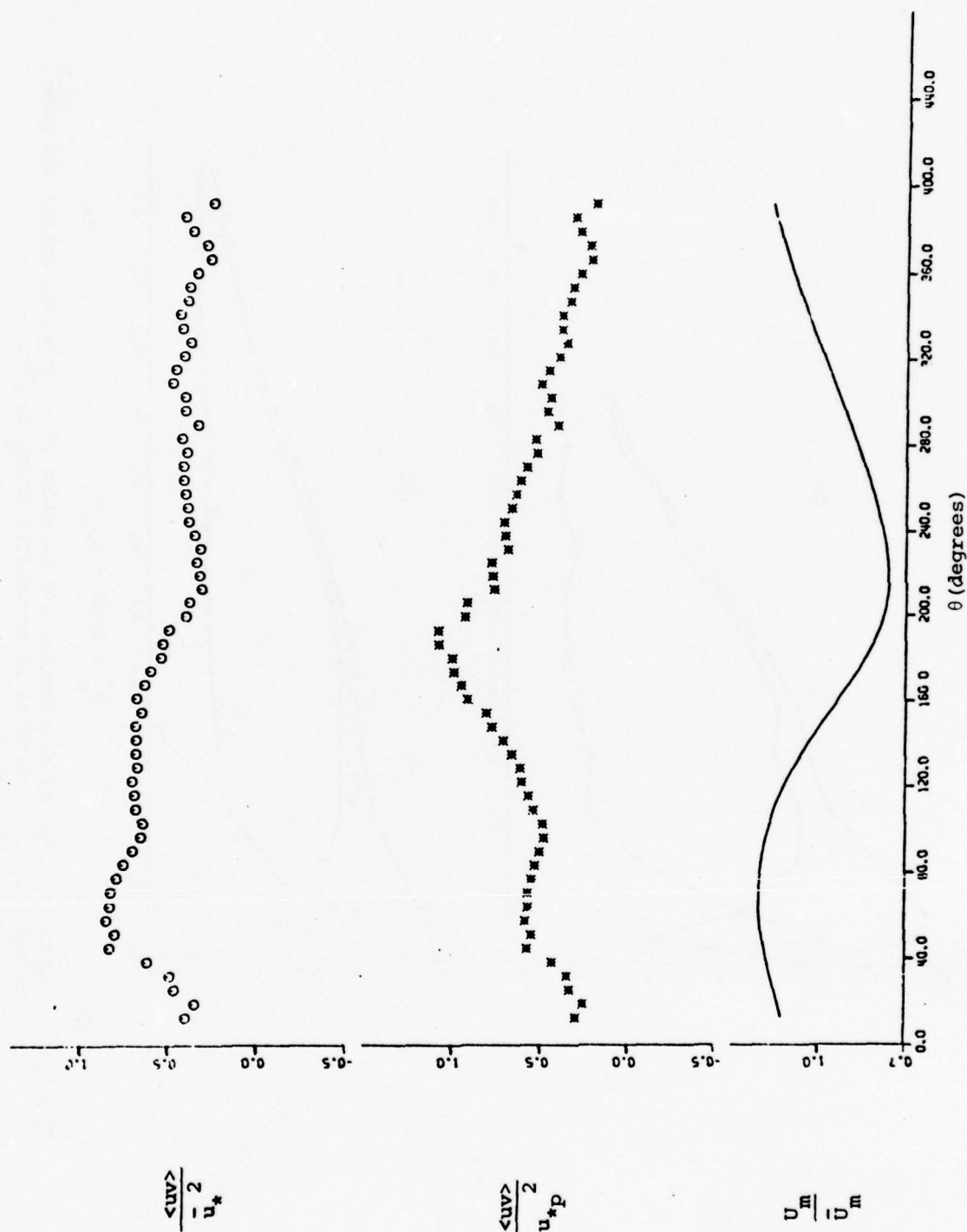


Figure 15(c). Time variation of the Reynolds shear stress with phase angle in oscillatory flow. distance: 10 mm from the wall; $f=1.75$ Hz (Run 13).

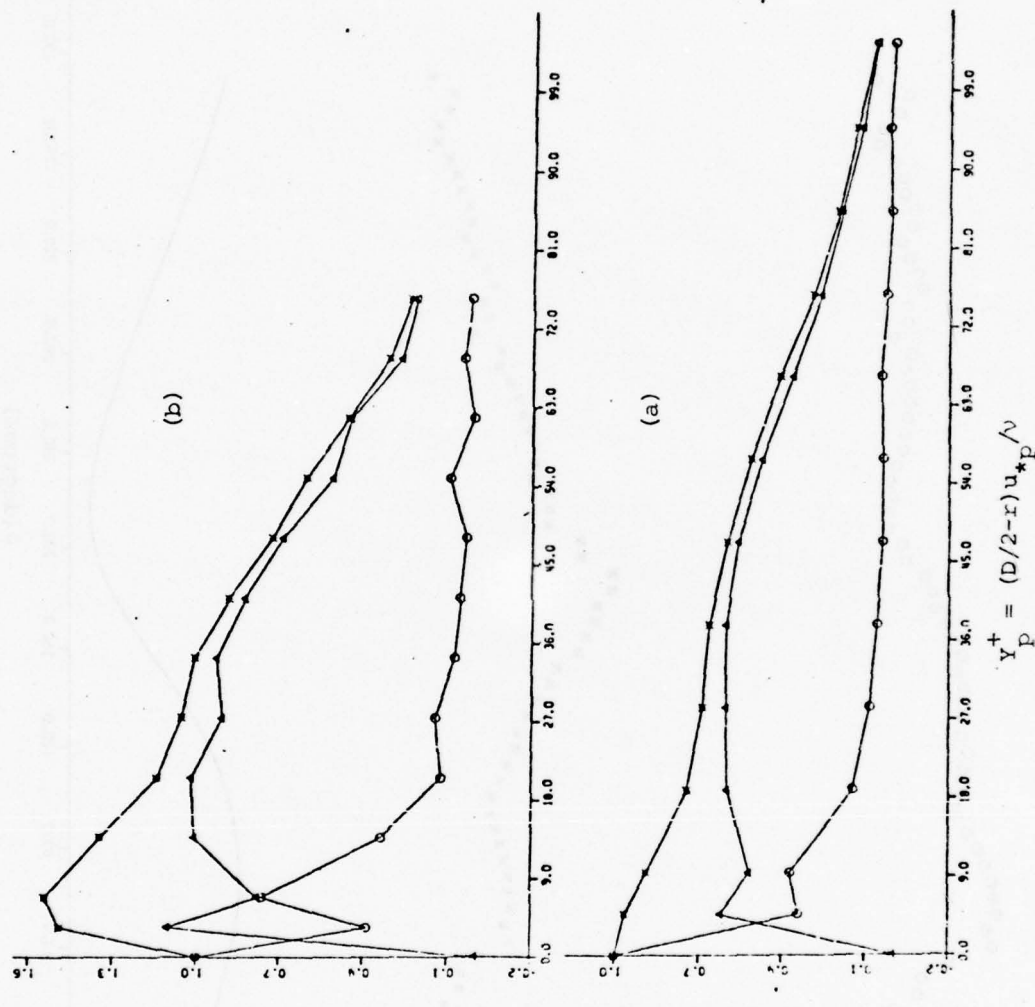


Figure 16. Distribution of total, laminar and Reynolds shear stresses across the pipe in wall-layer coordinates at prescribed phase angles.
 (a) $\theta = 77^\circ$ (b) $\theta = 160^\circ$
 —●—, total shear stress; —○—, laminar shear stress; —▲—, Reynolds shear stress. The stresses are normalized with respect to the wall shear stress at the corresponding phase angle.

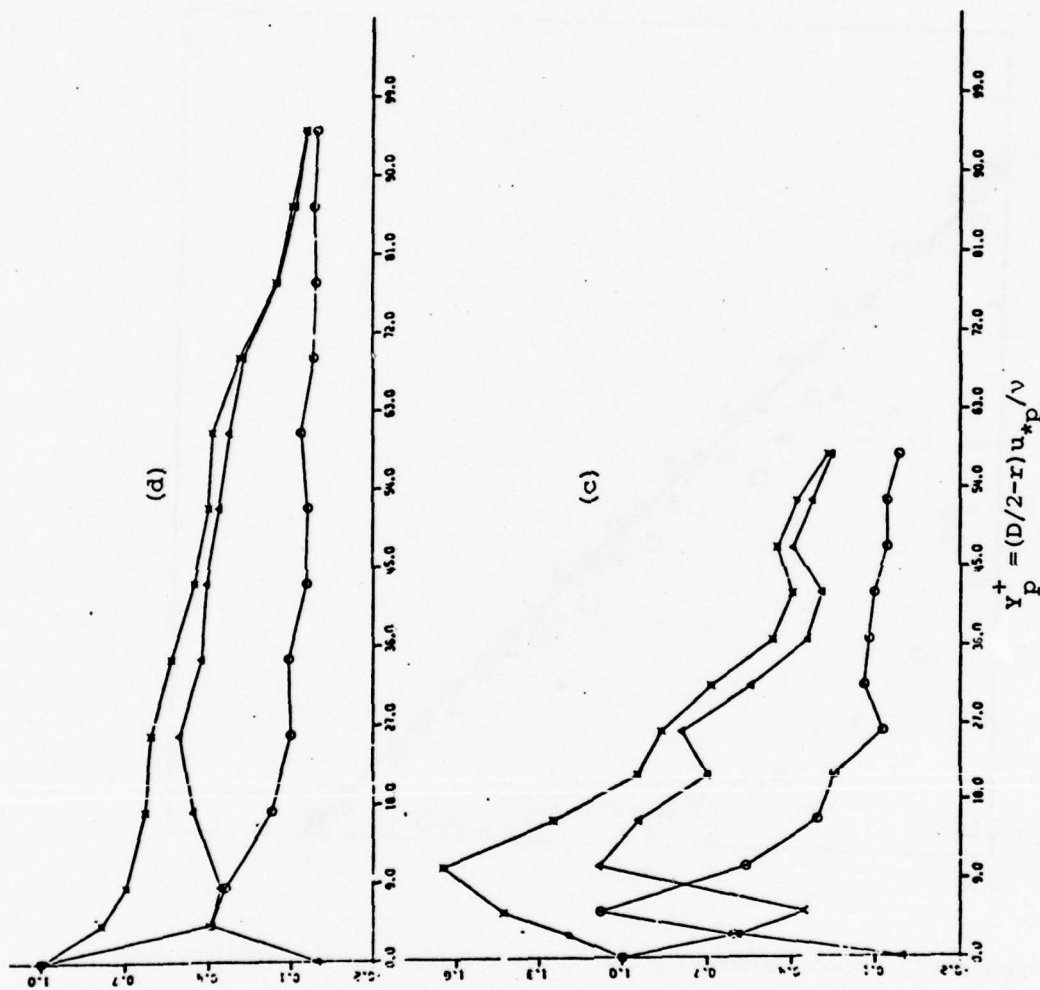


Figure 16. Distribution of total, laminar and Reynolds shear stresses across the pipe in wall-layer coordinates at prescribed phase angles
 (c) $\theta=212^\circ$ (d) $\theta=340^\circ$
 —, total shear stress; —○—, laminar shear stress; —△—, Reynolds shear stress. The stresses are normalized with respect to the wall shear stress at the corresponding phase angle

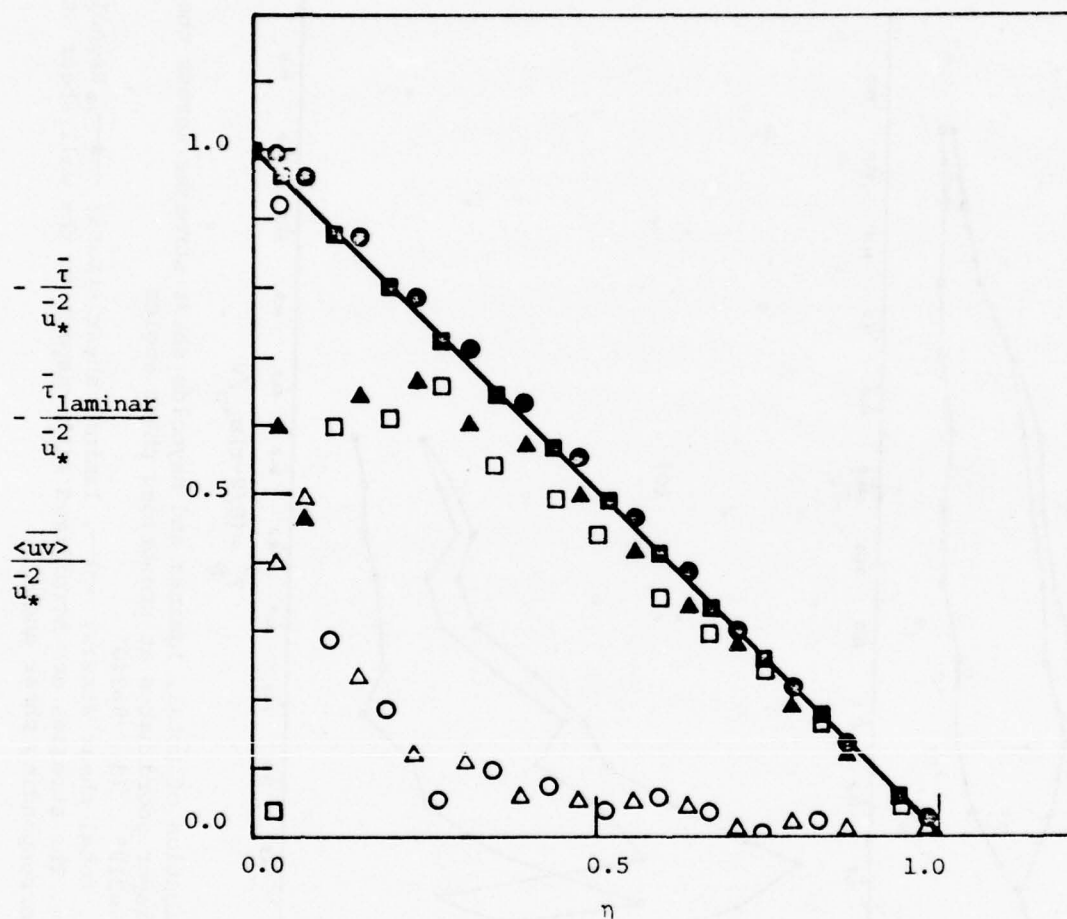


Figure 17. Distribution of the time-averaged total, laminar and Reynolds shear stresses across the pipe.

Steady turbulent flow at a Reynolds number of 2870 ($\theta=0^\circ$)

■, total shear stress; □, Reynolds shear stress;
○, laminar shear stress

Unsteady turbulent flow, $f=1.75$ Hz (Run 13)

●, total shear stress; ▲, Reynolds shear stress;
△, laminar shear stress

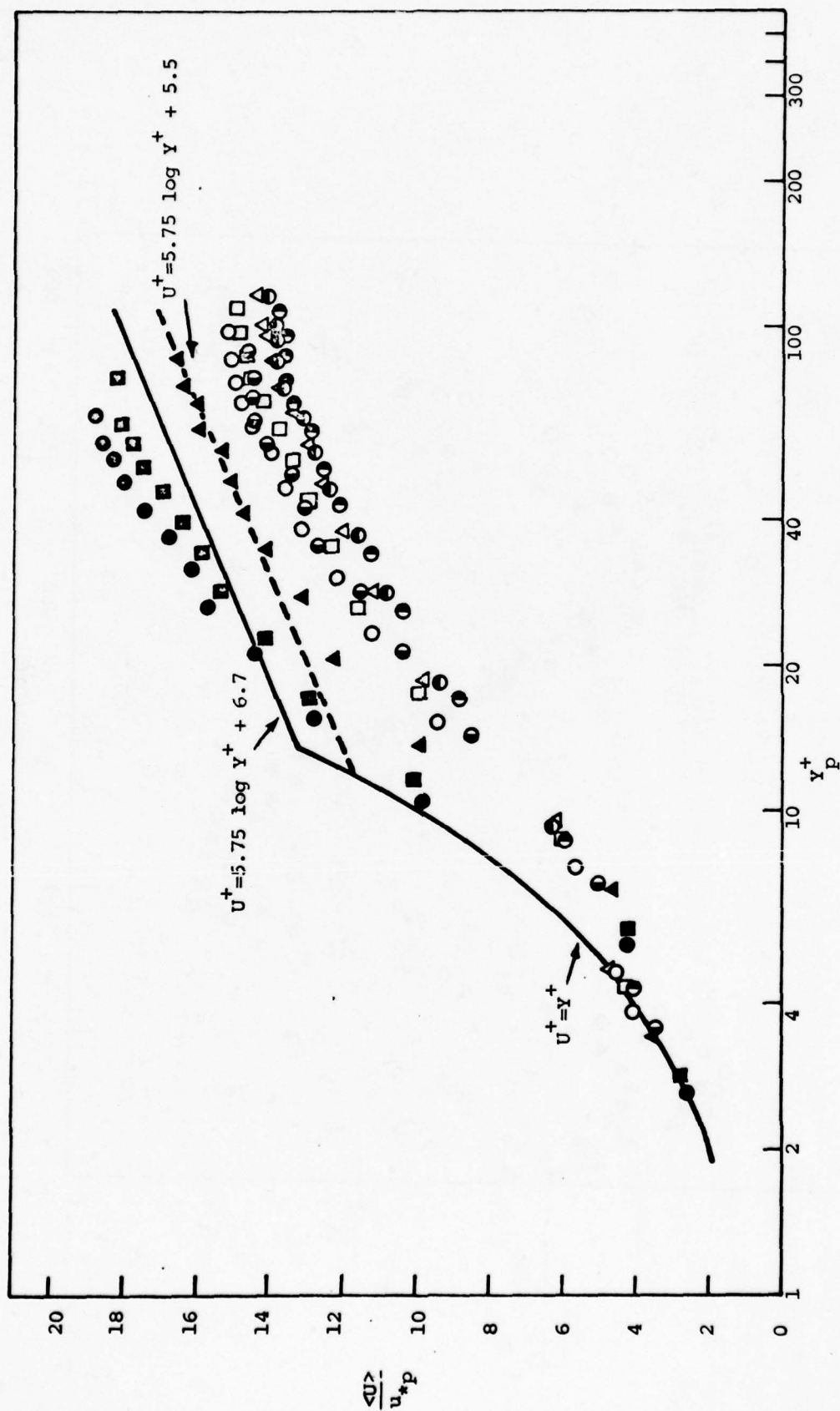


Figure 18. Velocity distribution in unsteady flow in wall-layer coordinates.
 symbol, phase angle θ (degrees): Δ , 77°; \square , 115°; \blacksquare , 160°; \bullet , 185°;
 \circ , 212°; \odot , 276°; \ominus , time-mean distribution \bar{U}/u_* vs $(D/2-r)u_*/\nu$; \circ , 340°;
 \bullet , 385°; —, steady flow ($\theta=0^\circ$); --- universal log law

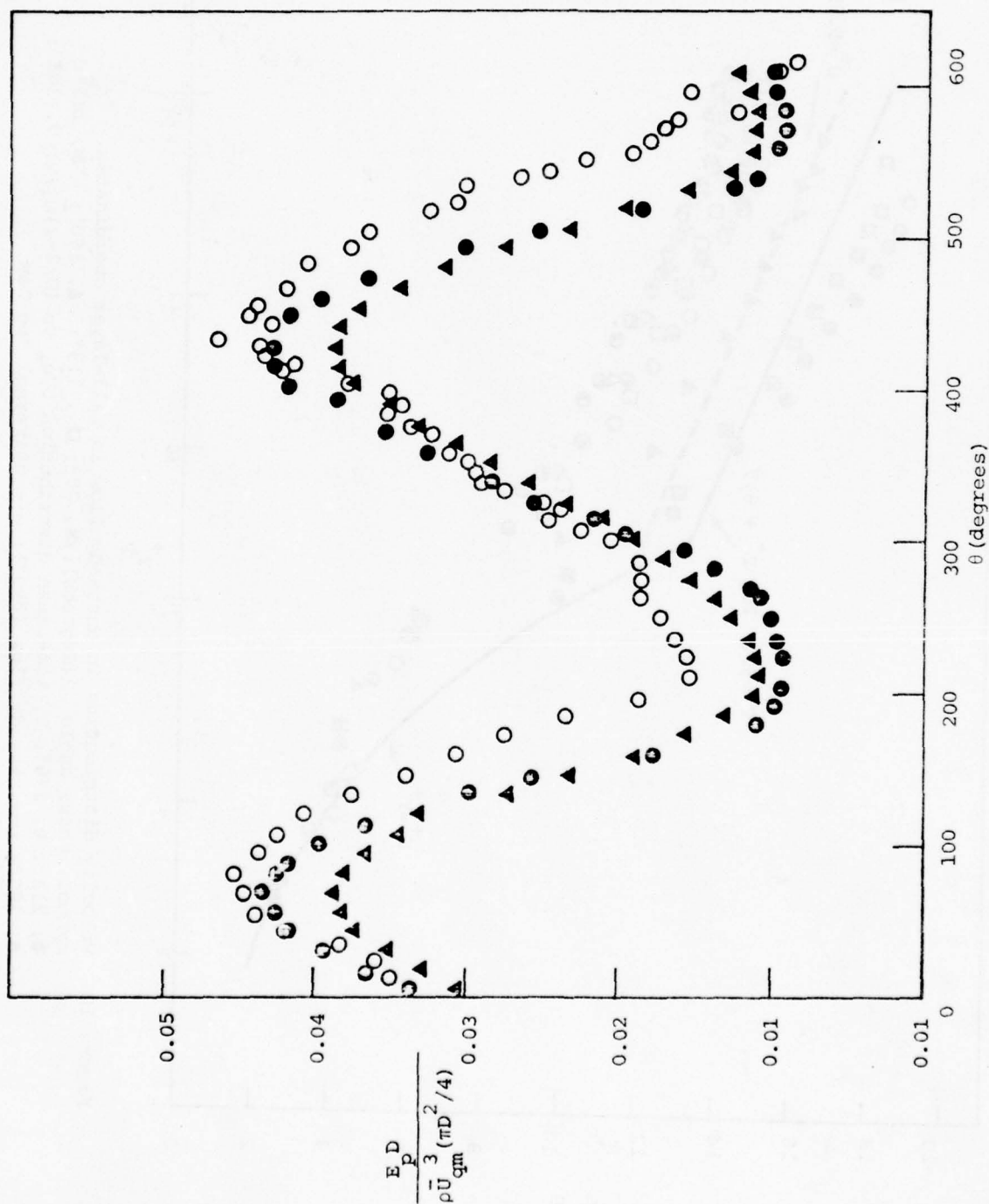
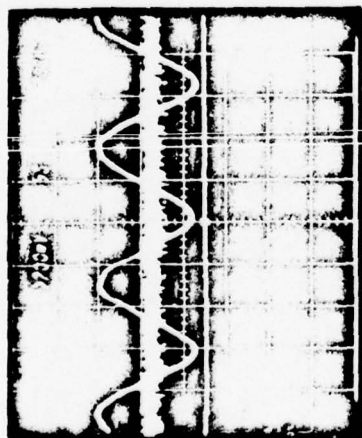
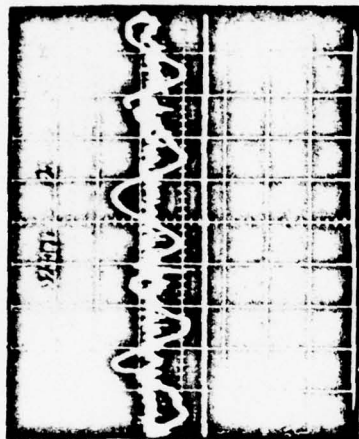


Figure 19. Variation of the rate of shear work with the phase angle.
 O, data from unsteady turbulent flow, $f=1.75$ Hz (Run 13); ▲, based on quasi-steady Blasius relation, $\lambda = 0.3165 Re^{-1/4}$; ●, based on quasi-steady pressure drop measurements in actual transitional flow



(a)

$f=0.047$ Hz



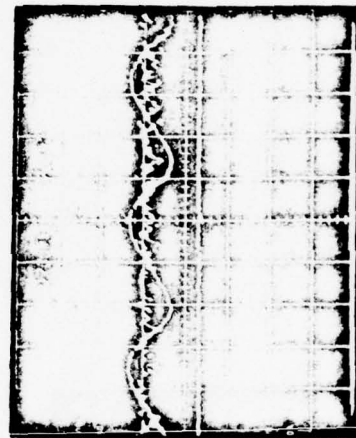
(b)

$f=0.228$ Hz



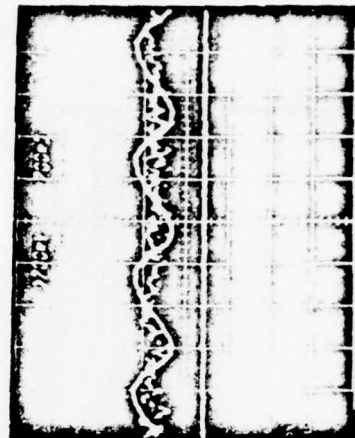
(c)

$f=0.926$ Hz



(d)

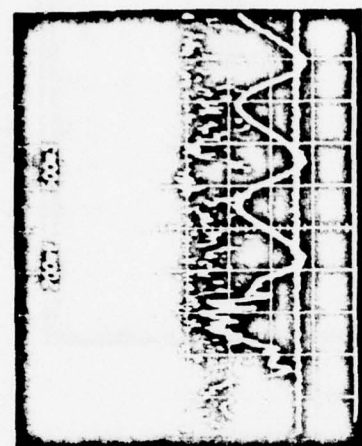
$f=1.37$ Hz



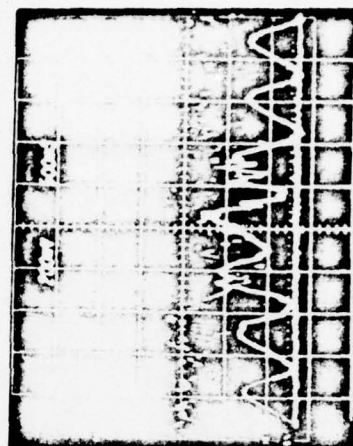
(e)

$f=1.75$ Hz

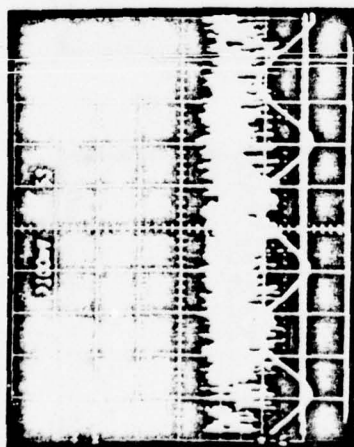
Figure 20. Oscilloscope traces of velocity signals from LDA from experiment series 2. $r=0$



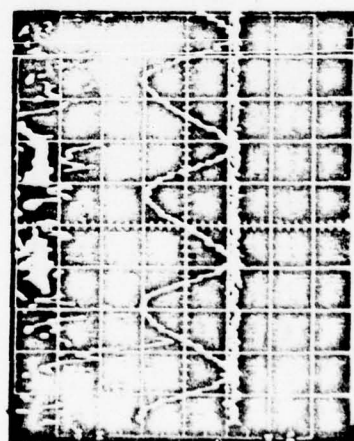
(a)
f=0.047 Hz



(b)
f=0.926 Hz



(c)
f=1.37 Hz



(d)
f=1.75 Hz

Figure 20. Oscilloscope traces of velocity signals from LDA from experiment series 2. r=18.4 mm.

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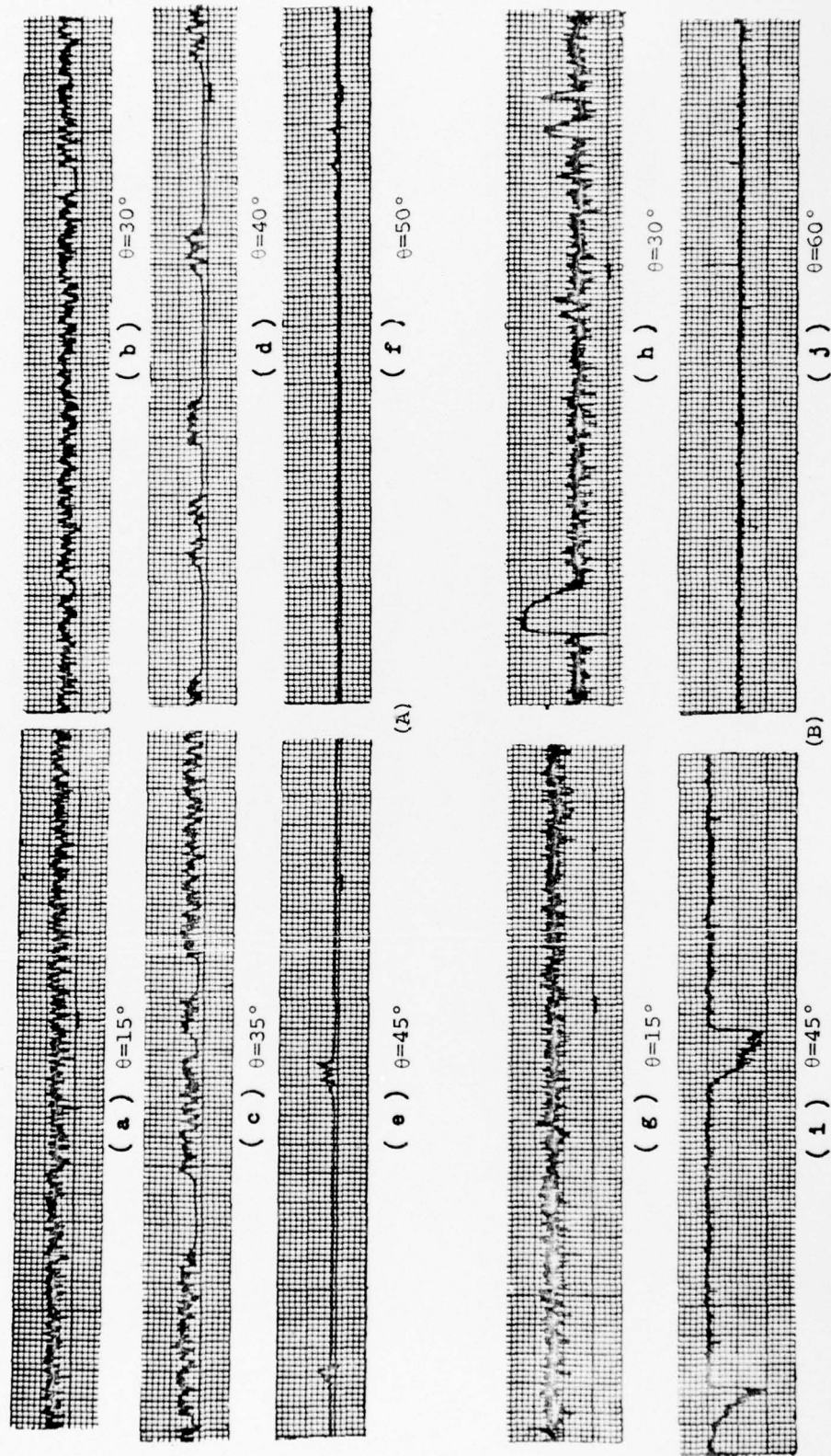


Figure 21. Typical strip chart records of the LDA output signal in steady flow from experimental series 2
(A) $r=18.4$ mm (B) $r=0$

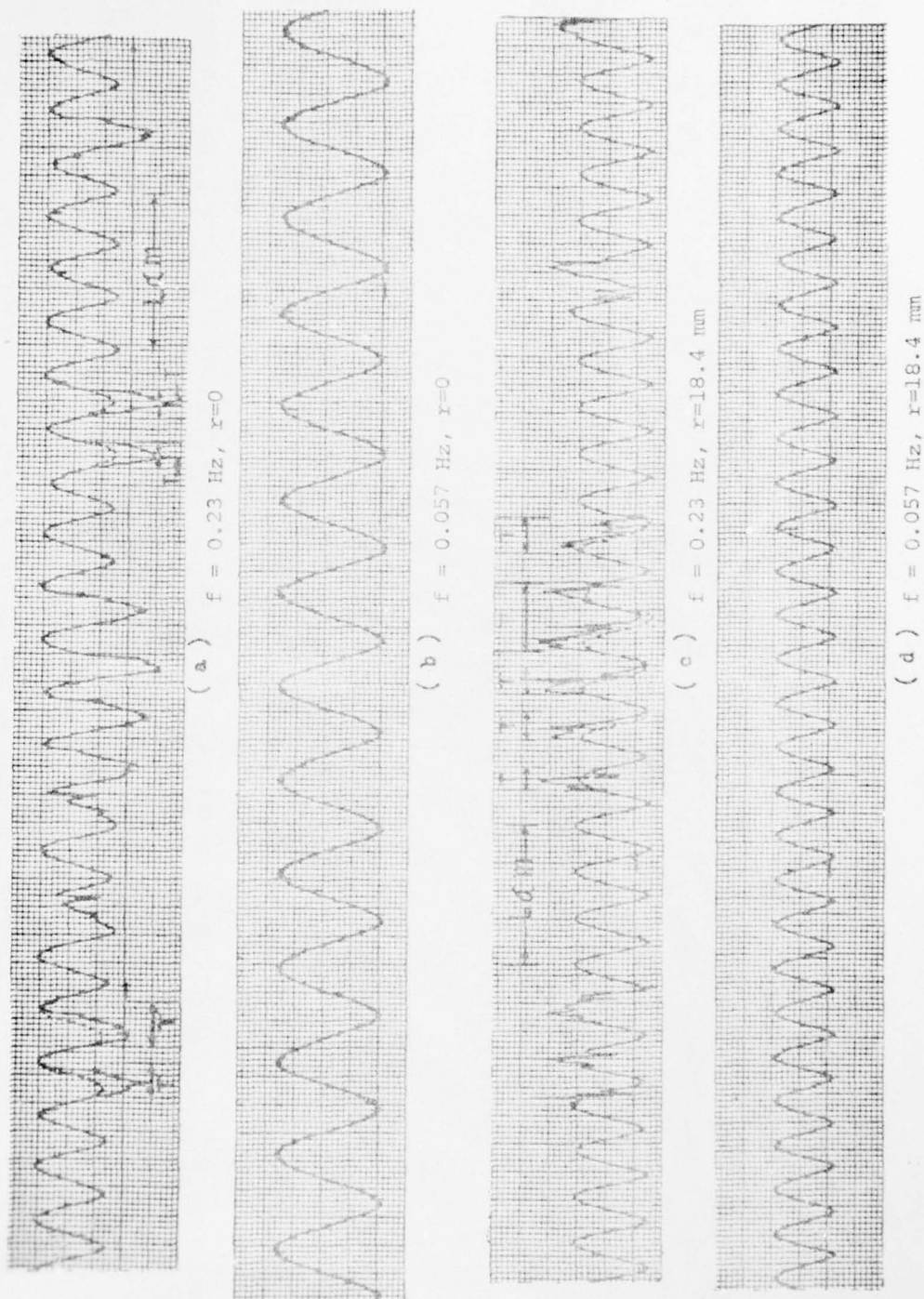


Figure 22. Typical strip chart records of the LDA output signal in oscillatory flow from experiment series 2. Intervals marked T denotes periods where the velocity trace is distorted from the normal laminar shape (shown by dotted lines) and are hence assumed to represent durations of turbulent puffs

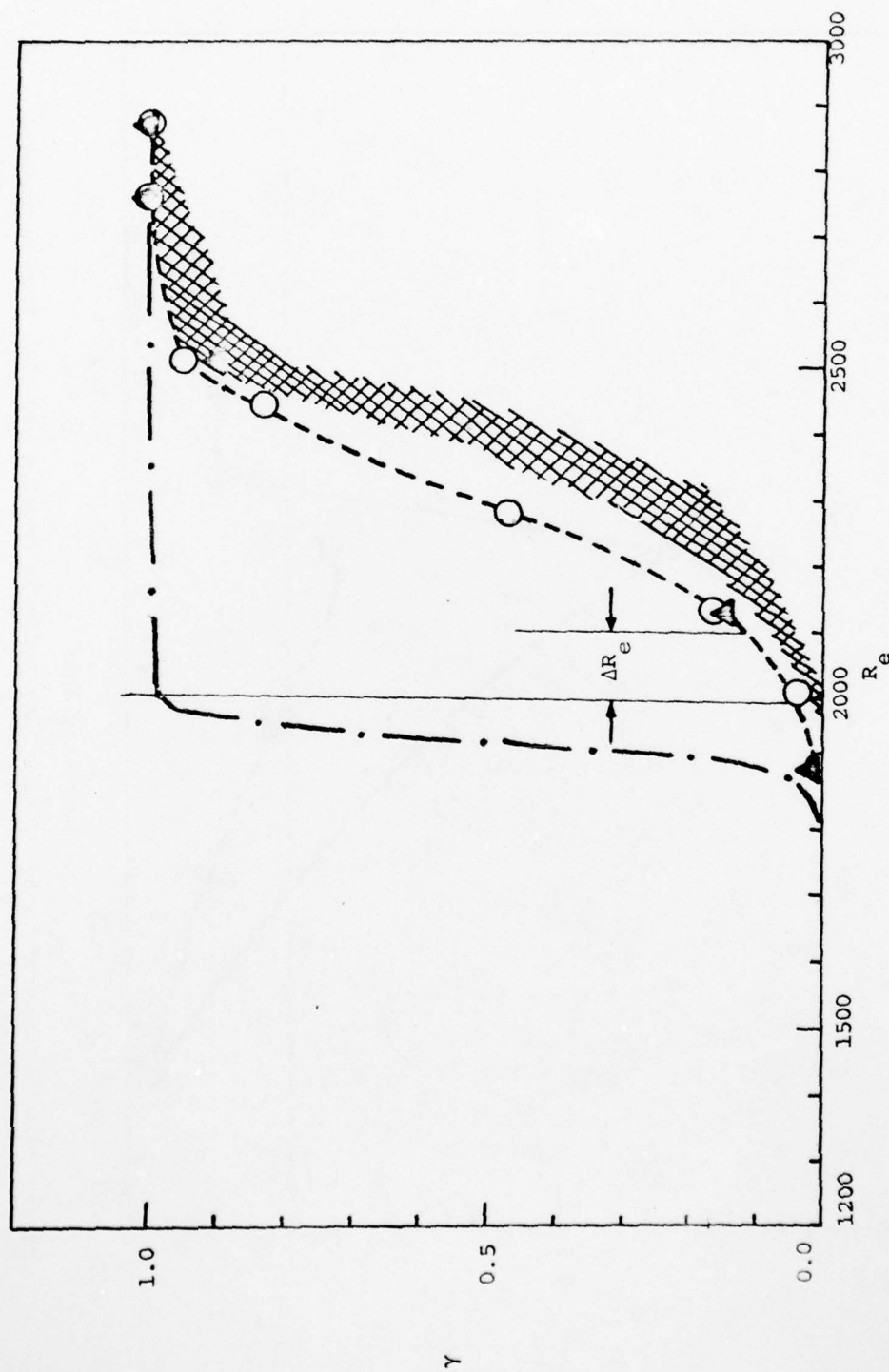


Figure 23. The intermittency of turbulent puffs in steady flow. Data from present series 2 experiments: $--\Delta--$, $r=0$; $--0--$, $r=18.4 \text{ mm}$. $---$, (estimated) intermittency data for steady flow experiments of series 1; shaded , data of Wygnanski and Champagne (1973)

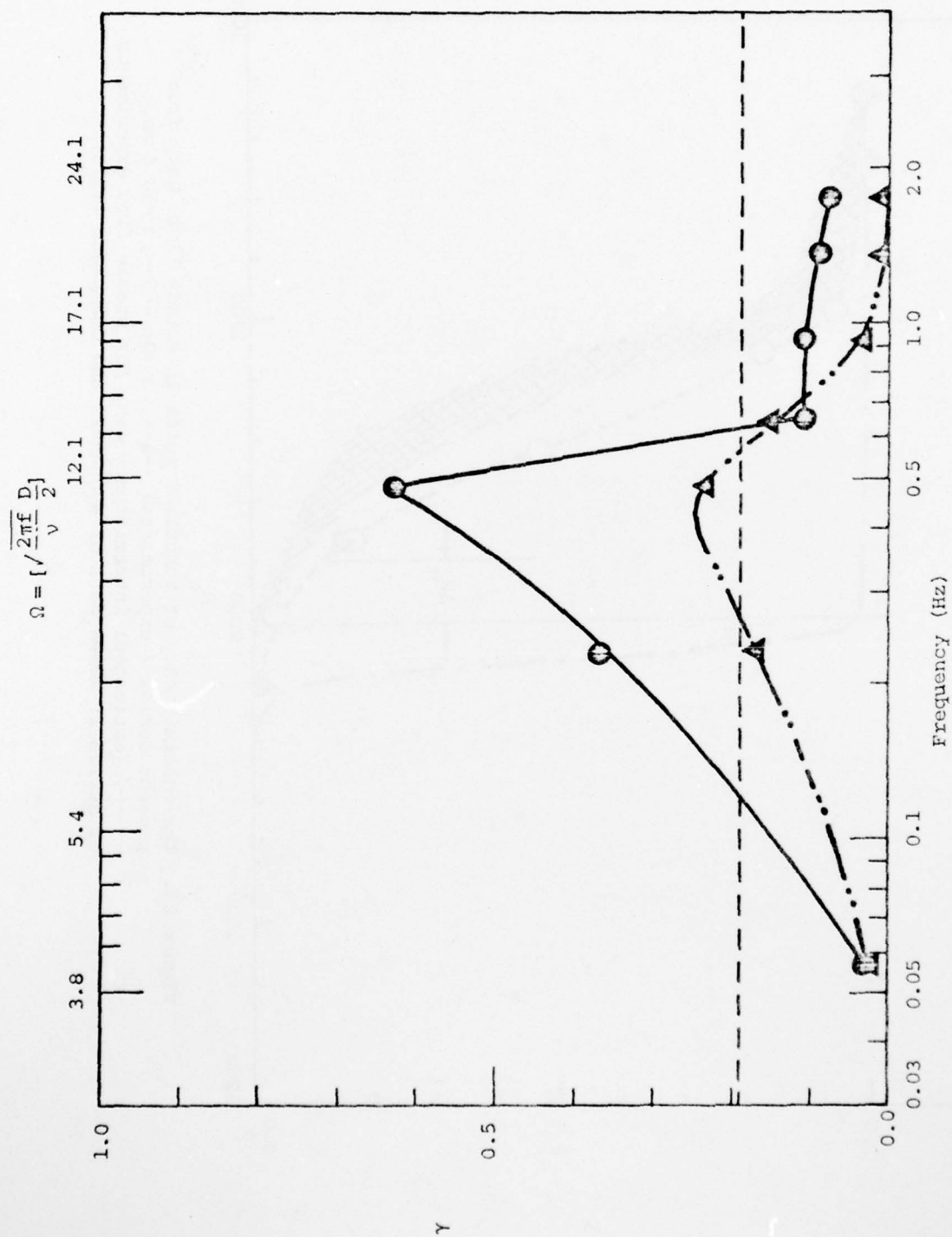


Figure 24. The intermittency of turbulent puffs in oscillatory flow from experiment series 2.

—●—, $r=0\text{mm}$; -·-·-·-·-, $r=18.4\text{ mm}$; - - - - -, mean quasi-steady flow at $Re=2100$ ($\theta=90^\circ$)

APPENDIX A

Description of the LDA System at IIHR and sample
calculations of velocity from LDA signals

Description of the IIHR LDA System

A. The LDA System

The simple channel LDA system at IIHR is shown schematically in figure A.1. The system consists of a SPECTRAPHYSICS 5 mw He-Ne laser, illuminating TSI (Thermo System Inc.) optics. The optics consists of a beam splitter which splits the laser beam into two beams each of half the original strength and spaced 50 mm apart. Each of the beams is then passed through an acousto-optic Bragg cell which shifts the frequency of the laser light by a preset amount. The Bragg-cells and the associated electronics were supplied by Opto-Elektronische-Instrumente. It's possible to shift the frequency of each beam independently by 7 selectable discrete frequencies ranging from 38.0 MHz to 44.0 MHz. By shifting the two beams by different frequencies one can obtain a relative frequency shift between the two outgoing beams. In the present case, a relative frequency shift of 0.3 MHz was used. The dual beams from the Bragg cells are focussed by the focussing lens of 104.1 mm focal length at the point (in reality, a finite sampling volume) in the fluid where the velocity is to be measured. The light scattered by a particle which passes through this volume is picked up by the receiving optics shown in the figure. The receiving optics consists of a pair of lenses and a prism that focusses the scattered light on to a photodiode. The photodiode converts the optical signal to an electrical signal which is then amplified.

In this particular arrangement, known as the dual beam system, the scattered light is essentially a mixture of the light scattered by the particle from the two incident beams. Let ν_0 be the original laser beam frequency, ν_{B1} and ν_{B2} be the frequency shifts caused by the Bragg cell on the two incident beams, \vec{n}_{i1} and \vec{n}_{i2} , the unit vectors in the directions of the incident beams, \vec{r} the unit vector in the direction of collection (see figure A-1). Then, for an idealized case of scattering occurring due to a single particle travelling with a velocity \vec{V} as shown, assuming uniform plane waves, one can write

$$\nu_1 = \nu_0 + \nu_{B1} + \left\{ \vec{V} \cdot \frac{\vec{r} - \vec{n}_{i1}}{\lambda_L} \right\} \quad (A.1)$$

$$\nu_2 = \nu_0 + \nu_{B2} + \left\{ \vec{V} \cdot \frac{\vec{r} - \vec{n}_{i2}}{\lambda_L} \right\} \quad (\text{A.2})$$

where ν_1 and ν_2 are the frequencies of scattered light from the two beams, and the bracketed terms represent the Doppler shift frequency in each case. The light picked up by the photodiode is a mixture of the above two. From the principle of heterodyning, it can be shown that the resulting light will contain the mixture of the sum and difference of the above two frequencies. Of these, the difference equal to

$$(\nu_{B1} - \nu_{B2}) + \vec{V} \cdot \left[\frac{\vec{n}_{i2} - \vec{n}_{i1}}{\lambda_L} \right] \quad (\text{A.3})$$

is the frequency of interest. This frequency is detected in the output signal by a frequency tracker. A TSI model 1090 tracker is used for this purpose. The tracker output, which is a linear function of the instantaneous velocity of the flow is low-pass filtered at 150 Hz to remove unwanted noise and then connected to the IIHR Data Acquisition System. The low-pass filtering frequency of 150 Hz was found to be high enough to include all significant turbulent frequencies in the flow. It is seen from Eq. A.3 that the output signal frequency is independent of the collection direction \vec{r} (through the intensity of the collected light does depend on \vec{r}). It is also seen that at zero velocity, the output frequency will be $\nu_{B1} - \nu_{B2}$ i.e., equal to the imposed relative frequency shift.

It is appropriate to mention here briefly some of the problems encountered in LDA measurements. One of them, viz., directional ambiguity has been overcome in the present studies by using frequency shifting technique. Secondly, particle size and distribution introduce complexities, not encountered in the simple single particle analysis. The particle size influences scattered light distribution and intensity, the ability of a particle to follow the flow and the signal to noise ratio. Also, the higher the particle concentration, the more will be the background noise due to phase differences between particles arriving at the sampling volume. Low particle concentrations, on the other hand, limit the velocity versus time information as well as generally increase the complexity of data processing

due to discontinuity in the data, or "signal drop out". Signal drop out can also be caused by large variations in velocity with time as can occur in highly turbulent flows, very low velocities and in oscillatory flows. In these cases, the accompanying frequency changes are too large to be tracked by the tracker. The use of frequency shifting, in fact, has the added advantage of bringing the range of frequency variations into the most efficient region of tracker operation. Ideally, the particles should have a high refractive index, be uniform in size, and be as large as possible (up to 5μ) while still following the flow. The concentration should be low enough to minimize Doppler ambiguity while high enough to obtain adequate time information on flow characteristics. To approach this ideal seeding is generally required. However, naturally occurring particulates in the fluid may often be adequate to give satisfactory results, as in the present study. Thirdly, the spatial resolution of LDA is limited by the requirement of a finite sampling volume. With reference to figure A-1 the dimensions L_m and D_m of the sampling volume depend on the intersection angle ϕ of the beams in the fluid and the diameter of the beam. In the present experiments the dimensions L_m and D_m are 1.1 mm and 0.7 mm respectively. The dimension L_m is very much larger than the diameter of a hot-wire ($2.5\ \mu\text{m}$) but comparable to the diameter of a total head tube. It is, however, to be noted that since oil was used in the present studies, the dimension L_m is still less than the thickness ($\approx 1.5\ \text{mm}$) of the viscous sublayer. The calculations required for obtaining the value of velocity from the LDA output are described in Appendix B.

B. The Traverse Mechanism for LDA

A simple one dimensional traverse mechanism was built for traversing the LDA optics along a horizontal diameter of the test section. The construction of this traverse can be seen from figure A-2. The upper aluminium channel slides over the bottom aluminium channel. The latter rests on a mild steel framework and can be adjusted to be level by using the four levelling screws. The upper channel is moved longitudinally by a spindle and has a travel of 50 mm. A dial indicator of 0.01 mm least count is mounted in such a way as to measure the displacement of

the upper channel. The laser, the entire optics and the photodiode are all mounted on wooden bases fixed to the upper aluminium channel and thus move together as one unit.

Because of the refraction effect, through the tube wall and the liquid, the actual displacement of the focal point (sampling volume) is not equal to the physical displacement of the traverse (apparent displacement). Knowing the thickness of the pipe wall and the refractive indices of the pipe wall and the oil, one can calculate the actual displacement of the focal point for a given apparent displacement. It was, however, felt that a practical calibration would be more desirable, as well as convenient, in the present case. A temporary arrangement consisting of an L-shaped point gage traversed by a precision micrometer (0.025 mm least count) was used for this purpose. The point gage was traversed through a hole in the tube wall, located at such a position that the tip of the gage travelled along the LDA axis. The location of the focal point could be easily determined from observing the light scattered by the tip of the gage as it moved along the axis of the LDA. The focal point was given a series of prescribed apparent displacements as measured by the dial indicator and the corresponding actual displacements as measured by the micrometer were obtained. The resulting calibration curve is shown in A.3 and is seen to be linear (as expected). This result was used in all subsequent experiments to obtain the actual displacement of the focal point. Theoretically, the uncertainty involved in the calibration was equal to the dimension " L_m " of the sampling volume. In practice, however, it was much less than this since it was possible to locate the two "extremes" of this region and set the point gage at the middle of these two positions. The finite length of the sampling volume did present some difficulty in fixing the "zero" distance from the wall during the velocity traverses. This difficulty was overcome by matching the velocity profile in steady laminar flow with the theoretical parabolic distribution. The "zero" so determined was used for the turbulent flow traverse also. In the unsteady flow, the location of the "zero" position was taken to be the point at which the oscillation amplitude (as observed on the oscilloscope) would suddenly go to zero. This was a very well defined point and could be located with

excellent repeatability.

C. Sample Calculation of Velocity from the LDA Signal

If f_D is the Doppler frequency shift, from Eq. (A.3)

$$f_D = \frac{n\vec{V}}{\lambda_L} \cdot (\vec{n}_{i1} - \vec{n}_{i2})$$

From Fig. A.1 $|\vec{n}_{i2} - \vec{n}_{i1}| = 2 \sin \phi/2$

$$\text{hence, } f_D = \frac{n\vec{V}}{\lambda_L} \cdot \vec{n}_{i2} - \vec{n}_{i1} = 2 \frac{nU}{\lambda_L} \sin \phi/2$$

where U is the velocity component normal to the bisector of \vec{n}_{i1} and \vec{n}_{i2} . The value of n is taken as unity in air and the angle as $\tan^{-1}(d/2L)$ where d is the original beam spacing introduced by the beam splitter and L is the focal length of the focussing lens. It can be easily shown that even when the beams pass through media of different refractive indices (in the present experiment, for example, they pass through the plexiglass tube wall and then through the oil), the produce $(n \cdot \sin \phi/2)$ can still be calculated using the above values for n and ϕ . Hence Eq. (A.3) can be written as

$$f_D = \frac{2U \sin [\tan^{-1}(d/2L)]}{\lambda_L}$$

or

$$U = f_D \left[\frac{\lambda_L}{2 \sin [\tan^{-1}(d/2L)]} \right] = K f_D$$

For the present LDA system, $\lambda_L = 632.8 \text{ nm}$, $L = 104.1 \text{ mm}$ and $d = 50 \text{ mm}$.

Hence,

$$K = 1.313 \text{ m/s/MHz}$$

If the relative frequency shift introduced by the Bragg cells is f_s and the measured frequency is f_m

$$U = (f_m - f_s) K$$

As already mentioned, the value of f_s in the present experiments was 0.3 Hz. The tracker output voltage E is proportional to f_m or $E = cf_m$.

Hence,

$$U = \left(\frac{E}{C} - f_s \right) K = \frac{(E - E_o) K}{C}$$

where E_0 is the tracker output voltage at zero velocity. In the present experiments c was $1 \text{ volt/MHz} \pm 0.4\%$. Thus,

$$U = (E - 0.3) \times 1.313 \text{ m/s}$$

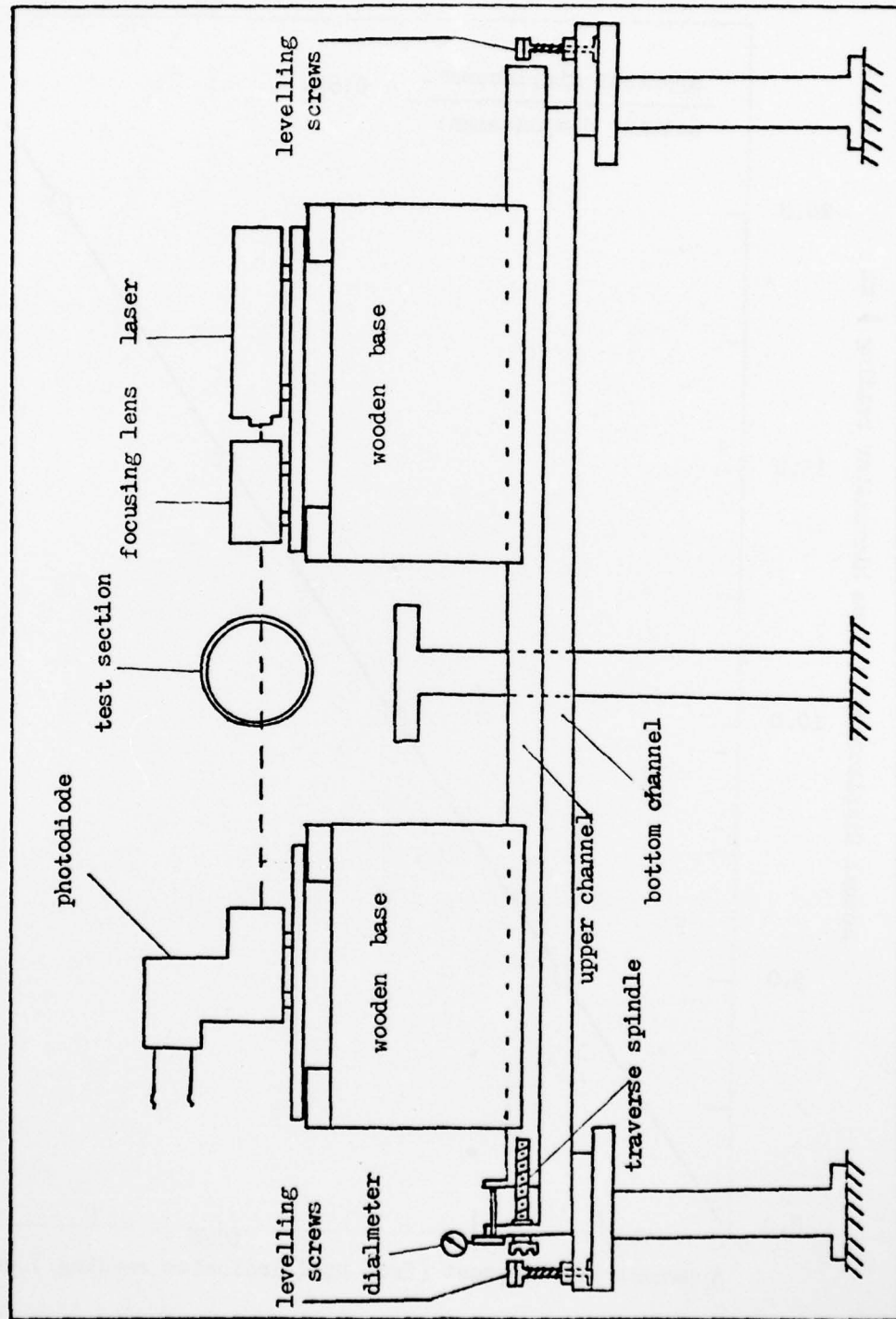


FIG.A2. DETAILS OF THE LDA TRAVERSE

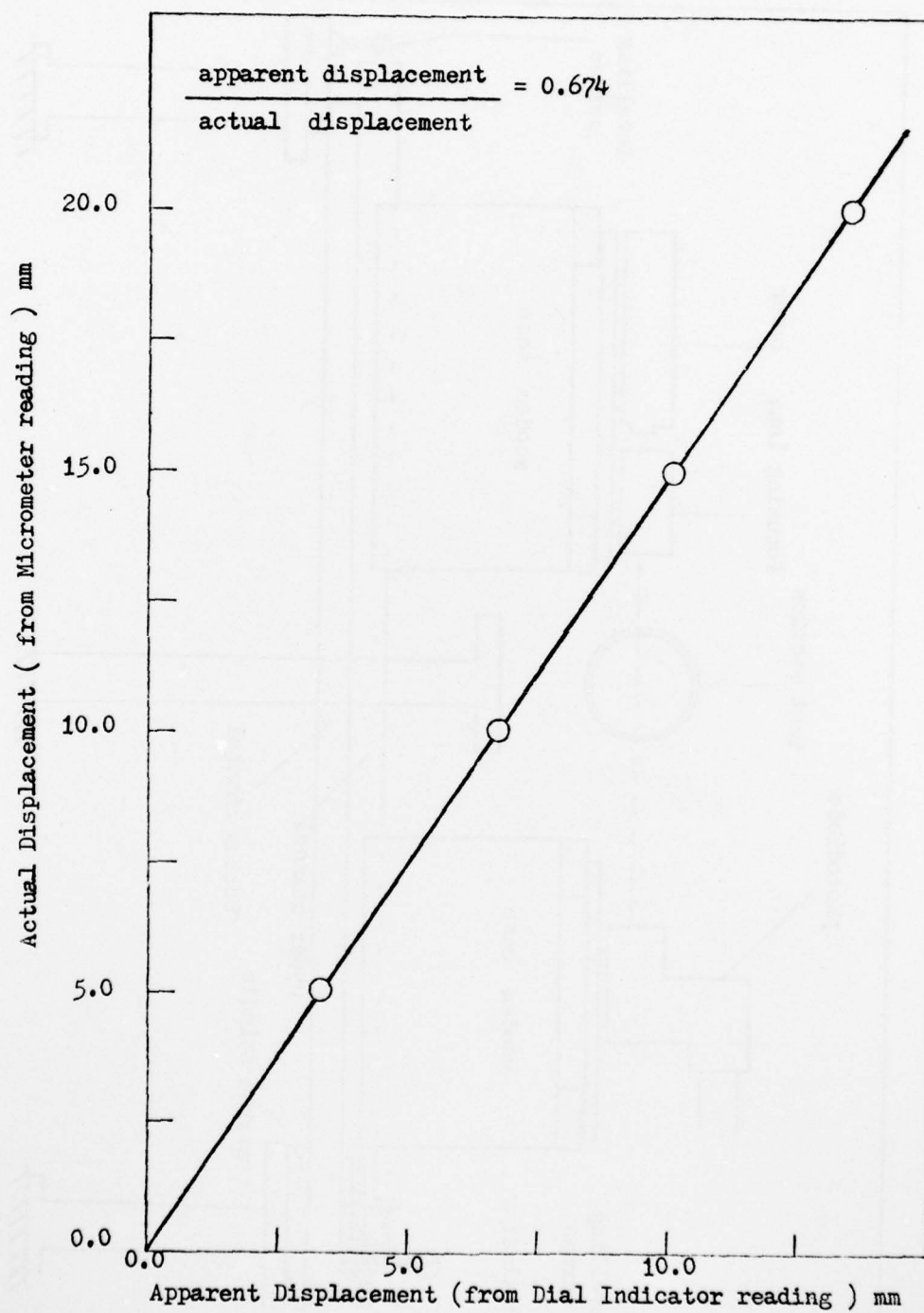


FIG.A3. CALIBRATION OF THE LDA TRAVERSE

APPENDIX B

Experimental Data

AD-A081 180

IOWA INST OF HYDRAULIC RESEARCH IOWA CITY
EXPERIMENTS ON TRANSITIONAL OSCILLATORY PIPE FLOW, (U)
AUG 79 B R RAMAPRIAN, S W TU

F/G 20/4

DAAG-29-79-G-0017

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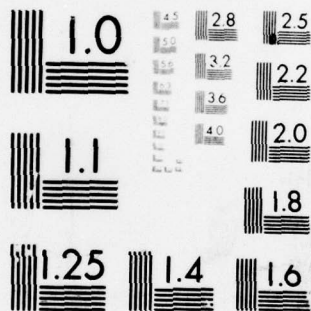
IIHR-221

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2 OF 2
AD
A081/180



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MICROCOPY RESOLUTION TEST CHART
NATIONAL BUREAU OF STANDARDS-1963-A

TABLE 1.
STEADY PRESSURE DROP

$\nu = 1.384 \times 10^{-5} \text{ m}^2/\text{s}$

$\frac{x}{D} \Delta p^*$	2872	2760	2513	2132	1818	1402	1278
6	0.0	0.0	0.0	0.0	0.0	0.0	0.0
12	0.561	0.458	0.475	0.589	0.687	1.506	0.941
24	-	1.479	1.989	1.267	1.153	1.442	-
36	1.415	1.532	1.617	1.624	1.914	2.266	2.578
42	1.553	-	-	-	-	-	2.874
48	-	2.022	2.144	2.302	2.552	2.844	3.171
54	2.033	-	-	-	-	-	3.567
60	-	2.628	2.618	2.819	3.018	3.339	3.915
66	2.575	-	-	-	-	-	4.262
72	-	3.246	3.093	3.336	3.558	3.874	4.608
78	3.184	-	-	-	-	-	4.956
84	-	3.788	3.825	3.854	4.098	4.781	5.253
90	3.715	-	-	-	-	-	5.649
96	-	4.299	4.428	4.370	4.540	5.399	5.945
102	4.304	-	-	-	-	-	6.244
108	-	4.863	4.993	4.959	4.982	5.977	6.541
114	4.854	-	-	-	-	-	-
120	-	5.416	5.532	5.405	5.448	6.553	7.186
126	5.395	-	-	-	-	-	-
132	-	6.076	6.186	5.958	5.840	7.172	7.831
138	5.965	-	-	-	-	-	-
144	-	6.726	6.777	6.547	6.282	7.789	8.424
150	6.486	-	7.123	-	-	-	-
156	-	7.236	7.393	7.153	6.649	8.326	8.969
162	7.075	-	7.726	-	6.943	-	9.265
168	7.390	7.864	7.996	7.795	7.189	8.821	9.564

$\bar{U}_{ave} : (\text{m/s}) , \quad dp/dx : (\text{newton/m}^2/\text{m})$

\bar{U}_{ave}	0.780	0.750	0.683	0.580	0.494	0.381	0.348
$-dp/dx$	233.73	224.78	191.95	140.59	74.93	57.65	49.95
$\lambda 10^{+2}$	4.620	4.850	5.000	5.090	3.730	4.820	5.020

TABLE 2.
MEASUREMENTS IN STEADY FLOW

η	Re = 2872 ($\theta = 0^\circ$)						Re = 1278 ($\theta = 90^\circ$)	
	RUN 12			RUN 22			RUN 11	RUN 21
	$\langle \bar{u} \rangle / \langle \bar{u} \rangle_{\max}$	$\langle \bar{u} \rangle / \bar{u}_*$	$y \bar{u}_* / \nu$	u' / \bar{u}_*	$\langle \bar{u} \rangle / \langle \bar{u} \rangle_{\max}$	u' / \bar{u}_*	$\langle \bar{u} \rangle / \langle \bar{u} \rangle_{\max}$	$\langle \bar{u} \rangle / \langle \bar{u} \rangle_{\max}$
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.039	0.218	4.15	4.14	1.55	0.327	1.70	0.095	0.099
0.118	0.619	11.48	12.42	2.35	0.631	2.39	0.221	0.236
0.197	0.745	13.98	20.71	2.21	0.759	2.23	0.362	0.372
0.276	0.828	15.36	28.99	1.90	0.832	1.91	0.470	0.484
0.354	0.851	16.11	37.28	1.60	0.866	1.65	0.582	0.583
0.433	0.894	16.59	45.56	1.46	-	-	0.675	-
0.512	0.926	17.17	53.84	1.28	0.957	1.12	0.769	0.749
0.591	0.943	17.49	62.13	1.19	-	-	0.826	-
0.670	0.969	17.97	70.41	1.05	-	-	0.880	0.877
0.748	0.983	18.23	78.69	0.92	-	-	0.927	-
0.827	0.986	18.34	86.98	0.85	0.991	0.9	0.964	0.962
0.945	1.0	18.55	99.40	0.80	1.0	0.85	1.0	1.0
$\langle \bar{u} \rangle_{\max}$ (m/s)	1.06			1.07			0.709	0.711
\bar{u}_{ave} (m/s)	0.783			*			0.351	*
\bar{u}_* (m/s)	0.057**			-			-	-

* In RUN 21 and RUN 22, measurements were made at only a few points to check RUN 11 and RUN 12, hence enough points were not available to calculate \bar{u}_{ave} . However, \bar{u}_{ave} in these experiments can be assumed to be the same as in RUN 11 and RUN 12 respectively.

** Based on pressure drop measurements.

TABLE 3.
MEASUREMENTS IN UNSTEADY FLOW (RUN 23)

$\bar{u}_{\max}=1.086\text{m/s}$, $(u_{qm})_{p\max}=0.43\text{ m/s}$, $\bar{u}_* = 0.0344\text{ m/s}$

η	\bar{u}/\bar{u}_{\max}	$u_{p\max}/(u_{qm})_{p\max}$	\bar{u}/\bar{u}_*	$y\bar{u}_*/\nu$	$\phi_*/\text{degrees}$
0.0	0.0	0.0	0.0	0.0	-
0.04	0.078	0.365	2.516	2.486	-60.8
0.08	0.163	0.602	5.164	4.972	-72.0
0.158	0.297	0.696	9.380	9.944	-79.2
0.197	0.361	0.672	11.400	12.430	-82.8
0.236	0.414	0.652	13.056	14.916	-86.4
0.276	0.470	0.647	14.827	17.402	-90.0
0.315	0.522	0.640	16.475	19.888	-79.2
0.354	0.572	0.647	18.043	22.374	-86.4
0.394	0.619	0.640	19.531	24.860	-82.8
0.472	0.700	0.640	22.10	29.831	-82.8
0.551	0.775	0.643	24.464	34.803	-82.8
0.630	0.836	0.659	26.404	39.775	-86.4
0.709	0.884	0.656	27.919	44.747	-82.8
0.787	0.929	0.656	29.327	49.719	-82.8
0.866	0.962	0.656	30.381	54.691	-86.4
0.984	1.0	0.656	31.568	62.149	-86.4

TABLE 4.
MEASUREMENTS IN UNSTEADY FLOW (RUN 24)

$\bar{u}_{\max} = 1.11 \text{ m/s}$, $(u_{qm})_{p\max} = 0.43 \text{ m/s}$, $\bar{u}_* = 0.036 \text{ m/s}$

η	\bar{u}/\bar{u}_{\max}	$u_{p\max}/(u_{qm})_{p\max}$	\bar{u}/\bar{u}_*	$y\bar{u}_*/\nu$	ϕ_* (degree)
0.0	0.0	0.0	0.0	0.0	-
0.04	0.082	0.214	2.541	2.583	- 7.2
0.08	0.170	0.395	5.286	5.166	+ 14.4
0.158	0.328	0.769	10.256	10.331	+ 14.4
0.236	0.461	1.029	14.365	15.497	+ 14.4
0.315	0.584	1.205	18.210	20.662	+ 14.4
0.394	0.691	1.367	21.535	25.828	0
0.472	0.780	1.463	24.322	30.994	0
0.551	0.856	1.607	26.667	36.160	- 14.4
0.630	0.910	1.743	28.372	41.325	- 7.2
0.709	0.954	1.771	29.719	46.491	- 7.2
0.787	0.998	1.983	31.117	51.657	- 21.6
0.866	1.007	1.914	31.364	56.822	- 14.4
0.984	1.000	1.897	31.151	64.571	- 21.6

TABLE 5.
MEASUREMENTS IN UNSTEADY FLOW (RUN 13)

$\bar{u}_{max}=0.818 \text{ m/s}$, $(u_{qm})_{pmax}=0.43 \text{ m/s}$, $\bar{u}_* = 0.0535 \text{ m/s}$							
η	\bar{u} / \bar{u}_{max}	$u_{pmax} / (u_{qm})_{pmax}$	\bar{u} / \bar{u}_*	$y \bar{u}_* / \nu$	ϕ_* (degree)	u' / \bar{u}_*	u' / \bar{u}_{max}
0.0	0.0	0.0	0.0	0.0	-	0.0	0.0
0.04	0.266	0.546	4.068	3.864	- 51.4	1.35	0.0883
0.08	0.370	0.652	5.664	7.729	- 64.3	1.66	0.1083
0.158	0.625	0.713	9.556	15.457	- 70.7	1.97	0.1284
0.236	0.741	0.651	11.339	23.186	- 77.1	1.86	0.1213
0.315	0.806	0.634	12.330	30.915	- 77.1	1.70	0.1115
0.394	0.867	0.675	13.265	38.643	- 70.7	1.44	0.0944
0.472	0.894	0.660	13.675	46.372	- 70.7	1.30	0.0850
0.551	0.921	0.643	14.091	54.101	- 64.2	1.19	0.0778
0.630	0.955	0.679	14.604	61.829	- 77.1	1.11	0.0721
0.709	0.975	0.660	14.923	69.558	- 83.6	1.01	0.0662
0.787	0.980	0.634	15.003	77.287	- 70.7	1.03	0.0670
0.866	0.993	0.638	15.197	85.016	- 83.6	0.974	0.0636
0.984	1.000	0.624	15.293	96.609	- 77.1	1.02	0.0667

APPENDIX C

Assembler Language Program for Sampling and
Processing Periodic Turbulent Flows on the IIHR
IBM/1800 System


```
// JOM 0000011111
// ASM ACSV3
*LIST
```

```
*****
PROCESS PROGRAM ACSV3
* THIS PROGRAM TAKES DATA FROM MPX3 PTS
* /1016,/1017,/1018. A SYNCHRONIZING SIGNAL
* MUST BE PRESENT FOR EXTERNAL SYNC ON THE ADC.
* EXITS AFTER 25 SECOND DELAY IF NO SYNC.
* THE NO. OF WAVES, THE NO. OF POINTS PER WAVE,
* AND THE DELAY TIME BETWEEN DATA POINTS ARE
* OBTAINED FROM FILE20. THE DATA OF THE 3 CHANNEL
* ARE TESTED FOR LOCKON OF THE LOG-TRACKER.
* THE RAW DATA FROM ALL THREE CHANNEL ARE
* STORED ON DISK IN FILES, FILE3, FILE4, FILE5.
* PROGRAMMED BY HUELLER BASED ON ACSV2
* MARCH, 1977
*****

0000 0 0077      START XIO      LITON
0001 30 17493003  CALL          PYL01
0003 20 20003A15  LIRE          MPTYM
0004 0 2002      DC            /2002
0005 1 1000      DC            DATES-1
0006 0 0000      ON            DC            /0800
0007 20 20003A15 LIRE          MPTYM
0008 0 0002      DC            /0002
0009 0 7000      MDX           *-3
000A 01 20000100 XIO L        LOGCA
000C 0 0000      AND          M0200
000D 0 0000      BSC          +
000E 0 7000      MDX          NOCNG
000F 30 22505003 CALL          SPECL
0011 30 03201547 CALL          CHANG
0013 30 24550000 CALL          UNC
0015 30 01102073 CALL          ACSV3
0017 0 0001      DC            1
0018 0 0000      XIO          LITOF
0019 30 25241000 CALL          VIAO
001A 01 04000100 NOCNG LD L    WNGHT      SET UP WORD COUNT TO STORE
001B 01 04000100 STO L        ST0T1      DATA IN DISK.
001C 01 04000100 STA L        ST0T2
0021 01 04001300 STO L        ST0T3
0023 0 1000      SET          32          SET ZERO IN A & D REG.
0024 01 00000100 STO L        AREAC+308
0026 01 00000100 STO L        AREAC+310
0028 01 00000100 STO L        AREAC+312
002A 01 00000100 XIO L        LOGCC      SHUT OFF LOGCC.
002C 00 01000000 LD L          /0000
002E 01 00000200 STO L        SAVE
0030 00 00000000 LD L          /0000
0032 01 00000100 STO L        AREAC+314
0034 00 20000000 STS L        /0000,/40
0036 0 0000      LD          ADDR1
0037 00 00000000 STO L        /0000
0039 0 0000      LD          DLY
003A 00 00000000 STO L        /0000
003C 01 00000100 XIO L        LOGCC
003E 20 01257005 LIRE          ALPTH
003F 0 1010      DC            /1010
0040 1 02F2      DC            DATA+2
0041 1 02F1      DC            DATA+1
0042 0 0300      DLY          -3125      LOOP COUNT FOR DELAY FOR SYNC
0043 20 01257005 LIRE          ALPTH
0044 0 0000      DC            /0000
```

0045 0 7000	MDX	*-3	
0046 01 00000100	XIO	L	10000
004A 00 00000000	STO	L	/0000
004C 0 7016	MDX		FORWD
004D 20 20003A15	EXIT1	LINE	WRTYH
			TERMINATES IF NO SYNC. SIG.
004F 0 2002	DC		/2002
004F 1 1050	DC		0MES7-1
0050 0 0000	DC		0
0051 20 20003A15	LINE		WRTYH
0052 0 0002	DC		/0002
0053 0 7000	MDX		*-3
0054 01 00000100	EXIT2	LN	L ARFAC+314
0056 00 00000000	STO	L	/0000
0058 01 00000000	LD	L	SAVE
005A 00 00000000	STO	L	/0000
005C 00 20010000	STO	L	/0000, /41
005E 01 00000100	XIO	L	10000
			START TIMERS
0060 0 0015	XIO		LITCF
0061 30 25241000	CALL		VIAQ
0063 01 40000100	FORWD	BSC	L PAU21
0065 0 0200	H0200	DC	/0200
0066 1 0007	ADDRT	DC	TIMEL
0067 0 0000	TIMEL	DC	***
0068 01 00000100	XIO	L	10000
			SHUT OFF TIMERS
006A 01 00000100	XIO	L	10000
			SENSE DESV.
006C 0 4078	BOSC		+Z-
006E 0 1000	POP		
006F 00 07000007	LDX	I3	103
0070 20 01257005	LINE		AIRTH
0071 0 3000	DC		/3000
0072 01 40000040	BSC	L	EXIT1
0074 0 0000	OFF	DC	0
0076 0 0000	BSC	F	0
			INSURE THAT AREA IS EVEN ADDRESS
0076 1 0070	LITCF	DC	OFF
0077 0 0170	DC		/0170
0078 1 0000	LITCF	DC	0
0079 0 0170	DC		/0170
007A 0 0000	AREA	DC	4
007B 31 00253000	INFORM	DC	FIL20
			INFORMATION STORED ON DISK.
007F 0 0000	DELAY	DC	***
			DELAY TIME.
007F 0 0000	POINTS	DC	***
			NO. OF POINTS ON A WAVE.
0080 0 0000	WAVES	DC	***
			NO. OF WAVES TAKEN.
0081 0 0000	CLICK	DC	***
			LOCATION OF RUN NO.
0082 0 0000	U00	DC	***
0083 0 0000	H11	DC	***
0084 0 0000	LIMNT	DC	***
0085 0130	ARFAC	BSC	313
008E 0000	BSC	F	0
010F 0 0000	IOCCA	DC	/0000
			READ D.E.S INTO A REG.
010F 0 0740	DC		/0740
0100 0 0000	IOCCB	DC	/0000
			SHUT OFF TIMERS
0101 0 0420	DC		/0420
0102 0 0000	IOCCC	DC	/0000
			TURN ON TIMER A
0103 0 0420	DC		/0420
0104 0 0000	IOCCD	DC	/0000
			SENSE DESV
0105 0 0721	DC		/0721
0106 0 2000	IOCCF	DC	/2000
			START TIMER C
0107 0 0420	DC		/0420
0108 0 0700	URGHT	DC	1020
0109 0 3200	D1200	DC	12000
			LENGTH OF FILE BY OR BY
010A 0 0005	PAU21	LD	URGHT
			SET UP WORD COUNT.
010B 01 00000070	STO	L	INFORM
010C 20 00207005	LINE		D1200
			READ INFORMATION FROM THE DISK.
010E 0 1000	DC		/1000
010F 1 0070	DC		INFORM

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 SIGNIFICANT NUMBER OF PAGES WHICH DO NOT
 REPRODUCE LEGIBLY.

0100	0	0140	MOCT2	DC	320	
0101	20	04202495		LINE	015KN	
0102	0	0100		DC	/0100	
0103	1	0070		DC	INFORM	
0104	0	7000		MOX	*-4	
0105	20	26063A15		LINE	MDTYN	
0106	0	2002		DC	/2002	
0107	1	1048		DC	DMESG-1	
0108	0	0000		DC	0	
0109	20	26063A15		LINE	MDTYN	
010A	0	0002		DC	/0002	
010F	0	7000		MOX	*-3	
010C	20	23A17172		LINE	TYPE2	
010D	1	0070		DC	DELAY	
010E	0	0003		DC	3	
010F	20	26063A15		LINE	MDTYN	
01F0	0	2002		DC	/2002	
01F1	1	1074		DC	DMESG-1	
01F2	0	0000		DC	0	
01F3	20	26063A15		LINE	MDTYN	
01F4	0	0002		DC	/0002	
01F5	0	7000		MOX	*-3	
01F6	20	23A17172		LINE	TYPE2	
01F7	1	0002		DC	000	
01F8	0	0003		DC	3	
01F9	01	04000002		LD	L 000	TRANSFER NO. 01, LIMIT
01FA	01	04000000		STO	L 00	
01FB	01	04000003		LD	L 011	
01FC	01	0400000A		STO	L 01	
01FD	01	04000008		LD	L LIMIT	
01FE	01	04000000		STO	L LIMIT	
01FF	01	04000000		LD	L WAVES	
01FF	01	0400000F		"	L POINTS	
01F9	0	1000		SLT	10	
01FA	0	0000		CMP	0120H	FILE LENGTH IS 40 SECTORS
01FB	0	7002		MOX	00000	
01FC	0	700A		MOX	0000	
01FD	0	7000		MOX	0000	
01FE	20	26063A15	NGOOD	LINE	MDTYN	
01FF	0	2002		DC	/2002	
0200	1	1004		DC	DMESG-1	
0201	0	0000		DC	0	
0202	20	26063A15		LINE	MDTYN	
0203	0	0002		DC	/0002	
0204	0	7000		MOX	*-3	
0205	01	00000000		DC	L EXIT1	OUT IF FILES TOO SMALL
0207	01	04000000	GOOD	LD	L WAVES	
0208	01	04000000		STO	L NUMBER	STORE NO. OF WAVES
0209	01	0400000F		LD	L POINTS	
0200	0	1001		SLA	1	MULTIPLY BY TWO
020F	01	04000000		STO	L THPTS	THICE THE NUMBER OF POINTS
0210	0	10A0		SLT	32	ZERO A AND 0 REP.
0211	01	04000000		S	L THPTS	
0213	01	04000000		STO	L THPTS	MINUS THICE THE NUMBER
0215	0	1010		SLA	10	ZERO A REP.
0216	01	0400000F		S	L POINTS	OBTAIN THICE THE NUMBER
0218	01	0400000F		STO	L THPTS	OF POINTS NEGATIVE.
021A	01	00000100		X10	L 10000	SHIFT OFF TIMES 0
021C	00	04000000		LD	L /0000	SAVE THE ADDRESS OF 10H'S
021F	01	0400000F		STO	L SAVE	LEVEL ZERO INTER. ROUTINE.
0220	00	20400000		STS	L 7000, 04	UNWRITE STOP POINT, SLT.
0222	01	04000000		LD	L ADDR	SUBSTITUTE OUR INTERRUPT
0224	00	04000000		STO	L /0000	ROUTINE ADDRESS.
0226	30	14002400		CALL	MASK	
0228	1	1AF0		DC	MSK1	
0229	1	1AF1		DC	MSK2	

```

022A 01 C400007F SYNC LD L DELAY SET UP DELAY INT TIMER A
022B 00 D5000000 STO L 40000 LOOP FOR DATA
022C 20 01257805 LDR ALPH TAKE FIRST PT. ONLY AFTER THE
0231 0 1010 DC /1010 SYNC. SIGNAL IS RECEIVED.
0232 1 02F2 DC DATA+2
0233 1 02F1 DC DATA+1
0234 0 0000 DC /0000
0235 20 01257805 LDR ALPH
0236 0 0000 DC /0000
0237 0 70F0 HX *--
0238 0 0000 XIO 10000 START TIMER A
0239 0 3000 DLY WAIT FOR TIMER INTERRUPT
023A 0 70FF HX *--2
023B 0 0000 TIMER DC *-- TIMER INTERRUPT ROUTINE
023C 0 0007 XIO 10000 SENSE DECM
023D 0 4070 BSCC *Z- RESET INDICATORS
023E 0 1000 NOP
023F 01 C400007F LD L DELAY
0241 00 D4000004 STO L /0004 RESET TIMER A
0243 20 01257805 LDR ALPH OBTAIN DATA SEQUENTIALLY.
0244 0 2000 DC /2000
0245 1 02F0 DC DATA
0246 1 02F8 DC ERROR
0247 20 01257805 LDR ALPH TEST FOR COMPLETION.
0248 0 0000 DC /0000
0249 0 70F0 HX *--3
024A 01 C400007F LD L DATA+2
024C 01 D4000000 DKST1 STO L STDT1+2 FOR CHANNEL1.
024E 01 74010260 HX L DKST1+1,1
0250 01 C400007F LD L DATA+3
0252 01 D4000000 DKST2 STO L STDT2+2 STORE CHAN.2 DATA IN DISK AREA.
0254 01 74010263 HX L DKST2+1,1 SET UP FOR NEXT CSL START.
* TEST FOR TRACKER
0256 01 C400007F LD L DATA+4 TEST IF UIXU0
0258 0 0010 A U0
0259 0 7010 BSCC -
025A 0 7015 HX OK
025B 01 C400007F LD L DATA+4 TEST /UI-UI-1/>UI
025D 0 0000 S LAST
025E 0 4010 BSCC -
025F 0 7003 HX LIMT
0260 0 0007 STO MEMO
0261 0 1010 SLA 10
0262 0 0005 S MEMO
0263 0 0000 LIMT CMP UI
0264 0 7000 HX OK
0265 0 7003 HX NOK
0266 0 7007 HX NOK
0267 0 0000 LAST DC *--
0268 0 0000 MEMO DC *--
0269 0 0040 U0 DC 1000 U0=100MVOLT
026A 0 0020 U1 DC 32 U1=2MVOLT
026B 0 0000 COUNT DC *--
026C 0 000A LIMT DC 10
026D 0 0000 ZERO DC 0
026E 01 74010260 HX HX L COUNT,1
0270 01 C400007F OK LD L DATA+4
0272 0 00F4 STO LAST
0273 01 D400130F DKST3 STO L STDT3+2 STORE CHAN.3 DATA ON DISK.
0275 01 74010274 HX L DKST3+1,1 SET UP FOR NEXT CSL START.
0277 0 7102 HX 1+2 DECREMENT INDEX REGISTER.
0278 0 7001 HX TIMEX RETURN FOR NEXT SAMPLE ON THIS HAVE
0279 0 7002 HX HAVE END SAMPLING. NEXT HAVE.
027A 01 40000230 TIMEX BSCC I TIMER END OF TIMER INTERRUPT ROUTINE.
027C 01 00000100 HAVE XIO L 10000 SHUT OFF TIMERS.

```

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027F 0	00FC	LD	COUNT	TEST NO OF BAD POINTS
027F 0	00FC	S	LIMIT	
0280 0	4008	BSC	+	
0281 0	7012	MDX	GOOD	
0282 20	23A17172	LIBF	TYPE2	
0283 1	026F	DC	COUNT	
0284 0	0001	DC	1	
0285 0	00C7	LD	DKST1+1	RESTORES ADDRESS CH.1
0286 01	9400007F	S	L POINTS	
0288 0	00C4	STO	DKST1+1	
0289 0	00C0	LD	DKST2+1	RESTORES ADDRESS CH.2
028A 01	9400007F	S	L POINTS	
028C 0	00C0	STO	DKST2+1	
028D 0	00FC	LD	DKST3+1	RESTORES ADDRESS CH.3
028F 01	9400007F	S	L POINTS	
0290 0	00F3	STO	DKST3+1	
0291 0	0000	LD	ZERO	RESET COUNT
0292 0	0000	STO	COUNT	
0293 0	700F	MDX	SYNCH	
0294 0	0000	LD	ZERO	
0295 0	0000	STO	COUNT	
0296 0	0000	LD	DKST1+1	
0297 01	94000000	S	L ADDR7	
0298 01	94000100	CMP	L ADDR7	CHECK TO SEE IF THE DISK
0299 0	7001	MDX	OUT	AREA IS FULL.
029C 0	7002	MDX	POINT	
029D 01	94000000	OUT	SET L	GO TO DISK OUTPUT SUBROUTINE.
029E 01	70FF0000	POINT	MDX L	DECREMENT NUMBER OF LINES.
029F 0	7008	MDX	SYNCH	GO BACK TO SYNCH LOOP.
02A2 01	94000000	SET	L	
02A5 0	0000	LD	SAVE	RESTORE I/O LEVEL ZERO
02A7 00	20410000	STO	L /0000	INTER. ROUTINE ADDRESS.
02A9 30	20550000	CALL	L /0000,CS	WRITE STORAGE PROT. BIT.
02AB 1	1AF0	DC	MSK1	
02AC 1	1AF1	DC	MSK2	
02AD 01	00000100	XIO	L	TURN ON TEST C.
02AF 30	03400000	CALL	CLOCK	OBTAIN RUN NUMBER.
02B1 1	0001	DC	CLICK	
02B2 0	003A	LD	DE320	
02B3 01	94000070	STO	L INFO1	
02B5 20	04202405	LIBF	DISKN	WRITE OUT THE DATA ON DISK.
02B6 0	3000	DC	73000	DATA MAY BE USED FOR PLOTTING.
02B7 1	0070	DC	INFO1	
02B8 0	0000	DC	/0000	
02B9 20	04202405	LIBF	DISKN	
02BA 0	0100	DC	/0100	
02BB 1	0070	DC	INFO1	
02BC 0	7000	MDX	SEE	
02BD 01	00000001	LD	L	
02BF 20	02255103	LIBF	BINDC	CONVERT RUN NUMBER FOR
02C0 1	1007	DC	INOUT	PRINTOUT.
02C1 20	08503500	LIBF	HOLEC	
02C2 0	0000	DC	/0000	
02C3 1	1007	DC	INOUT	
02C4 1	1AF0	DC	OTPUT	
02C5 0	0000	DC	6	
02C6 20	23A17155	LIBF	TYPRN	PRINT RUN NUMBER.
02C7 0	2002	DC	/2002	
02C8 1	1AF0	DC	DEB3-1	
02C9 0	0000	DC	0	
02CA 20	23A17155	LIBF	TYPRN	TEST OP. COMPLETE.
02CB 0	0000	DC	0	
02CC 0	70F0	MDX	0-3	
02CD 30	20550000	CALL	UNC	
02CE 30	011F2073	CALL	ACGV3	

0201	1	0435	DC	UNK	
0202	30	189028F3	CALL	CHPHE	
0206	0	0001	DC	1	
0207	0	0000	DC	0	
0208	01	00000070	XIO L	LITOF	
020A	30	75261F00	CALL	VIAO	
020C	0	0000	NUMBER	DC	*** NUMBER OF WAVES TO BE SAMPLED
020D	0	0000	THPTS	DC	*** TWICE NO. OF POINTS.
020E	0	0000	THPTS	DC	*** MINUS TWICE NO. OF PTS.
020F	0	0000	SAVE	DC	*** SAVED ADDRESS IN /0000
0210	0	0000	DATAH	DC	4
02F1	0	1010	DC	/1010	
02F2	1	02F2	DC	DATAH+2	
02F3	1	02F3	DC	DATAH+3	
02F4	1	02F4	DC	DATAH+4	
02F5	0	0003	DC	3	
02F6	0	0000	ERR08	DC	***
02F8	01	407002F0	ERR08	DC	ERR08
02F9	1	0230	ADDRA	DC	TIMER ADDRESS OF TIMER ROUTINE
02FA	0	2717	SCALE	DC	10007 SCALING COEF.
02FB	0	0140	DF320	DC	320 CONSTANT USED FOR DISKN
02FE	0	0000	DC	E 0	
02FF	0	0130	AREAR	DC	315 DISKN AREA
0420	0	0000	OUTS	DC	*** DISK OUTPUT SUBROUTINE.
042A	20	04202495	LIFE	DISKN	RUN RAW DATA INTO DISK
042B	0	3000	DC	/3000	FOR CHAN.1.
042C	1	0469	ADCC1	DC	STDT1
042D	0	0000	DC	0	
042E	20	04202495	LIFE	DISKN	
042F	0	0100	DC	/0100	
0430	1	0469	DC	STDT1	
0431	0	70FC	MAX	***	
0432	20	04202495	LIFE	DISKN	RUN RAW DATA INTO DISK
0433	0	3000	DC	/3000	FOR CHAN.2.
0434	1	00FC	ADCC2	DC	STDT2
0435	0	0001	UNK	DC	1
0436	20	04202495	LIFE	DISKN	
0437	0	0100	DC	/0100	
0438	1	00FC	DC	STDT2	
0439	0	70FC	MAX	***	
043A	20	04202495	LIFE	DISKN	RUN RAW DATA INTO DISK
043B	0	3000	DC	/3000	FOR CHAN.3.
043C	1	1300	ADCC3	DC	STDT3
043D	0	0000	DC	0	
043E	20	04202495	LIFE	DISKN	
043F	0	0100	DC	/0100	
0440	1	1300	DC	STDT3	
0441	0	70FC	MAX	***	
0442	01	040000FC	LD L	STDT2+1	
0443	0	0022	A	DECC	CHANGE OF SECTOR ADDRESS.
0444	01	040000FC	STO L	STDT2+1	
0445	01	0400136F	LD L	STDT3+1	
0446	0	8010	A	DECC	CHANGE OF SECTOR ADDRESS.
0447	01	0400136F	STO L	STDT3+1	
0448	0	C010	LD	STDT1+1	
0449	0	8010	A	DECC	CHANGE OF SECTOR ADDRESS.
044A	0	8010	STO	STDT1+1	
044B	01	74010466	MAX L	STCHT,1	
044C	0	C010	LD	ADCC4	
0452	01	04000240	STO L	DKST1+1	RESTORE STORE ADDRESS.
0453	0	C00F	LD	ADCC5	
0454	01	04000253	STO L	DKST2+1	
0455	0	C00C	LD	ADCC6	
0456	01	04000274	STO L	DKST3+1	
0457	0	C00B	LD	STCHT	

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0450	0	0000	END	DEF12	
0450	1	7000	END	ENDIT	
0450	0	7000	END	OUT2	
0450	01	40000000	OUT2	DEF1	1
0460	01	40000000	ENDIT	DEF1	1
0462	1	0000	AD006	DC	ST01+2
0463	1	0000	AD005	DC	ST02+2
0464	1	1300	AD006	DC	ST03+2
0465	0	0000	DEF12	DC	12
0466	0	0000	ST01	DC	---
0467	0	0000	DEF12	DC	6
0468	1	0000	AD007	DC	ST01+1
0469	31	00253033	ST01	DC	FIL03 SEDIMENT CONCENTRATION.
0460		0777	SSS		1919
0461	31	00253034	ST02	DC	FIL04 HORIZONTAL VELOCITY COMPONENT.
0462		0777	SSS		1919
0463	31	00253035	ST03	DC	FIL05 VERTICAL VELOCITY COMPONENT.
0464		0777	SSS		1919
1AF0	0	0000	DEF1	DC	/DEF1
1AF0	0	0000	DEF1	DC	/DEF1
1AF1	0	0000	DEF1	DC	/DEF1
1AF2	0	0000	DEF1	DC	/DEF1
1AF3	0	0000	DEF1	DC	/DEF1
1AF4	0	0000	DEF1	DC	/DEF1
1AF5	0	0000	DEF1	DC	/DEF1
1AF6	0	0000	DEF1	DC	/DEF1
1AF7	0	0000	DEF1	DC	/DEF1
1AF8	0	0000	DEF1	DC	/DEF1
1AF9	0	0000	DEF1	DC	/DEF1
1B00	0	0000	DEF1	DC	/DEF1
1B01	0	0000	DEF1	DC	/DEF1
1B02	0	0000	DEF1	DC	/DEF1
1B03	0	0000	DEF1	DC	/DEF1
1B04	0	0000	DEF1	DC	/DEF1
1B05	0	0000	DEF1	DC	/DEF1
1B06	0	0000	DEF1	DC	/DEF1
1B07	0	0000	DEF1	DC	/DEF1
1B08	0	0000	DEF1	DC	/DEF1
1B09	0	0000	DEF1	DC	/DEF1
1B10	0	0000	DEF1	DC	/DEF1
1B11	0	0000	DEF1	DC	/DEF1
1B12	0	0000	DEF1	DC	/DEF1
1B13	0	0000	DEF1	DC	/DEF1
1B14	0	0000	DEF1	DC	/DEF1
1B15	0	0000	DEF1	DC	/DEF1
1B16	0	0000	DEF1	DC	/DEF1
1B17	0	0000	DEF1	DC	/DEF1
1B18	0	0000	DEF1	DC	/DEF1
1B19	0	0000	DEF1	DC	/DEF1
1B20	0	0000	DEF1	DC	/DEF1
1B21	0	0000	DEF1	DC	/DEF1
1B22	0	0000	DEF1	DC	/DEF1
1B23	0	0000	DEF1	DC	/DEF1
1B24	0	0000	DEF1	DC	/DEF1
1B25	0	0000	DEF1	DC	/DEF1
1B26	0	0000	DEF1	DC	/DEF1
1B27	0	0000	DEF1	DC	/DEF1
1B28	0	0000	DEF1	DC	/DEF1
1B29	0	0000	DEF1	DC	/DEF1
1B30	0	0000	DEF1	DC	/DEF1
1B31	0	0000	DEF1	DC	/DEF1
1B32	0	0000	DEF1	DC	/DEF1
1B33	0	0000	DEF1	DC	/DEF1
1B34	0	0000	DEF1	DC	/DEF1
1B35	0	0000	DEF1	DC	/DEF1
1B36	0	0000	DEF1	DC	/DEF1
1B37	0	0000	DEF1	DC	/DEF1
1B38	0	0000	DEF1	DC	/DEF1
1B39	0	0000	DEF1	DC	/DEF1
1B40	0	0000	DEF1	DC	/DEF1
1B41	0	0000	DEF1	DC	/DEF1
1B42	0	0000	DEF1	DC	/DEF1
1B43	0	0000	DEF1	DC	/DEF1
1B44	0	0000	DEF1	DC	/DEF1
1B45	0	0000	DEF1	DC	/DEF1
1B46	0	0000	DEF1	DC	/DEF1
1B47	0	0000	DEF1	DC	/DEF1
1B48	0	0000	DEF1	DC	/DEF1
1B49	0	0000	DEF1	DC	/DEF1
1B50	0	0000	DEF1	DC	/DEF1
1B51	0	0000	DEF1	DC	/DEF1
1B52	0	0000	DEF1	DC	/DEF1
1B53	0	0000	DEF1	DC	/DEF1
1B54	0	0000	DEF1	DC	/DEF1
1B55	0	0000	DEF1	DC	/DEF1
1B56	0	0000	DEF1	DC	/DEF1
1B57	0	0000	DEF1	DC	/DEF1
1B58	0	0000	DEF1	DC	/DEF1
1B59	0	0000	DEF1	DC	/DEF1
1B60	0	0000	DEF1	DC	/DEF1
1B61	0	0000	DEF1	DC	/DEF1
1B62	0	0000	DEF1	DC	/DEF1
1B63	0	0000	DEF1	DC	/DEF1
1B64	0	0000	DEF1	DC	/DEF1
1B65	0	0000	DEF1	DC	/DEF1
1B66	0	0000	DEF1	DC	/DEF1
1B67	0	0000	DEF1	DC	/DEF1
1B68	0	0000	DEF1	DC	/DEF1
1B69	0	0000	DEF1	DC	/DEF1
1B70	0	0000	DEF1	DC	/DEF1
1B71	0	0000	DEF1	DC	/DEF1
1B72	0	0000	DEF1	DC	/DEF1
1B73	0	0000	DEF1	DC	/DEF1
1B74	0	0000	DEF1	DC	/DEF1
1B75	0	0000	DEF1	DC	/DEF1
1B76	0	0000	DEF1	DC	/DEF1
1B77	0	0000	DEF1	DC	/DEF1
1B78	0	0000	DEF1	DC	/DEF1
1B79	0	0000	DEF1	DC	/DEF1
1B80	0	0000	DEF1	DC	/DEF1
1B81	0	0000	DEF1	DC	/DEF1
1B82	0	0000	DEF1	DC	/DEF1
1B83	0	0000	DEF1	DC	/DEF1
1B84	0	0000	DEF1	DC	/DEF1
1B85	0	0000	DEF1	DC	/DEF1
1B86	0	0000	DEF1	DC	/DEF1
1B87	0	0000	DEF1	DC	/DEF1
1B88	0	0000	DEF1	DC	/DEF1
1B89	0	0000	DEF1	DC	/DEF1
1B90	0	0000	DEF1	DC	/DEF1
1B91	0	0000	DEF1	DC	/DEF1
1B92	0	0000	DEF1	DC	/DEF1
1B93	0	0000	DEF1	DC	/DEF1
1B94	0	0000	DEF1	DC	/DEF1
1B95	0	0000	DEF1	DC	/DEF1
1B96	0	0000	DEF1	DC	/DEF1
1B97	0	0000	DEF1	DC	/DEF1
1B98	0	0000	DEF1	DC	/DEF1
1B99	0	0000	DEF1	DC	/DEF1
1C00	0	0000	DEF1	DC	/DEF1

NO ERRORS IN ABOVE ASSEMBLY.

AD003
DUP FUNCTION COMPLETED

```
// JOB 0000011111
// ASM COMPT
*LIST
```

```
*****
* PROGRAM : COMPT
* THIS PROGRAM COMPUTES THE PERIODIC MEAN
* AND THE RMS OF THE RANDOM COMPONENT
* OF THE SIGNALS FOR 3 CHANNELS FROM THE DATA
* STORED ON DISK BY THE PROCESS PROGRAM AGSV3.
* PROGRAMMED BY A. MUELLER, APRIL 1977
*****

0000 01 0C000152 START XIO L LITON
0002 01 C40006F9 LD L STD1+1 SAVE SECTOR ADDRESS.
0004 01 D400007A STO L SECSV
0006 01 C4000370 LD L DES20 SET UP WORD COUNT TO OBTAIN
0008 01 D4000163 STO L INFOM EXPERIMENTAL PARAMETERS.
000A 20 04262495 LIBF DISKN READ FIL20 FROM DISK
000B 0 1000 DC /1000 WHICH CONTAINS THE
000C 1 0163 DC INFOM NUMBER OF POINTS PER WAVE,
000D 0 0000 DC /0000 THE NUMBER OF WAVES SAMPL-
000E 20 04262495 LIBF DISKN ED AND THE RUN NUMBER.
000F 0 0100 DC /0100
0010 1 0163 DC INFOM
0011 0 70FC MDX *-4
0012 01 C4000165 LOOP1 LD L WAVES SET UP COUNTER FOR NUMBER
0014 01 D400015A STO L NUMBR OF AVERAGES COMPUTED.
0016 01 C4000167 LD L PONT5 COMPUTE TWICE THE NUMBER
0018 0 1001 SLA 1 OF POINTS.
0019 01 D4000158 STO L TNPTS
001B 0 10A0 SLT 32 CLEAR STORAGE FOR
001C 01 65800158 LDX 11 TNPTS ACCUMULATION OF SUMS.
001E 01 D00002A6 CLEAR STD L1 AREAC-2 AREAC : USED FOR ACCUMULA-
0020 0 71FE MDX 1 -2 TION OF SUMS.
0021 0 70FC MDX CLEAR
0022 00 6500FDC0 LDX L1 -576 CLEAR AREAD.
0024 01 D50005B5 CLER2 STO L1 AREAD+576
0026 0 7101 MDX 1 1
0027 0 70FC MDX CLER2
0028 01 94000158 S L TNPTS OBTAIN MINUS TWICE THE
002A 01 D4000158 STO L TNPTS NUMBER OF POINTS. TNPTS
002C 01 C400007C LD L XR4 CONTAINS -2*PONT5.
002E 01 D400007D CMP L TWO CHECK FOR LOOP, SET UP OF
0030 0 7002 MDX NSKIP ADDRESSES.
0031 0 7016 MDX SKIP
0032 0 701A MDX SKIP
0033 0 C02F NSKIP LD ADDD1+1
0034 01 94000158 S L TNPTS MODIFY ADDRESSES FOR
0036 0 D02C STO ADDD1+1 ACCUMULATION AND
0037 0 D02D STO ADDD1+3 MANIPULATION OF DATA.
0038 01 D4000099 STO L LDDD1+1
003A 01 C400011C LD L ADDD2+1 SET UP ADDRESSES.
003C 01 94000158 S L TNPTS DO FOR FIRST LOOP ONLY.
003E 01 D400011C STO L ADDD2+1
0040 01 D400011E STO L ADDD2+3
0042 0 1010 SLA 16 ZERO A REG.
0043 01 94000167 S L PONT5 COMPUTE MINUS THE
0045 01 D4000159 STO L MNPTS NUMBER OF POINTS.
0047 01 C4000167 LD L PONT5
0049 01 84000114 A L SURCP+1
004B 01 D4000114 STO L SUBCP+1
004D 01 C4000157 SKIP LD L WDCNT SET UP WORD COUNT FOR
004F 01 D40006F8 STO L STD1 DISK READ.
0051 20 04262495 READD LIBF DISKN READ IN THE FIRST SET OF
0052 0 1000 DC /1000 DATA STORED ON DISK IN
```

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0053 1 06F8          DC      STDT1
0054 0 0000          DC      /0000
0055 20 04262495     LIBF     DISKN
0056 0 0100          DC      /0100
0057 1 06F8          DC      STDT1
0058 0 70FC          MDX     *-4
0059 01 65800158     AGAIN LDX 11 TNPTS   LOAD INDEX REGISTERS TO
005B 01 66800159     LDX 12 MNPTS   BEGIN SIGNAL AVERAGING.
005D 01 C40006FA     LOAD1 LD L STDT1+2
005F 0 0019          STO      SAVE1
0060 0 C018          LD      SAVE1
0061 0 1890          SRT      16        COMPUTE SIGNAL AVERAGED
0062 01 8D0002A8     ADDD1 AD L1 AREAC   RESULTS.
0064 01 D00002A8     STD      L1 AREAC
0066 01 7401005E     MDX L LOAD1+1,1   MODIFY ADDRESS.
0068 0 00F5          LD      LOAD1+1   CHECK FOR END OF DATA BLOCK.
0069 01 9400015B     S      L ADC01
006B 01 B4000157     CMP L WDCNT
006D 0 400F          BSI      MORDT     MORE DATA REQUIRED.
006E 0 7001          MDX      MCOMP     COMPUTATIONS CONTINUE.
006F 0 400D          BSI      MORDT     MORE DATA REQUIRED.
0070 0 7201          MCOMP MDX 2 1     DECREMENT XR2.
0071 0 1000          NOP
0072 0 7102          MDX 1 +2         DECREMENT XR1.
0073 0 70E9          MDX LOAD1        GO BACK FOR MORE DATA.
0074 01 74FF015A     MDX L NUMBR,-1   DECREMENT NUMBER OF WAVES.
0076 0 70E2          MDX AGAIN        GET ANOTHER WAVE SET.
0077 0 701C          MDX COMPT        GO TO COMPUTATION SCHEME.
0078 0 0000          TEHP DC *-A*     TEMPORARY STORAGE.
0079 0 0000          SAVE1 DC *-+     TEMPORARY STORAGE.
007A 0 0000          SECSV DC *-+     SAVE SECTOR ADDRESS FOR
007B 0 0002          TWQ DC 2         RAW DATA.
007C 0 0003          XR4 DC 3         INDEX REGISTER FOR LOOP.
*****
* DISK DATA SUBROUTINE TO OBTAIN MORE DATA.
*****
007D 0 0000          MORDT DC *-+     SUBROUTINE TO GET
007E 01 C400015B     LD L ADC01     MORE DATA FROM DISK.
0080 01 D400005E     STO L LOAD1+1   RESET ADDRESSES OF LOADING
0082 01 D4000112     STO L LOAD2+1   OPERATION.
0084 01 C40006F9     LD L STDT1+1   UPDATE SECTOR ADDRESS.
0086 01 84000162     A L DEC6
0088 01 D40006F9     STO L STDT1+1
008A 20 04262495     LIBF     DISKN     CALL TO DISK FOR
008B 0 1000          DC      /1000     MORE DATA.
008C 1 06F8          DC      STDT1
008D 0 0000          DC      /0000
008E 20 04262495     LIBF     DISKN
008F 0 0100          DC      /0100
0090 1 06F8          DC      STDT1
0091 0 70FC          MDX     *-4
0092 01 4C80007D     BSC J MORDT     END SUBROUTINE.
*****
0094 01 65800158     COMPT LDX 11 TNPTS   LOAD INDEX REGISTERS
0096 01 66800159     LDX 12 MNPTS   TO SCALE THE DATA.
0098 01 C00002A8     LDD01 LDD L1 AREAC
009A 01 AC000168     D L WAVES
009C 01 D40005B8     STOR2 STO L CBQCD+2   UNSCALED SIGNAL AVERAGED
009E 01 7401009D     MDX L STOR2+1,1   RESULT STORED IN FIL27
00A0 0 7102          MDX 1 +2         RESULT STORED BACK INTO
00A1 0 1000          NOP AREAC.
00A2 0 7201          MDX 2 +1
00A3 0 70F4          MDX LDD01
00A4 01 74FF007C     MDX L XR4,-1   DECREMENT OF INDEX REG.
00A6 0 7001          MDX LUCKY        FOR LOOP COUNTER.
00A7 0 701B          MDX LOOP4

```

00A8	01	C400007C	LUCKY	LD	L	XR4	
00A8	01	0800007B		CHP	L	TWO	
00AD	0	7008		MDX		LOOP4	
00AE	0	7000		MDX		LOOP3	
00AF	01	C4000E7B	LOOP2	LD	L	STD2+1	SET UP SECTOR ADDRESS FOR
00B1	01	D40006F9		STO	L	STD1+1	CHANNEL 2.
00B3	01	C400015B		LD	L	ADCO1	CHANNEL2 & RESET LOAD
00B5	01	D400005E		STO	L	LOAD1+1	INSTRUCTION.
00B7	01	C4000012		BSC	L	LOOP1	GO BACK TO OPERATE ON
00B9	01	C4000E7E	LOOP3	LD	L	STD3+1	CHANNEL 2 & GET SUM. OF CHAN.3.
00BB	01	D40006F9		STO	L	STD1+1	
00BD	01	C400015B		LD	L	ADCO1	
00BF	01	D400005E		STO	L	LOAD1+1	
00C1	01	C4000012		BSC	L	LOOP1	GO BACK TO OPERATE ON
00C3	01	C400007A	LOOP4	LD	L	SECSV	CHANNEL 3.
00C5	01	D40006F9		STO	L	STD1+1	SAVE SECTOR ADDRESS FOR
00C7	01	7403007C		MDX	L	XR4.3	CHANNEL1.
00C9	0	C005		LD		CONST	SAVE SECTOR ADDRESS FOR
00CA	01	D40005B6		STO	L	CB3CD	CB3CD.
00CC	20	04262495		LIBF		DISKN	STORE UNSCALED SIGNAL
00CD	0	3000		DC		/3000	AVERAGED DATA (AREAE)
00CE	1	0586		DC		CB3CD	INTO DISK.
00CF	0	0140	CONST	DC		320	
00D0	20	04262495		LIBF		DISKN	
00D1	0	0100		DC		/0100	
00D2	1	0586		DC		CB3CD	
00D3	0	70FC		MDX		*-4	
00D4	01	C4000168	INDEX	LD	L	WAVES	
00D6	01	D400015A		STO	L	NUMBER	
00D8	01	C400007C		LD	L	XR4	LOAD INDEX REGISTER TO
00DA	01	D400007B		CHP	L	TWO	CHECK THE LOOP STEP.
00DC	0	7028		MDX		READF	
00DD	0	7014		MDX		LOOPB	
00DE	01	C4000E7B	LOOPA	LD	L	STD2+1	LOAD & STORE THE DATA OF
00E0	01	D40006F9		STO	L	STD1+1	CHANNEL 2 & CHANGE ADDRESS
00E2	01	C4000114		LD	L	SUBCP+1	
00E4	01	84000167		A	L	PONTS	
00E6	01	D4000114		STO	L	SUBCP+1	
00E8	01	C400015B		LD	L	ADCO1	
00EA	01	D4000112		STO	L	LOAD2+1	
00EC	0	C02F		LD		ADD2+1	MODIFY ADDRESS FOR
00ED	01	94000158		S	L	TNPTS	ACCUMULATION & MANIPULATION
00EF	0	D02C		STO		ADD2+1	OF DATA.
00F0	0	D02D		STO		ADD2+3	
00F1	0	7013		MDX		READF	
00F2	01	C4000E7E	LOOPB	LD	L	STD3+1	LOAD & STORE THE DATA OF
00F4	01	D40006F9		STO	L	STD1+1	CHANNEL 3 & CHANGE ADDRESS.
00F6	01	C4000114		LD	L	SUBCP+1	
00F8	01	84000167		A	L	PONTS	
00FA	01	D4000114		STO	L	SUBCP+1	
00FC	01	C400015B		LD	L	ADCO1	
00FE	01	D4000112		STO	L	LOAD2+1	
0100	0	C01B		LD		ADD2+1	MODIFY ADDRESS FOR
0101	01	94000158		S	L	TNPTS	ACCUMULATION & MANIPULATION
0103	0	D018		STO		ADD2+1	OF DATA.
0104	0	D019		STO		ADD2+3	
0105	20	04262495	READF	LIBF		DISKN	READ OUT THE SET OF DATA
0106	0	1000		DC		/1000	STORED ON DISK.
0107	1	06F8		DC		STD1	
0108	0	0000		DC		/0000	
0109	20	04262495		LIBF		DISKN	
010A	0	0100		DC		/0100	
010B	1	06F8		DC		STD1	
010C	0	70FC		MDX		*-4	
010D	01	G5800158	AGANI	LNX	11	TNPTS	LOAD INDEX REGISTER TO

010F 01 66800159		LDX	I2	MNPTS	BEGIN SIGNAL AVERAGING.
0111 01 C40000EFA	LOAD2	LD	L	STD1+2	LOAD FROM DISK AREA.
0113 01 960000568	SUBCP	S	L2	AREAE-1	SUBTRACT UNSCALED MEAN
0115 01 A400015C		M	L	SCALE	RAW DATA & MEAN VALUE.
0117 01 D4000078		STO	L	TEMP	
0119 01 A4000078		M	L	TEMP	
011B 01 80000374	ADD2	AD	L1	AREAD-1	
011D 01 D0000374		STD	L1	AREAD-1	
011F 01 74010112		MDX	L	LOAD2+1,1	MODIFY ADDRESS.
0121 0 C0F0		LD		LOAD2+1	CHECK FOR END OF DATA BLOCK
0122 01 9400015B		S	L	ADCO1	
0124 01 B4000157		CHP	L	WDCHT	
0126 0 7001		MDX		DATA1	MORE DATA REQUIRED.
0127 0 7002		MDX		MCHP1	MORE COMPUTATIONS.
0128 01 4400007D	DATA1	BSI	L	WORDT	
012A 0 7201	MCHP1	MDX	2	1	DECREMENT XR2.
012B 0 1000		NOP			
012C 0 7102		MDX	1	+2	DECREMENT XR1.
012D 0 70E3		MDX		LOAD2	GO BACK FOR MORE DATA.
012E 01 74FF015A		MDX	L	NUMBR,-1	DECREMENT NO. OF WAVES.
0130 0 70DC		MDX		AGAH1	GET ANOTHER WAVE SET.
0131 01 74FF007C		MDX	L	XR4,-1	
0133 0 7001		MDX		LOOPZ	
0134 0 7002		MDX		LAST	
0135 01 4C0000D4	LOOPZ	BSC	L	INDEX	
0137 01 C400013E	LAST	LD	L	WORDC	
0139 01 D4000372		STO	L	CPVST	RANDOM COMPONENT OF THE
013B 20 04262495		LIBF		DISKN	CONC. FLUCTL TO DISK.
013C 0 3000		DC		/3000	
013D 1 0372		DC		CPVST	
013E 0 0240	WORDC	DC		576	
013F 20 04262495		LIBF		DISKN	
0140 0 0100		DC		/0100	
0141 1 0372		DC		CPVST	
0142 0 70FC		MDX		*-4	
0143 20 04262495		LIBF		DISKN	READ IN ALL INFORMATIONS
0144 0 3000		DC		/3000	OF CONSTANTS ONTO INFORM.
0145 1 0163		DC		INFORM	
0146 0 0000		DC		/0000	
0147 20 04262495		LIBF		DISKN	
0148 0 0100		DC		/0100	
0149 1 0163		DC		INFORM	
014A 0 70FC		MDX		*-4	
014B 01 0C000150		XIO	L	LITOF	
014D 30 25241600		CALL		VIAQ	
0150 0000		BSS	E	0	
0150 1 0155	LITOF	DC		OFF	
0151 0 617D		DC		/617D	
0152 1 0154	LITON	DC		ON	
0153 0 617D		DC		/617D	
0154 0 0200	ON	DC		/0200	
0155 0 0000	OFF	DC		/0000	
0156 0 0008	EIGHT	DC		8	
0157 0 0780	WDCHT	DC		1920	WORD COUNT - READ IN DATA.
0158 0 0000	THPTS	DC		*-*	MINUS TWICE NO. OF PTS.
0159 0 0000	MNPTS	DC		*-A*	MINUS NO. OF PTS.
015A 0 0000	NUMBR	DC		*-*	NBR. OF WAVES.
015B 1 06FA	ADCO1	DC		STD1+2	ADDR. CHECK ON ENOUGH DATA.
015C 0 2717	SCALE	DC		10007	SCALING COEF.
015D 0003	DVSEP	BSS		3	
0160 0 0000	AVRGE	DC		*-*	
0162 0 0000		BSS	E	0	
0162 0 0006	DEC6	DC		6	
0163 31 06253CB0	INFORM	DSA		FIL20	INFORMATION STORED ON DISK.
0166 0 FF80	DELAY	DC		-80	DELAY TIME.
0167 0 0060	PONTS	DC		96	NUMBER OF POINTS ON A WAVE.

0168	0	0064	WAVES	DC	100	NUMBER OF WAVES.
0168	0	0000	CLICK	DC	96	LOCATION OF RUN NUMBER.
01CA	0003		AREAF	BSS	3	DISK AREA.
01CD	0003		AREAG	BSS	3	
01DD	0008		AREAH	BSS	216	
02A8	00C8		AREAC	BSS	E 200	SCALED.
0370	0	0140	DE320	DC	320	CONSTANT.
0372	0000			BSS	E 0	
0372	31	06253CB2	CPVST	DSA	FIL22	USES FIL22 AND FIL23
0375	0240		AREAD	BSS	576	
0586	0000			BSS	E 0	
05B6	31	06253CB7	CRJCD	DSA	FIL27	STORAGE OF UNSCALED SIGNAL
05B9	013F		AREAC	BSS	319	AVERAGED RESULT.
06F8	31	06253C33	STD1	DSA	FIL03	SEDIMENT CONCENTRATION.
06FB	077F			BSS	1919	
0E7A	31	06253C34	STD2	DSA	FIL04	HORIZONTAL VELOCITY COMPONENT.
0E7D	31	06253C35	STD3	DSA	FIL05	VERTICAL VELOCITY COMPONENT.
0E80	0	0009	DEC9	DC	9	
0E81	0	0019	DEC25	DC	25	
0E82	0006		INPUT	BSS	6	
0E88	0000		END		START	

NO ERRORS IN ABOVE ASSEMBLY.

COMPT

DUP FUNCTION COMPLETED

// JOB 0000011111

// END OF ALL JOBS

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```
// JOB 0000011111
// ASM CHANG
*.LIST
```

```
*****
*                                     *
* THIS PROCESS PROGRAM IS CALLED BY A CALL SPECIF *
* FROM THE SIGNAL AVERAGING PROGRAM ASSV3 *
* AND ALLOWS THE USER TO CHANGE PROGRAM *
* CONSTANTS. THESE CONSTANTS ARE THE NUMBER OF *
* WAVES TO BE SAMPLED, THE NUMBER OF POINTS *
* PER WAVE, THE DELAY TIME IN MS BETWEEN DATA *
* POINTS, THE MIN VALUE IN MW, THE MAX *
* DIFFERENCE IN MW AND THE NUMBER LIMIT OF *
* ALLOWED BAD POINTS TO TEST THE LOG-TRACKER. ALL *
* ENTRIES ARE MADE THROUGH THE DATA ENTRY *
* SWITCHES AND AN ECHO CHECK IS PRINTED. *
*****
```

0000	20	23A17155	START	LINE	TYPEH	INTRODUCTORY MESSAGE.
0001	0	2002		DC	/2002	
0002	1	02FC		DC	DMES9-1	
0003	0	0000		DC	0	
0004	20	23A17155		LINE	TYPEH	
0005	0	0002		DC	/0002	
0006	0	70FD		MDX	*-3	
0007	20	23A17155		LINE	TYPEH	
0008	0	2002		DC	/2002	AT PAUSE ENTER THE NUMBER
0009	1	01FF		DC	DMES1-1	OF WAVES TO BE SAMPLED.
000A	0	0000		DC	0	
000B	20	23A17155		LINE	TYPEH	
000C	0	0002		DC	/0002	
000D	0	70FD		MDX	*-3	
000E	01	0A000000		LD	L AREA	
0010	01	0A000000		STO	I INFO	
0012	20	0A262695		LINE	DISKN	READ IN THE AREA FROM DISK
0013	0	1000		DC	/1000	
0014	1	0000		DC	INFO	
0015	0	0000		DC	0	
0016	20	0A262695		LINE	DISKN	ONLY THE FIRST 3 WORDS
0017	0	0100		DC	/0100	IN THE AREA WILL BE CHANGED.
0018	1	0000		DC	INFO	
0019	0	70FD		MDX	*-3	
001A	20	17064085		LINE	PAUSE	PROGRAMMED WAIT
001B	1	02F2		DC	ONE	
001C	01	0C00000A		XIO	L 100CA	READ CONTENTS OF DES. TO WA VES
001E	20	23A17155		LINE	TYPEH	ECHO CHECK ON THE NUMBER
001F	0	2002		DC	/2002	OF WAVES ENTERED.
0020	1	022A		DC	DMES2-1	
0021	0	0000		DC	0	
0022	20	23A17155		LINE	TYPEH	
0023	0	0002		DC	/0002	
0024	0	70FD		MDX	*-3	
0025	01	0A000001		LD	L WAVES	
0027	01	4A000200		STI	L PRINT	
0029	20	23A17155		LINE	TYPEH	MESSAGE TO ENTER THE
002A	0	2002		DC	/2002	NUMBER OF DATA POINTS
002B	1	0237		DC	DMES3-1	
002C	0	0000		DC	0	
002D	20	23A17155		LINE	TYPEH	
002F	0	0002		DC	/0002	
002F	0	70FD		MDX	*-3	
0030	20	17064085		LINE	PAUSE	WAIT TO ENTER VIA DES.
0031	1	02F3		DC	TWO	
0032	0	0C79		XIO	10000	READ DES TO POINTS
0033	20	23A17155		LINE	TYPEH	ECHO CHECK ON THE NUMBER

0034 0 2002	DC	/2002	OF POINTS ENTERED.
0035 1 0258	DC	DME54-1	
0036 0 0000	DC	0	
0037 20 23A17155	LICF	TYPEH	
0038 0 0002	DC	/0002	
0039 0 70F0	MOX	*-3	
003A 01 C6000000	LD	L	POINTS
003B 01 44000200	BSI	L	PRINT
003C 20 23A17155	LICF	TYPEH	MESSAGE TO ENTER THE DELAY
003D 0 2002	DC	/2002	TIME VIA DES.
0040 1 0250	DC	DME55-1	
0041 0 0000	DC	0	
0042 20 23A17155	LICF	TYPEH	
0043 0 0002	DC	/0002	
0044 0 70F0	MOX	*-3	
0045 20 17064005	LICF	PAUSE	WAIT TO ENTER INFORMATION.
0046 1 02F4	DC	THREE	
0047 0 0000	XIO	10000	READ DES. TO DELAY
0048 20 23A17155	LICF	TYPEH	ENTER CHECK ON THE NUMBER
0049 0 2002	DC	/2002	OF MILLISECONDS DELAY TIME.
004A 1 02C9	DC	DME56-1	
004B 0 0000	DC	0	
004C 20 23A17155	LICF	TYPEH	
004D 0 0002	DC	/0002	
004E 0 70F0	MOX	*-3	
004F 0 0000	LD	DELAY	
0050 01 44000200	BSI	L	PRINT
0051 0 1010	SLA	16	ZERO A REG
0052 0 0000	S	DELAY	A REG. CONTAINS MINUS DELAY
0053 0 1003	SLA	3	MULTIPLY BY 3
0054 0 0000	STO	DELAY	STORE IN DELAY
0055 20 23A17155	LICF	TYPEH	READ IN NO
0056 0 2002	DC	/2002	
0057 1 0275	DC	DME10-1	
0058 0 0000	DC	0	
0059 20 23A17155	LICF	TYPEH	
005A 0 0002	DC	/0002	
005B 0 70F0	MOX	*-3	
005C 20 17064005	LICF	PAUSE	
005D 1 02F5	DC	FOUR	
005E 0 0050	XIO	10000	
005F 20 23A17155	LICF	TYPEH	
0060 0 2002	DC	/2002	
0061 1 02A5	DC	DME13-1	
0062 0 0300	DC	0	
0063 20 23A17155	LICF	TYPEH	
0064 0 0002	DC	/0002	
0065 0 70F0	MOX	*-3	
0066 01 C6000000	LD	L	NO
0067 01 44000200	BSI	L	PRINT
0068 01 C6000000	LD	L	NO
0069 0 1004	SLA	4	MULTIPLY BY 16
006A 01 C6000000	STO	L	NO
006B 20 23A17155	LICF	TYPEH	READ IN NO
006C 0 2002	DC	/2002	
006D 1 0255	DC	DME11-1	
006E 0 0000	DC	0	
006F 20 23A17155	LICF	TYPEH	
0070 0 0002	DC	/0002	
0071 0 70F0	MOX	*-3	
0072 20 17064005	LICF	PAUSE	
0073 1 02F6	DC	FIVE	
0074 0 0030	XIO	10000	
0075 20 23A17155	LICF	TYPEH	
0076 0 2002	DC	/2002	
0077 1 02F1	DC	DME14-1	

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0070	0	0000	DC	0	
0071	20	23A17155	LICF	TYPER	
0072	0	0002	DC	/0002	
0080	0	70F0	MDX	*-3	
0081	01	64000004	LD	L	U1
0083	01	64000202	BSI	L	PRINT
0085	01	64000004	LD	L	U1
0087	0	1004	SIA	4	MULTIPLY BY 16
0088	01	64000004	STO	L	U1
008A	20	23A17155	LICF	TYPER	READ IN LIMIT
008B	0	2002	DC	/2002	
008C	1	020F	DC	DHF12-1	
008D	0	0000	DC	0	
008F	20	23A17155	LICF	TYPER	
008F	0	0002	DC	/0002	
0090	0	70F0	MDX	*-3	
0091	20	170F4005	LICF	PAUSE	
0092	1	0207	DC	SIX	
0093	0	0000	XIO	INCR	
0094	20	23A17155	LICF	TYPER	
0095	0	2002	DC	/2002	
0096	1	0200	DC	DHF15-1	
0097	0	0000	DC	0	
0098	20	23A17155	LICF	TYPER	
0099	0	0002	DC	/0002	
009A	0	70F0	MDX	*-3	
009B	01	64000005	LD	L	LIMIT
009C	01	64000202	BSI	L	PRINT
009F	20	04262495	LICF	DISKN	READ OUT ONTO DISK
00A0	0	3001	DC	/3000	
00A1	1	0000	DC	TYPER	
00A2	0	0000	DC	/0000	
00A3	20	04262495	LICF	DISKN	
00A4	0	0100	DC	/0100	
00A5	1	0000	DC	INCR	
00A6	0	70F0	MDX	*-4	
00A7	30	02063600	CALL	BACK	
00A8	0	0000	BSI	F	0
00A9	1	0001	LOGGA	DC	WAVES
00AB	0	0240	DC	/0240	READ DES TO LOC. WAVES
00AC	1	0000	LOGGB	DC	POINTS
00AD	0	0240	DC	/0240	READ DES. TO NO. OF PTS.
00AE	1	0000	LOGGA	DC	DELAY
00AF	0	0240	DC	/0240	READ DES. DELAY TIME.
00B0	1	0003	LOGGB	DC	NO
00B1	0	0240	DC	/0240	READ DES TO LOC. NO
00B2	1	0004	LOGGE	DC	U1
00B3	0	0240	DC	/0240	READ DES TO LOC. U1
00B4	1	0005	LOGGE	DC	LIMIT
00B5	0	0240	DC	/0240	READ DES TO LOC. LIMIT
00B6	0	0000	DATSW	DC	/0000
00B7	0	0740	DC	/0740	
00B8	0	0140	AREA	DC	320
00B9	31	06253000	FILE	DATA	FIL20
00BC	31	06253000	INCR	DATA	FIL20
00BF	0	0000	DELAY	DC	***
00C0	0	0000	POINTS	DC	***
00C1	0	0000	WAVES	DC	***
00C2	0	0000	CLICK	DC	***
00C3	0	0000	U0	DC	***
00C4	0	0000	U1	DC	***
00C5	0	0000	LIMIT	DC	***
00C6	0	0130	BSI		313
01FF	0	002A	DC		DHF12-DHF15
0200	0	0020	DHF1	DHF5	IDENTITY OF CONSTANTS FOR SIGNAL
0210	0	0012	DHF5		AVERAGING PROGRAM, 15

0210	0022	DMES	ENTERED NUMBER OF WAVES AT PAUSE 1, 'E
0222	0000	DMES2 RES	0
0222	0018	DMES2 DMES	DMESX-DMES2
0237	0000	DMESX RES	2RTIME NO. OF WAVES IS 'E
0237	0010	DC	0
0237	0010	DC	DMESX-DMES3
0248	0000	DMES3 DMES	2RTIME ENTER NO. OF DATA POINTS, 'E
0248	000F	DMESX RES	0
0248	001F	DC	DMESX-DMES4
0249	001F	DMES4 DMES	2RTIME NO. OF DATA POINTS IS 'E
0258	0000	DMESU RES	0
0258	0010	DC	DMESU-DMES5
0259	0020	DMES5 DMES	2RTIME ENTER DELAY TIME IN MSEC, 'E
0269	0000	DMESU RES	0
0269	000F	DC	DMESU-DMES6
026A	0016	DMES6 DMES	2RTIME DELAY TIME IS 'E
0275	0000	DMESV RES	0
0275	000F	DC	DMESV-DMES10
0276	001F	DMES10 DMES	2RTIME ENTER MIN. VAL. NO IN IV, 'E
0285	0000	DMESV RES	0
0285	0010	DC	DMESV-DMES11
0286	0020	DMES11 DMES	2RTIME ENTER MAX. DIFF. UI IN HV, 'E
0286	0000	DMES0 RES	0
0286	000F	DC	DMES0-DMES12
0287	0010	DMES12 DMES	2RTIME ENTER LIMIT OF BAD PT., 'E
0287	0000	DMES0 RES	0
0287	000F	DC	DMES0-DMES13
0288	0016	DMES13 DMES	2RTIME MIN. VALUE NO IS 'E
0288	0000	DMES0 RES	0
0288	000F	DC	DMES0-DMES14
0289	001F	DMES14 DMES	2RTIME MAX. DIFF. UI IS 'E
0289	0000	DMES0 RES	0
0289	000F	DC	DMES0-DMES15
028F	001A	DMES15 DMES	2RTIME LIMIT OF BAD PT. IS 'E
028F	0000	DMESV RES	0
028F	0000	PRINT DC	*** PRINTING SUBROUTINE
028F	20	02255103	LINE BINARY TO DECIMAL
028F	1	0220	DC BINARY
028F	20	08503500	LINE HOLLER
028F	0	0000	DC /0000
028F	1	0220	DC BINARY
028F	1	0250	DC PTOUT
028F	0	0000	DC 6
028F	20	25A17155	LINE TYPEIN PRINT OUT NUMBER
028F	0	2002	DC /2002
028F	1	0258	DC PTOUT-1
028F	0	0000	DC /0000
028F	20	25A17155	LINE TYPEIN
028F	0	0002	DC /0002
028F	0	70F0	DC *-3
028F	01	40F00200	DC 1 PRINT END OF SUBROUTINE PRINT
028F	0006	BHOUT BSS	6
028F	0001	ONE DC	1
028F	0002	TWO DC	2
028F	0003	THREE DC	3
028F	0004	FOUR DC	4
028F	0005	FIVE DC	5
028F	0006	SIX DC	6
028F	0003	DC	3
028F	0003	PTOUT BSS	3
028F	0012	DC	DMES0-DMES0
028F	14.093 02	1442 NOT READY 0010	DMES0 DMES 20'AAC03'B CONST
028F	0006	DMES	MODIFIED'E
028F	0000	DMESR RES	0

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0300 0000 END START
NO ERRORS IN ABOVE ASSEMBLY.
CHANG
DUP FUNCTION COMPLETED

// JOB 0000011111

// ASM CNVRT

*LIST

```

*****
*      PROGRAM : CNVRT      *
*  THIS PROGRAM CONVERTS THE DATA IN MV. TO      *
*  (PPM) FOR CHANNEL 1 (SEDIMENT CONCENTRATION)  *
*  AND 1000*(FT/S) FOR CHANNEL 3 (VERTICAL VELOCIT *
*  Y) THROUGH THE SCALING PROCEDURE.              *
*  PROGRAMED BY LOCHER AND NAKATO                  *
*****
0000 01 C400013C  START LD  L  DEC10  SET UP WORD COUNT TO
0002 01 D4000204  STO  L  INFOM  GET INFORMATION
0004 20 04262495  LIBF  DISKN  READ FIL20
0005 0 1000  DC  /1000
0006 1 0204  DC  INFOM
0007 0 0140  WDCNT DC  320
0008 20 04262495  LIBF  DISKN
0009 0 0100  DC  /0100
000A 1 0204  DC  INFOM
000B 0 70FC  MDX  *-4
000C 0 C0FA  LD  WDCNT  LOAD WORD COUNT ON FIL27
000D 01 D4000346  STO  L  CB@CD
000F 20 04262495  LIBF  DISKN  READ FIL27 TO GET UNSCALED
0010 0 1000  DC  /1000  (MEAN + PERIODIC)
0011 1 0346  DC  CB@CD
0012 0 0000  DC  /0000
0013 20 04262495  LIBF  DISKN
0014 0 0100  DC  /0100
0015 1 0346  DC  CB@CD
0016 0 70FC  MDX  *-4
0017 01 C4000208  LD  L  PONTS
0019 0 1001  SLA  1
001A 01 D4000140  STO  L  TNPTS
001C 0 1010  SLA  16  SET UP ZERO IN A-REG.
001D 01 94000208  S  L  PONTS  SUBTRACT NO. OF PTS.
001F 01 D400013F  STO  L  MNPTS  MINUS NO. OF PONTS
0021 01 6580013F  LDX  11 MNPTS  DO LOOP FOR CHANNEL1
0023 01 C4000348  LOOP1 LD  L  AREA-1  LOAD (MEAN + PERI)
0025 01 84000142  A  L  ZERO1  ADD UNSCALED ZERO VOLY
0027 01 A4000143  M  L  SCALE  SCALING
0029 01 D4000144  ARRAG STO  L  AREAG
002B 01 74010024  MDX  L  LOOP1+1,1
002D 01 7401002A  MDX  L  ARRAG+1,1
002F 0 7101  MDX  1 1  INCREASE INDEX REG.1 BY 1
0030 0 70F2  MDX  LOOP1  GO TO LOOP1
0031 0 C0F2  LD  LOOP1+1
0032 01 94000208  S  L  PONTS
0034 0 D0EF  STO  LOOP1+1
0035 0 C0F4  LD  ARRAG+1
0036 01 94000208  S  L  PONTS
0038 0 D0F1  STO  ARRAG+1
0039 01 C4000488  LD  L  ADRE  CALCUL. ADRESS 3.CH.
003B 01 84000140  A  L  TNPTS
003D 01 9400013A  S  L  DEC1
003F 0 D003  STO  LOOP2+1
0040 01 6680013F  LDX  12 MNPTS  DO LOOP FOR CHANNEL 3
0042 00 C4000000  LOOP2 LD  L  *-  LOAD MEAN + PERIODIC
0044 01 A4000143  M  L  SCALE
0046 01 D40001A4  ARRAH STO  L  AREAH
0048 01 74010043  MDX  L  LOOP2+1,1
004A 01 74010047  MDX  L  ARRAH+1,1
004C 0 7201  MDX  2 1  RAISE INDEX REG.2 BY 1
004D 0 70F4  MDX  LOOP2

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004E	0	COF7		LD	ARRAH	
004F	01	94000208		S	L	PONTS
0051	0	D0F5		STO	ARRAH+1	
0052	20	23A17171		LIBF	TYPE1	PRINT RUNNO
0053	1	020A		DC	CLICK	
0054	0	0001		DC	1	
0055	01	0C0000E4		XIO	L	IOCCA
0057	01	E40000E7		AND	L	MASC2
0059	0	4820		BSC	Z	SKIP IF DES 2 IS NOT SET
005A	0	700D		MDX	SKIPP	SKIPP OUTPUT CHANNEL 1
005B	20	26663A15		LIBF	WRTYN	WRITE MESSAGE FOR SEDIMENT
005C	0	2001		DC	/2001	
005D	1	0489		DC	DMES1-1	
005E	0	0000		DC	/0000	
005F	20	26663A15		LIBF	WRTYN	
0060	0	0001		DC	/0001	
0061	0	70FD		MDX	*-3	
0062	01	C4000208		LD	L	PONTS
0064	0	D002		STO	NOP	
0065	20	23A17171		LIBF	TYPE1	TYPE OUT SED. CONCENTRATION
0066	1	0144		DC	AREAG	IN PPM UNIT
0067	0	0000	NOP	DC	**	
0068	20	26663A15	SKIPP	LIBF	WRTYN	WRITE MESSAGE FOR V-COMP
0069	0	2001		DC	/2001	
006A	1	049A		DC	DMES2-1	
006B	0	0000		DC	/0000	
006C	20	26663A15		LIBF	WRTYN	
006D	0	0001		DC	/0001	
006E	0	70FD		MDX	*-3	
006F	01	C4000208		LD	L	PONTS
0071	0	D002		STO	NNOP	
0072	20	23A17171		LIBF	TYPE1	TYPE OUT V-COMP.
0073	1	01A4		DC	AREAH	IN 1000*(FT/S) UNIT
0074	0	0000	NNOP	DC	*-A*	
0075	01	0C0000E4		XIO	L	IOCCA
0077	01	E40000E6		AND	L	MASC
0079	0	4808		BSC	+	
007A	0	7067		MDX	OUT	
007B	20	03059115		LIBF	CARDN	FEEDS 1 CARD
007C	0	3000		DC	/3000	
007D	0	0000		DC	0	
007E	20	03059115		LIBF	CARDN	
007F	0	0000		DC	/0000	
0080	0	70FD		MDX	*-3	
0081	01	C400020A		LD	L	CLICK
0083	20	02255103		LIBF	BINDC	PUNCH RUNNO
0084	1	00E9		DC	OUTPT	
0085	01	C4000209		LD	L	WAVES
0087	20	02255103		LIBF	BINDC	PUNCH NO OF WAVES
0088	1	00EF		DC	OUTPT+6	
0089	01	C400013D		LD	L	DEC12
008B	0	D05C		STO	AREA	
008C	20	03059115		LIBF	CARDN	
008D	0	2000		DC	/2000	
008E	1	00E8		DC	AREA	
008F	0	0000		DC	0	
0090	20	03059115		LIBF	CARDN	
0091	0	0000		DC	/0000	
0092	0	70FD		MDX	*-3	
0093	01	C400013E		LD	L	DEC72
0095	0	D052		STO	AREA	PUNCH MEAN AND
0096	01	65800208		LDX	11	PERIODIC ON CARDS
0098	0	620C	PUNCH	LDX	2	12
0099	01	C40001A4	CONV	LD	L	AREAH
009B	20	02255103		LIBF	BINDC	12 VALUES PER CARD
009C	1	00E9	OTP	DC	OUTPT	

009D	01	7406009C	MDX	L	OTP,6	FIELD FOR NEXT VALUE
009E	01	7401009A	MDX	L	CONV+1,1	NEXT VALUE.
00A1	0	72FF	MDX	2	-1	
00A2	0	70F6	MDX		CONV	
00A3	20	03059115	LIBF		CARDN	
00A4	0	2000	DC		/2000	
00A5	1	00E8	DC		AREA	
00A6	0	0000	DC		0	
00A7	20	03059115	LIBF		CARDN	
00A8	0	0000	DC		/0000	
00A9	0	70FD	MDX		*-3	
00AA	01	74E8009C	MDX	L	OTP,-72	RESTORES 1. OUTPUT AD.
00AC	0	71F4	MDX	1	-12	
00AD	0	70EA	MDX		PUNCH	
00AE	01	C4000208	LD	L	PONTS	PRINTOUT OF REST
00B0	0	1890	SRT		16	
00B1	01	AC00013D	D	L	DEC12	
00B3	0	1090	SLT		16	
00B4	01	B4000139	CHP	L	ZERO	
00B6	0	7002	MDX		GOON	
00B7	0	7024	MDX		RSTOR	
00B8	0	7023	MDX		RSTOR	
00B9	01	D4000141	GOON	STO	L	REST
00BB	01	A400013B	M	L	DEC6	
00BD	0	1090	SLT		16	
00BE	01	D40000E8	STO	L	AREA	
00C0	0	C0D9	LD		CONV+1	SET ADDRESS IN AREA H
00C1	0	D006	STO		CONVV+1	
00C2	01	84000141	A	L	REST	
00C4	0	D0D5	STO		CONVV+1	
00C5	01	66800141	LDX	12	REST	
00C7	00	C4000000	CONVV	LD	L	*-*
00C9	20	02255103	LIBF		BINDC	
00CA	1	00E9	OTTP	DC	OUTPT	
00CB	01	740600CA	MDX	L	OTTP,6	
00CD	01	740100C8	MDX	L	CONVV+1,1	
00CF	0	72FF	MDX	2	-1	
00D0	0	70F6	MDX		CONVV	
00D1	20	03059115	LIBF		CARDN	
00D2	0	2000	DC		/2000	
00D3	1	00E8	DC		AREA	
00D4	0	0000	DC		0	
00D5	20	03059115	LIBF		CARDN	
00D6	0	0000	DC		/0000	
00D7	0	70FD	MDX		*-3	
00D8	0	C0F1	LD		OTTP	RESTORES OTTP
00D9	01	940000E8	S	L	AREA	
00DB	0	D0EE	STO		OTTP	
00DC	01	C400009A	RSTOR	LD	L	CONV+1
00DE	01	94000208	S	L	PONTS	RESTORES ADR. IN CONV+1
00E0	01	D400009A	STO	L	CONV+1	
00E2	30	059C98C0	OUT	CALL	EXIT	
00E4	0	0000	BSS	E	0	
00E4	0	0000	IOCCA	DC	/0000	READ DATA ENTRY SW.
00E5	0	0740	DC		/0740	
00E6	0	0001	MASC	DC	/0001	
00E7	0	0002	MASC2	DC	/0002	MASK FOR DES 2
00E8	0	0000	AREA	DC	*-A*	OUTPUT AREA FOR CARDS
00E9	0050		OUTPT	BSS	80	
0139	0	0000	ZERO	DC	0	
013A	0	0001	DEC1	DC	1	
013B	0	0006	DEC6	DC	6	
013C	0	0068	DEC10	DC	104	
013D	0	000C	DEC12	DC	12	
013E	0	0048	DEC72	DC	72	
013F	0	0000	PNPTS	DC	*-*	

0140	0	0000	TNPTS	DC	***	
0141	0	0000	REST	DC	***	
0142	0	0000	ZERO1	DC	0	ZERO SHIFT CHAN.1
0143	0	2717	SCALE	DC	10007	
0144		0060	AREAG	BSS	96	PPM FOR SED. CONC.
01A4		0060	AREAH	BSS	96	1000*(FT/S)FOR V-COMP.
0204	31	06253CB0	INFOM	DSA	FIL20	
0207	0	0000	DELAY	DC	***	
0208	0	0000	POINTS	DC	***	
0209	0	0000	WAVES	DC	***	
020A	0	0000	CLICK	DC	***	
020B		0060	AREAB	BSS	96	
0260		00DB	AREAF	BSS	219	
0346	31	06253CB7	CBQCD	DSA	FIL27	
0349		013F	AREAE	BSS	319	
0488	1	0349	ADRE	DC	AREAE	
0489	0	0010		DC	DMESA-DMES1	
048A		000B	DMES1	DMES	'2R'PRESSURE	
048F		0013		DMES	(MEAN AND PERIODIC)'E	
0499	0	8105		DC	/8105	
049A		0000	DMESA	BES	0	
049B	0	0015		DC	DMESD-DMES2	
049B		0014	DMES2	DMES	'2R'VELOCITY COMPONENT	
04A5		0014		DMES	(MEAN AND PERIODIC)'E	
04AF	0	8105		DC	/8105	
04B0		0000	DMESB	BES	0	
04B0		0000		END	START	

NO ERRORS IN ABOVE ASSEMBLY.

CONVRT

DUP FUNCTION COMPLETED

// JOB 0000011111

// END OF ALL JOBS

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// JOB 0000011111
// ASM CONVT
*LIST
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*****
* PROGRAM : CONVT
* THIS PROGRAM CONVERTS VOLTAGE UNIT OF RANDOM
* FLUCTUATIONS FOR PRINTOUT, AND PUNCHES CARDS.
* DES1 UP : CARDS ARE PUNCHED
* DES2 UP : PRINTOUT CHANNEL 1 IS SUPRESSED
* PROGRAMMED BY A. MUELLER MARCH 1977
*****
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		START	LD	L	DEC9	LOAD WORD COUNT ON FIL20
0000	01	C400022C				
0002	01	D4000234	STO	L	INFOM	
0004	20	04262495	LIBF		DISKN	GET INFORMATION
0005	0	1000	DC		/1000	
0006	1	0234	DC		INFOM	
0007	0	0000	DC		/0000	
0008	20	04262495	LIBF		DISKN	
0009	0	0100	DC		/0100	
000A	1	0234	DC		INFOM	
000B	0	70FC	MDX		**4	
000C	01	C4000487	LD	L	WORDC	LOAD WORD COUNT ON FIL22
000F	01	D4000242	STO	L	CPVST	
0010	20	04262495	LIBF		DISKN	GET SQUARE VALUE OF
0011	0	1000	DC		/1000	RANDOM FLUCTUATION
0012	1	0242	DC		CPVST	
0013	0	0000	DC		/0000	
0014	20	04262495	LIBF		DISKN	
0015	0	0100	DC		/0100	
0016	1	0242	DC		CPVST	
0017	0	70FC	MDX		**4	
0018	0	1010	SLA		16	SET A REGISTER ZERO
0019	01	94000238	S	L	PONTS	
001B	01	D400022D	STO	L	MINPTS	MINUS NO. OF PONTS
001D	0	1001	SLA		1	MULTIPLY BY TWO
001E	01	D400022E	STO	L	TNPTS	-2* NO. OF PONTS
0020	0	1001	SLA		1	
0021	01	D400022F	STO	L	FNPTS	-4* NO. OF PONTS
0023	01	C4000239	LD	L	WAVES	
0025	0	1690	SRT		16	SET UP DOUBLE PRECISION
0026	30	051064E3	CALL		EDFLT	FLOAT NO. OF WAVES
0028	20	058A3580	LIBF		ESTO	STORE FLOATED WAVES
0029	1	0230	DC		DVSR	
002A	20	23A17171	LIBF		TYPE1	PRINT RUNNO
002B	1	023A	DC		CLICK	
002C	0	0001	DC		1	
002D	01	0C000112	XIO	L	IOCCA	READ DATA ENTRY SWITCH
002F	01	E4000115	AND	L	MASC2	TEST FOR SWITCH 2
0031	0	4820	BSC		Z	SKIP IF DES 2 IS NOT SET
0032	0	7037	MDX		SKIPP	SKIPP OUTPUT CHANNEL 1
0033	20	26663A15	LIBF		WRTYN	CARRAGE RETURN
0034	0	2001	DC		/2001	
0035	1	0488	DC		CARIG.	
0036	0	0000	DC		0	
0037	20	26663A15	LIBF		WRTYN	
0038	0	0001	DC		/0001	
0039	0	70FD	MDX		**3	
003A	20	26663A15	LIBF		WRTYN	
003B	0	2001	DC		/2001	
003C	1	0494	DC		DMES1-1	HEADING FOR CHANNEL 1
003D	0	0000	DC		0	
003E	20	26663A15	LIBF		WRTYN	
003F	0	0001	DC		/0001	
0040	1	003E	DC		**3	

0041	20	26663A15	LIBF	WRTYN	CARRAGE RETURN
0042	0	2001	DC	/2001	
0043	1	0488	DC	CARIG	
0044	0	0000	DC	0	
0045	20	26663A15	LIBF	WRTYN	
0046	0	0001	DC	/0001	
0047	0	70FD	MDX	*-3	
0048	01	6580022E	LDX	I1 TNPTS	SET UP INDEX REG. 1
004A	01	CC000244	LOOP1 LDD	L AREAD-1	LOOP FOR CHANNEL 1
004C	30	051064E3	CALL	EDFLT	FLOAT THE VALUE
004E	20	05109940	LIBF	EDIV	DEVIDE BY NO. OF WAVES
004F	1	0230	DC	DYSER	
0050	30	05898640	CALL	ESQR	TAKE SQUARE ROOT
0052	20	091899C0	LIBF	IFIX	CONVERT TO INTEGER
0053	01	D400016C	ADO	STO L AREAG	
0055	01	74010054	MDX	L ADO+1,1	
0057	01	7402004B	MDX	L LOOP1+1,2	
0059	0	7102	LOOPC MDX	1 2	
005A	0	70EF	MDX	LOOP1	
005B	01	C4000238	LD	L PONTs	
005D	0	0002	STO	NPON	
005E	20	23A17171	LIBF	TYPE1	PRINTOUT 1.CHANNEL
005F	1	016C	DC	AREAG	
0060	0	0000	NPON	DC	**
0061	0	C0F2	LD	ADO+1	RESTORES ADR. IN AREAG
0062	01	94000238	S	L PONTs	
0064	01	D4000054	STO	L ADO+1	
0066	0	C0E4	LD	LOOP1+1	
0067	01	8400022E	A	L TNPTS	
0069	0	D0E1	STO	LOOP1+1	
006A	20	26663A15	SKIPP	LIBF	CONVERSION CHANNEL 3
006B	0	2001	DC	/2001	
006C	1	0488	DC	CARIG	
006D	0	0000	DC	0	
006E	20	26663A15	LIBF	WRTYN	
006F	0	0001	DC	/0001	
0070	0	70FD.	MDX	*-3	
0071	20	26663A15	LIBF	WRTYN	HEADING FOR CHANNEL 3
0072	0	2001	DC	/2001	
0073	1	04A2	DC	DMES2-1	
0074	0	0000	DC	0	
0075	20	26663A15	LIBF	WRTYN	
0076	0	0001	DC	/0001	
0077	0	70FD	MDX	*-3	
0078	20	26663A15	LIBF	WRTYN	CARRAGE RETURN
0079	0	2001	DC	/2001	
007A	1	0488	DC	CARIG	
007B	0	0000	DC	0	
007C	20	26663A15	LIBF	WRTYN	
007D	0	0001	DC	/0001	
007E	0	70FD	MDX	*-3	
007F	01	6580022E.	LDX	I1 TNPTS	
0081	01	C4000485	LD	L ADRD	SETS ADR. FOR 3.CHANNEL
0083	01	9400022F	S	L FNPTS	
0085	01	94000486	S	L DEC1	
0087	0	D001	STO	LOOP2+1	
0088	00	CC000000	LOOP2 LDD	L **	LOOP FOR CHANNEL 3
008A	30	051064E3	CALL	EDFLT	FLOAT THE VALUE
008C	20	05109940	LIBF	EDIV	DIVISION ROUTINE
008D	1	0230	DC	DYSER.	
008E	30	05898640	CALL	ESQR	SQUARE ROOT
0090	20	091899C0	LIBF	IFIX	CONVERTS TO INTEGER
0091	01	D40001CC	AD1	STO L AREAH	FIELD FO INT. VALUE
0093	01	74010092	MDX	L AD1+1,1	
0095	01	74020089	MDX	L LOOP2+1,2	
0097	0	7102	LOOPB MDX	1 2	

0098	0	70EF	MDX	LOOP2	
0099	01	C4000238	LD	L	PONTS
009B	0	D002	STO		NPPON
009C	20	23A17171	LIBF	TYPE1	PRINTOUT 3.CHANNEL
009D	1	01CC	DC		AREAH
009E	0	0000	NPPON DC	**	
009F	0	C0F2	LD		AD1+1
00A0	01	94000238	S	L	PONTS
00A2	0	D0EF	STO		AD1+1
00A3	01	0C000112	XIO	L	IOCCA
00A5	01	E4000114	AND	L	MASC
00A7	0	4808	BSC		+
00A8	0	7066	MDX		OUT
00A9	20	03059115	LIBF		CARDN
00AA	0	3000	DC		/3000
00AB	0	0000	DC		0
00AC	20	03059115	LIBF		CARDN
00AD	0	0000	DC		/0000
00AE	0	70FD	MDX		*-3
00AF	01	C400023A	LD	L	CLICK
00B1	20	02255103	LIBF		BINDC
00B2	1	0117	DC		OTPUT
00B3	01	C4000239	LD	L	WAVES
00B5	20	02255103	LIBF		BINDC
00B6	1	011D	DC		OTPUT+6
00B7	01	C4000169	LD	L	DEC12
00B9	0	D05C	STO		AREA
00BA	20	03059115	LIBF		CARDN
00BB	0	2000	DC		/2000
00BC	1	0116	DC		AREA
00BD	0	0000	DC		0
00BE	20	03059115	LIBF		CARDN
00BF	0	0000	DC		/0000
00C0	0	70FD	MDX		*-3
00C1	01	C400016A	LD	L	DEC72
00C3	0	D052	STO		AREA
00C4	01	65800238	LDX	11	PONTS
00C6	0	620C	PUNCH LDX	2	12
00C7	01	C40001CC	CONV	LD	L
00C9	20	02255103	LIBF		BINDC
00CA	1	0117	DC		OTPUT
00CB	01	740600CA	MDX	L	OTP,6
00CD	01	740100C8	MDX	L	CONV+1,1
00CE	0	72FF	MDX	2	-1
00D0	0	70F6	MDX		CONV
00D1	20	03059115	LIBF		CARDN
00D2	0	2000	DC		/2000
00D3	1	0116	DC		AREA
00D4	0	0000	DC		0
00D5	20	03059115	LIBF		CARDN
00D6	0	0000	DC		/0000
00D7	0	70FD	MDX		*-3
00D8	01	74B800CA	MDX	L	OTP,-72
00DA	0	71F4	MDX	1	-12
00DB	0	70EA	MDX		PUNCH
00DC	01	C4000238	LD	L	PONTS
00DE	0	1890	SRT		16
00DF	01	AC000169	D	L	DEC12
00E1	0	1090	SLT		16
00E2	01	B4000167	CMP	L	ZERO
00E4	0	7002	MDX		GOON
00E5	0	7023	MDX		RSTOR
00E6	0	7022	MDX		RSTOR
00E7	01	D400016B	GOON STO	L	REST
00E9	01	A4000168	M	L	DEC6
00EB	0	1090	SLT		16

00EC	01	04000116	STO	L	AREA	
00EF	0	0009	LD		CONV+1	SET ADDRESS IN AREA
00EF	0	0008	STO		CONVV+1	
00F0	01	8400016B	A	L	REST	
00F2	0	00D5	STO		CONV+1	
00F3	01	6680016B	LDX	12	REST	
00F5	00	C4000000	CONVV	LD	L	---
00F7	20	02255103	LIBF		BINDC	
00F8	1	0117	OTTP	DC	OTPUT	
00F9	01	740600F8	MDX	L	OTTP,6	
00FC	01	740100F6	MDX	L	CONVV+1,1	
00FD	0	72FF	MDX	2	-1	
00FE	0	70F6	MDX		CONVV	
00FF	20	03059115	LIBF		CARDN	
0100	0	2000	DC		/2000	
0101	1	0116	DC		AREA	
0102	0	0000	DC		0	
0103	20	03059115	LIBF		CARDN	
0104	0	0000	DC		/0000	
0105	0	70FD	MDX		---3	
0106	0	C0F1	LD		OTTP	RESTORES OTTP
0107	0	900E	S		AREA	
0108	0	D0EF	STO		OTTP	
0109	01	C40000C8	RSTOR	LD	L	CONV+1
						RESTORES ADR. IN CONV+1
010B	01	94000238	S	L	PONTS	
010D	01	D40000C8	STO	L	CONV+1	
010F	30	059C98C0	OUT	CALL	EXIT	
0112		0000	BSS	E	0	
0112	0	0000	IOCCA	DC	/0000	READ DATA ENTRY SW.
0113	0	0740	DC		/0740	
0114	0	0001	MASC	DC	/0001	
0115	0	0002	MASC2	DC	/0002	MASK FOR DES 2
0116	0	0000	AREA	DC	---	OUTPUT AREA FOR CARDS
0117		0050	OTPUT	BSS	80	
0167	0	0000	ZERO	DC	0	
0168	0	0006	DEC6	DC	6	
0169	0	000C	DEC12	DC	12	
016A	0	0048	DEC72	DC	72	
016B	0	0000	REST	DC	---	
016C		0060	AREAG	BSS	96	STOR. 1. CHANNEL
01CC		0060	AREAH	BSS	96	STOR. 2. CHANNEL
022C	0	0009	DEC9	DC	9	
022D	0	0000	INPTS	DC	---	
022E	0	0000	TNPTS	DC	---	
022F	0	0000	FNPTS	DC	---	
0230		0003	DVSR	BSS	3	
0234		0000		BSS	E	0
0234	31	06253C00	INFORM	DSA	FIL20	INFORMATION FOR EXP.CONST
0237	0	0000	DELAY	DC	---	
0238	0	0000	PONTS	DC	---	
0239	0	0000	WAVES	DC	---	
023A	0	0000	CLICK	DC	---	
023B		0006		BSS	6	
0242		0000		BSS	E	0
0242	31	06253CB2	CPVST	DSA	FIL22	USES FIL22 AND FIL23
0245		0240	AREAD	BSS	576	SQUARE OF RANDOM FLUCTU.
0485	1	0245	ADRD	DC	AREAD	
0486	0	0001	DEC1	DC	1	
0487	0	0240	WORDC	DC	576	
0488	0	0001	CARIG	DC	1	
0489	0	8181		DC	/8181	
048A	0	0008		DC	8	
048B		0008	OUTPT	BSS	8	
0493	0	2121		DC	/2121	
0494	0	0000		DC	DMESA-DMES1	
0495		0018	DMES1	DMES		'2RRMS VALUES OF PRESSURE'E

04A1	0	8105		DC	/8105
04A2		0000	DMESA	BES	0
04A2	0	001B		DC	DMESB-DMES2
04A3		001B	DMES2	DMES	'2RMS VALUES OF THE RANDOM '
04B0		0019		DMES	COMPONENT OF THE VELOCITY'E
04C0	0	8105		DC	/8105
04DE		0000	DMESB	BES	0
04DE		0000		END	START

NO ERRORS IN ABOVE ASSEMBLY.

CONVT

JUP FUNCTION COMPLETED

// JOB 0000011111

// END OF ALL JOBS